

Techno-economic study of CO₂ capture plant with heat pump

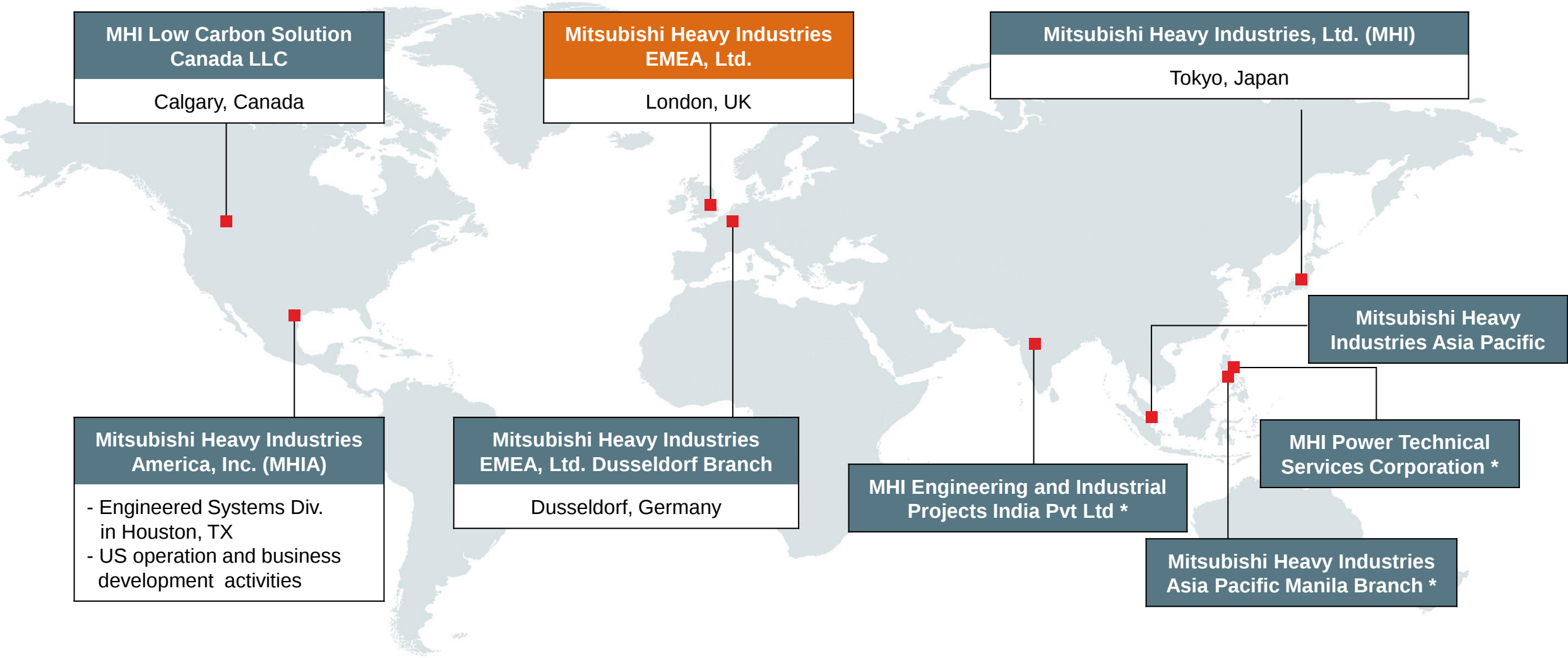
PCCC8
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Akihito Otani
Process Engineering Manager

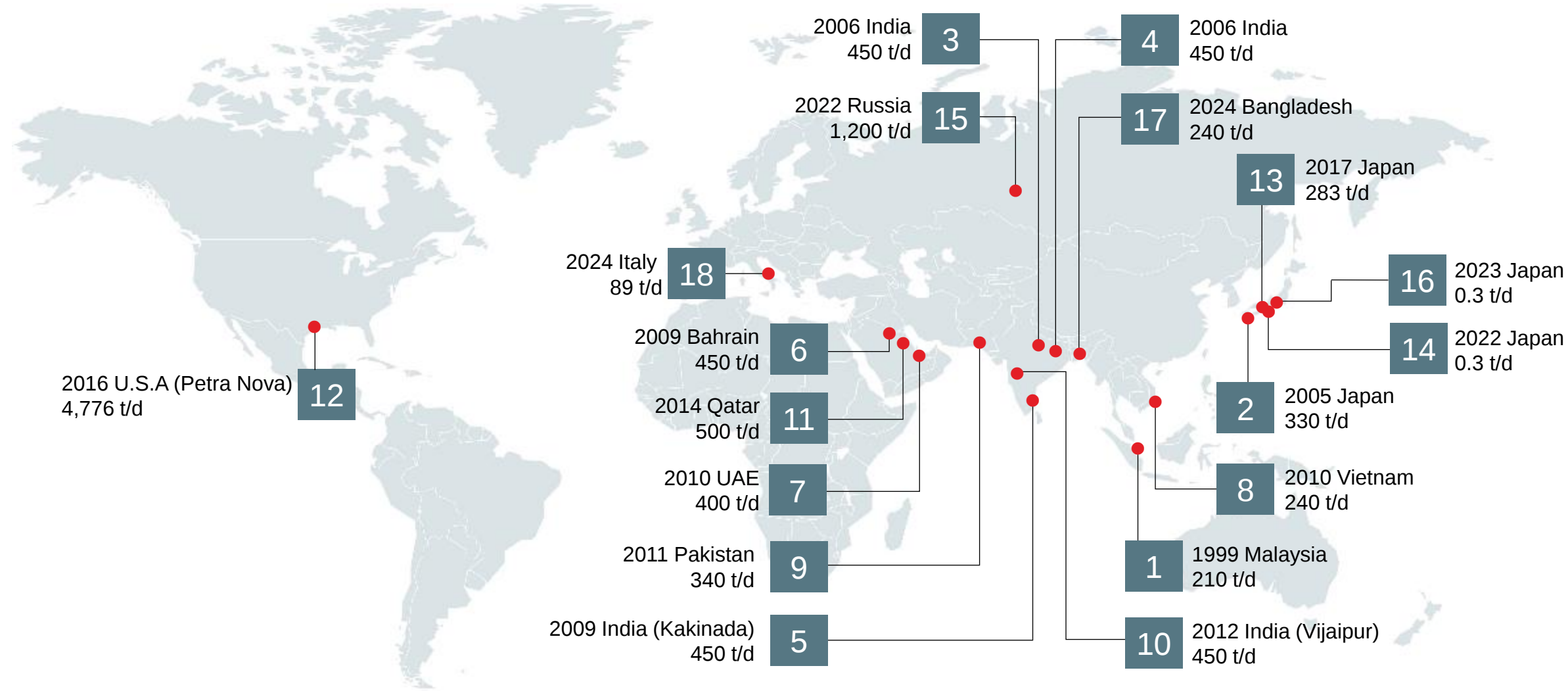
Mitsubishi Heavy Industries EMEA, Limited.

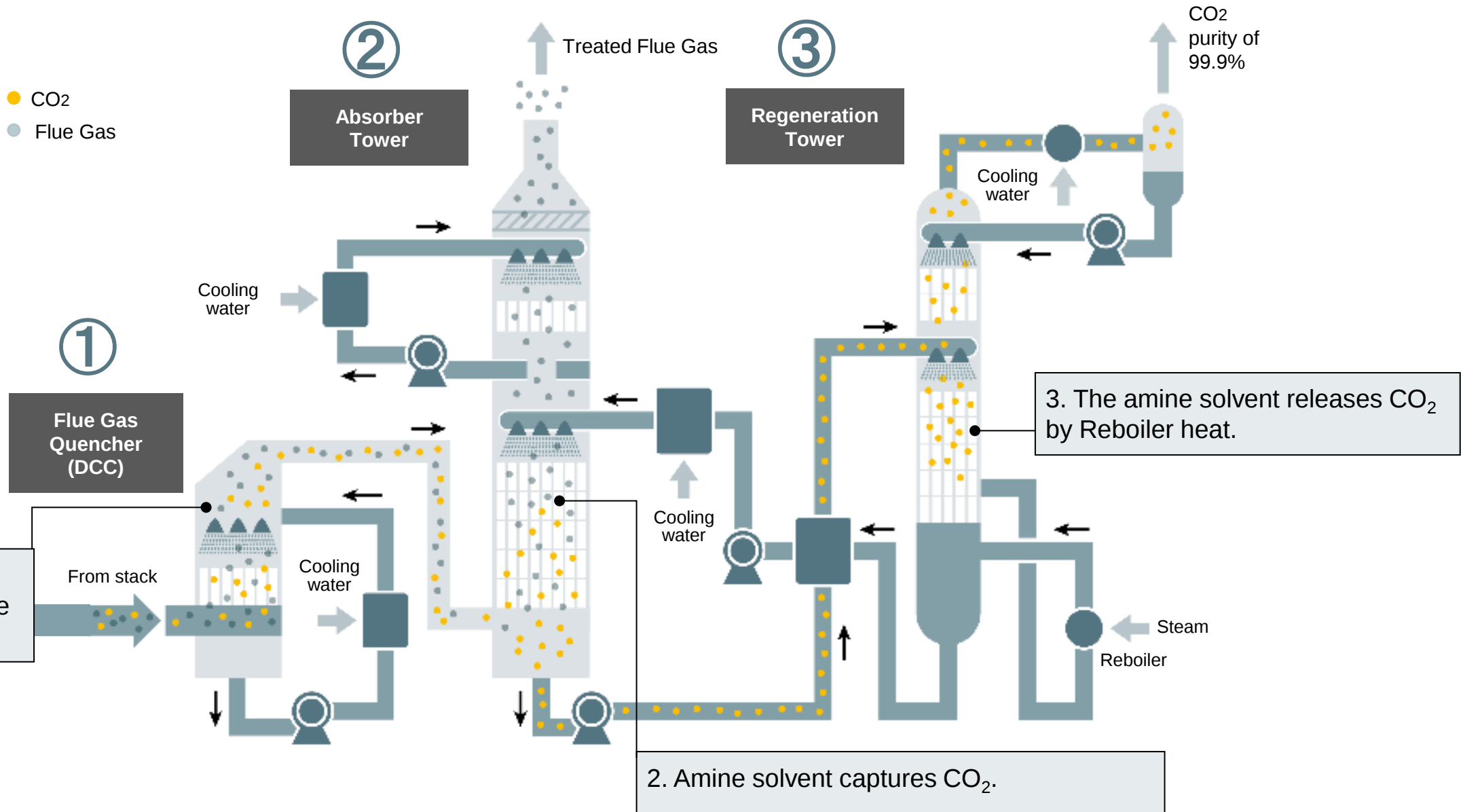


Mitsubishi Heavy Industries (MHI) CO₂ capture business global operation



* High value engineering function in India and Philippines







OVER 40 YEARS OF A VIABLE SUSTAINABILITY

Since 1980, Turboden S.p.A. is a pioneer in the energy transition, offering technological solutions to industries and utilities for **heat decarbonization and power generation**, in particular:

- **Large Heat Pump (LHP) and Mechanical Vapor Recompression (MVR)** for heat supply decarbonization.
- **Organic Rankine Cycle (ORC) System and Gas Expander** for green distributed electrical power generation in multiple applications (geothermal, biomass, waste heat recovery);

Having established itself as a **world-leading company in sustainable power production**, with 460 Organic Rankine Cycle (ORC) plants in more than 50 countries, Turboden is one of the major technology partners for energy efficiency and sustainability.



From 2013, Turboden is part of MHI Group. Today, Turboden and MHI are committed to **achieving carbon neutrality by 2040** – *Mission Net Zero* – both in their operations as well as in their value chain.

Turboden S.p.A, MHI group company, received orders of large heat pump

Site: Brescia, Italy
Customer: Ironworks(O.R.I. MARTIN S.P.A.)



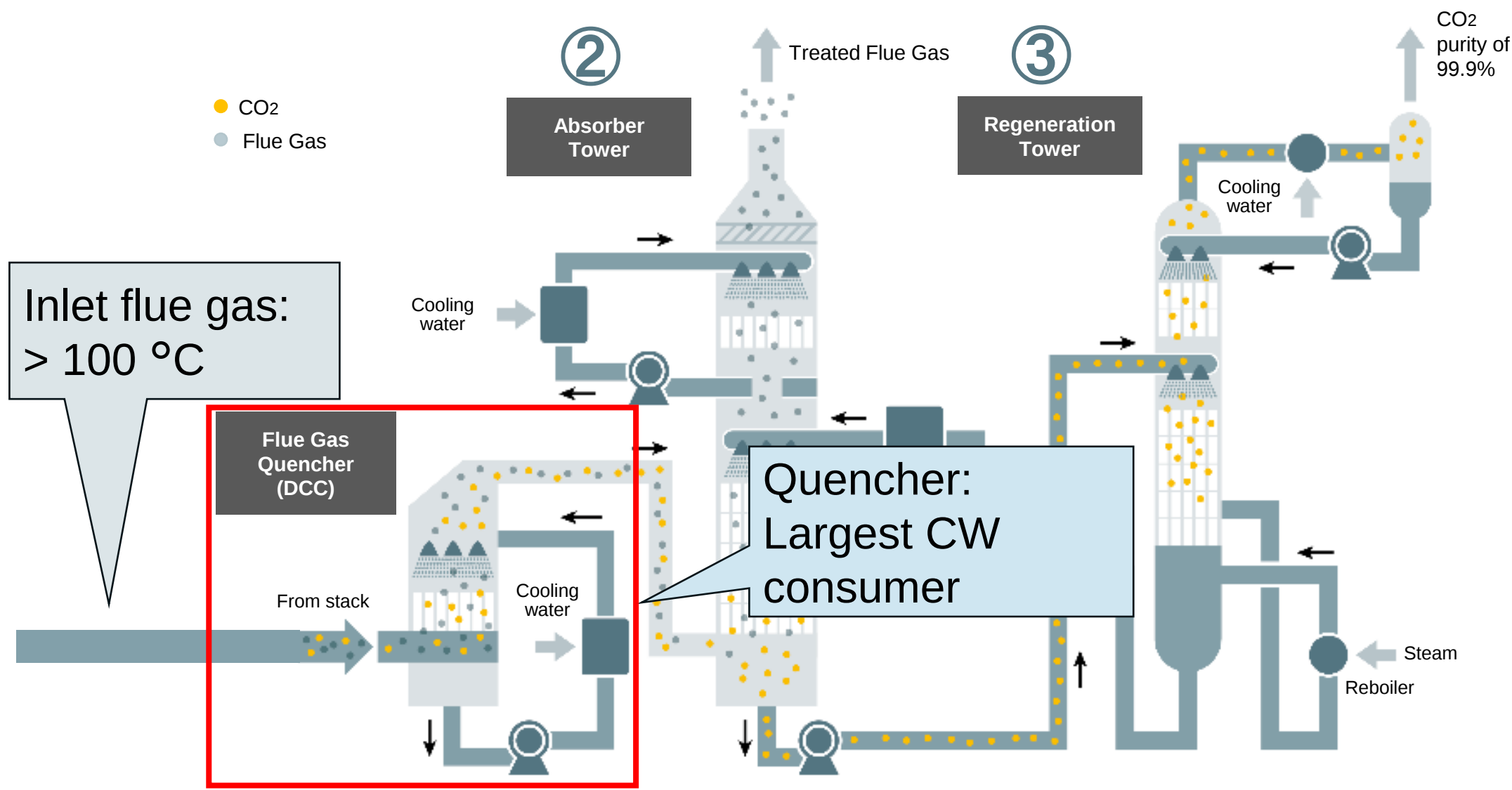
Power: **6MWt** up to 120deg.C

Site: Northern EU
Customer: Pulp & paper company

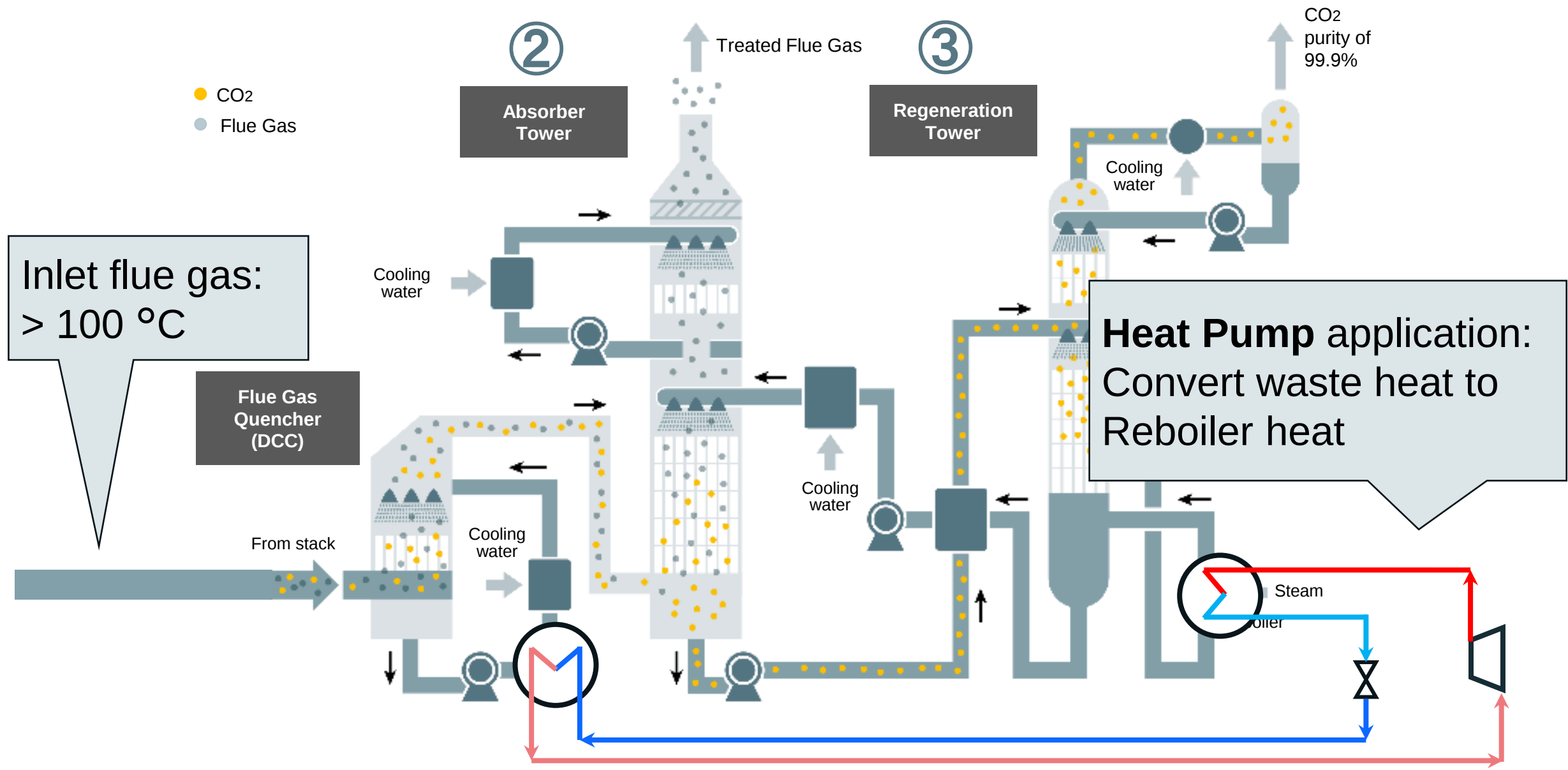


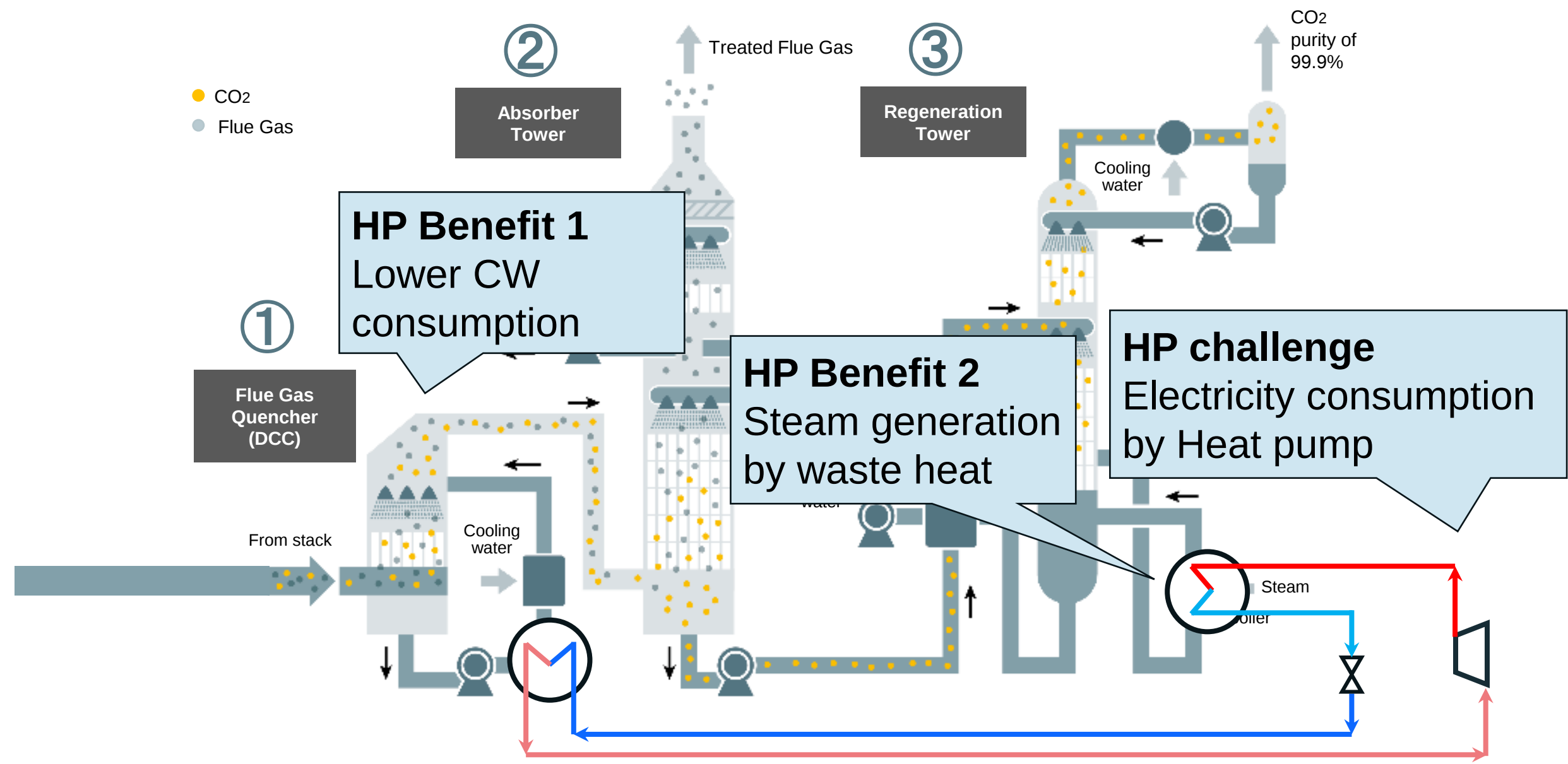
Power: **12MWt** steam @170deg.C

KM CDR Process™ with Heat Pump Concept



KM CDR Process™ with Heat Pump Concept





Aim of this study

KM CDR™ with Heat Pump vs Steam Boiler

- Sensitive analysis of utility price
(Electricity price VS Steam price)

Utility Cost's Sensitive analysis

- CAPEX
- OPEX
- Total of CAPEX+OPEX
- COP analysis
- Cost matrix evaluation

Key performance indicator: COP

$$\text{COP (Coefficient of Performance)} = \frac{Q}{W}$$

*Higher COP = efficient heat pump system

Q: Heat supplied by the heat pump (Heat)

W: Net work input to the system (Electricity)

- Case study conditions

	Project A (Europe)
Flue gas source	Cement
Capture ratio (%)	90
Flue gas flow rate (Nm ³ /hr @101.3kPa 15 °C)	310,000
Flue gas pressure (barG)	0
Flue gas temperature (°C)	130
Flue gas H ₂ O concentration (mol%)	34
Flue gas CO ₂ concentration (mol%-dry)	18.6
Product CO ₂ capacity (tonne/day)	1,700 (0.6 TPA)
Product CO ₂ concentration (%-dry)	More than 99.9
Product CO ₂ temperature (°C)	35

→Heat Pump COP=2.8

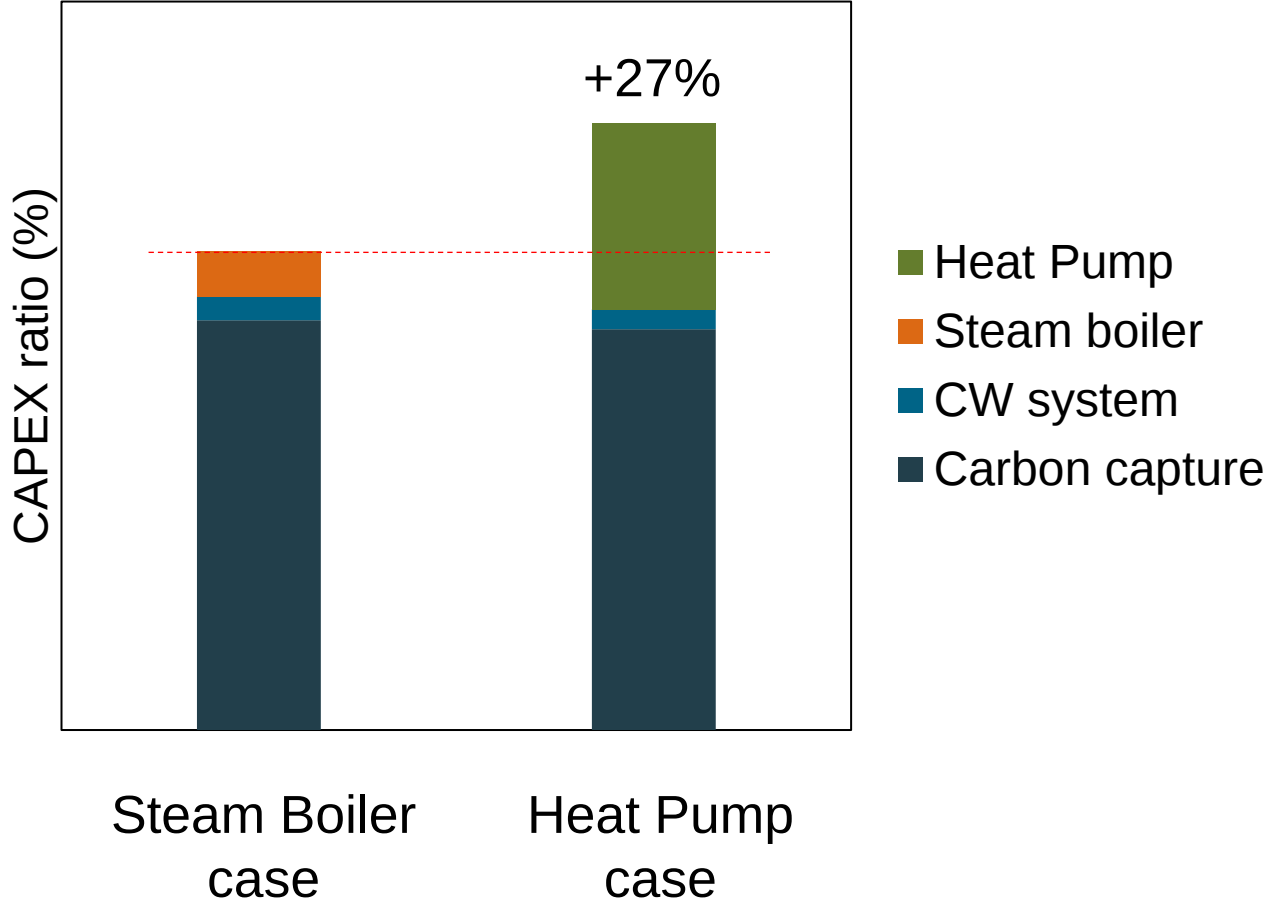
- CAPEX components

CAPEX	Direct cost	Purchased equipment
		Instrumentation
		Electrical
		Piping
		Construction
	Indirect cost	Engineering
		Construction
		Transportation
		Process license fee
		Contingency
KS-21™ initial fill		

→EPC price

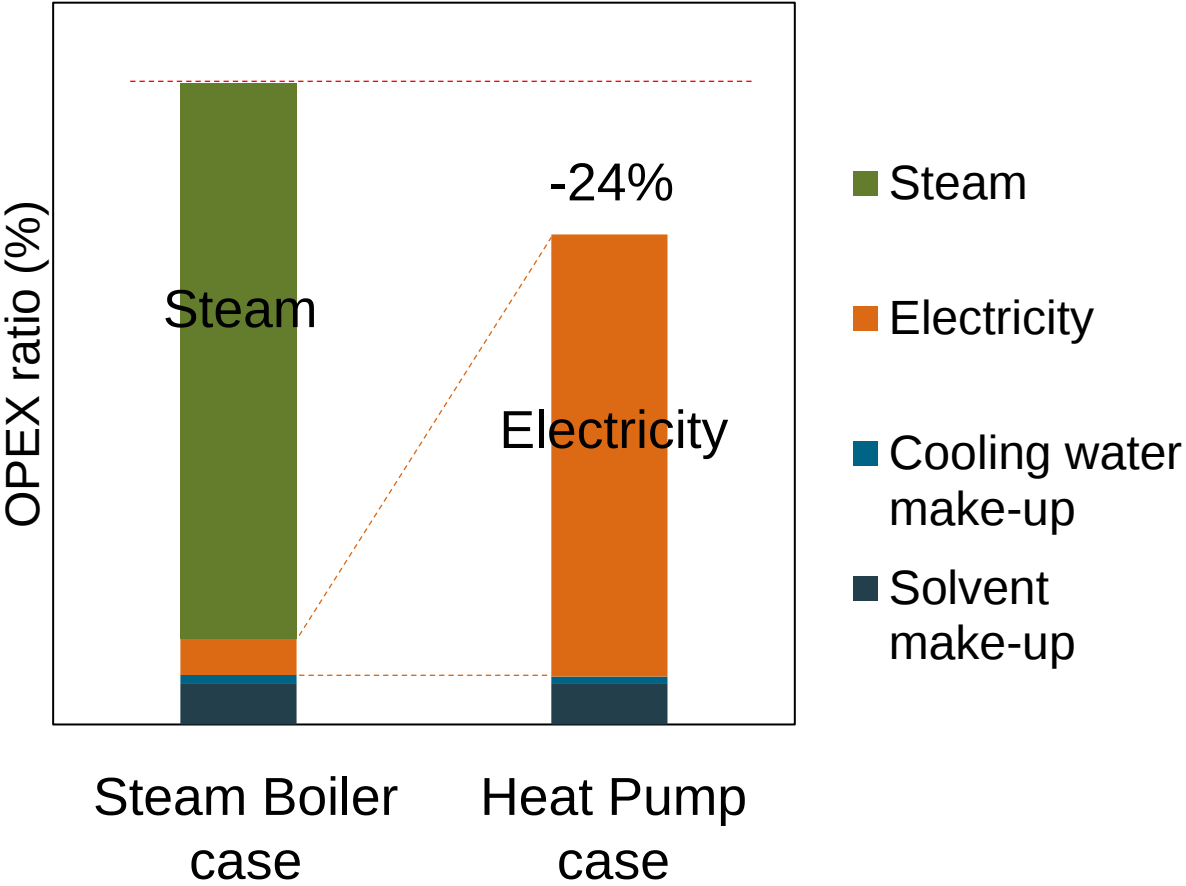
Steam boiler case:
Heat pump case:

Reboiler heat generation by steam boiler
Reboiler heat generation by heat pump



Next step:
How much OPEX benefit is required to overcome CAPEX increase?

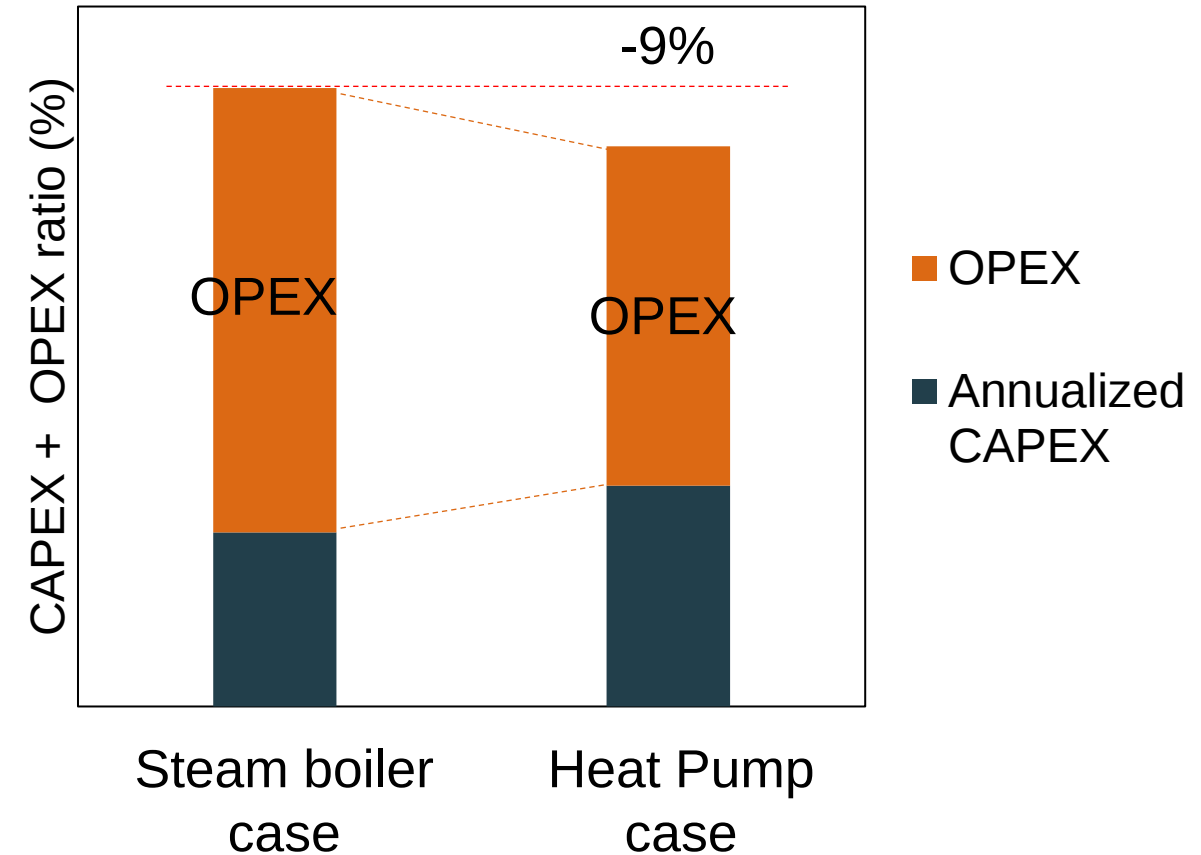
Electricity price	100 Euro/MWh
(Example of European price)	
LP steam price	30 Euro/ton-steam
Equivalent Natural Gas price	12 Euro/MMBTU
(Example of European price)	
Cooling water make-up	0.2 Euro/m ³
Solvent cost	Be considered



- CAPEX annualization & normalization conditions

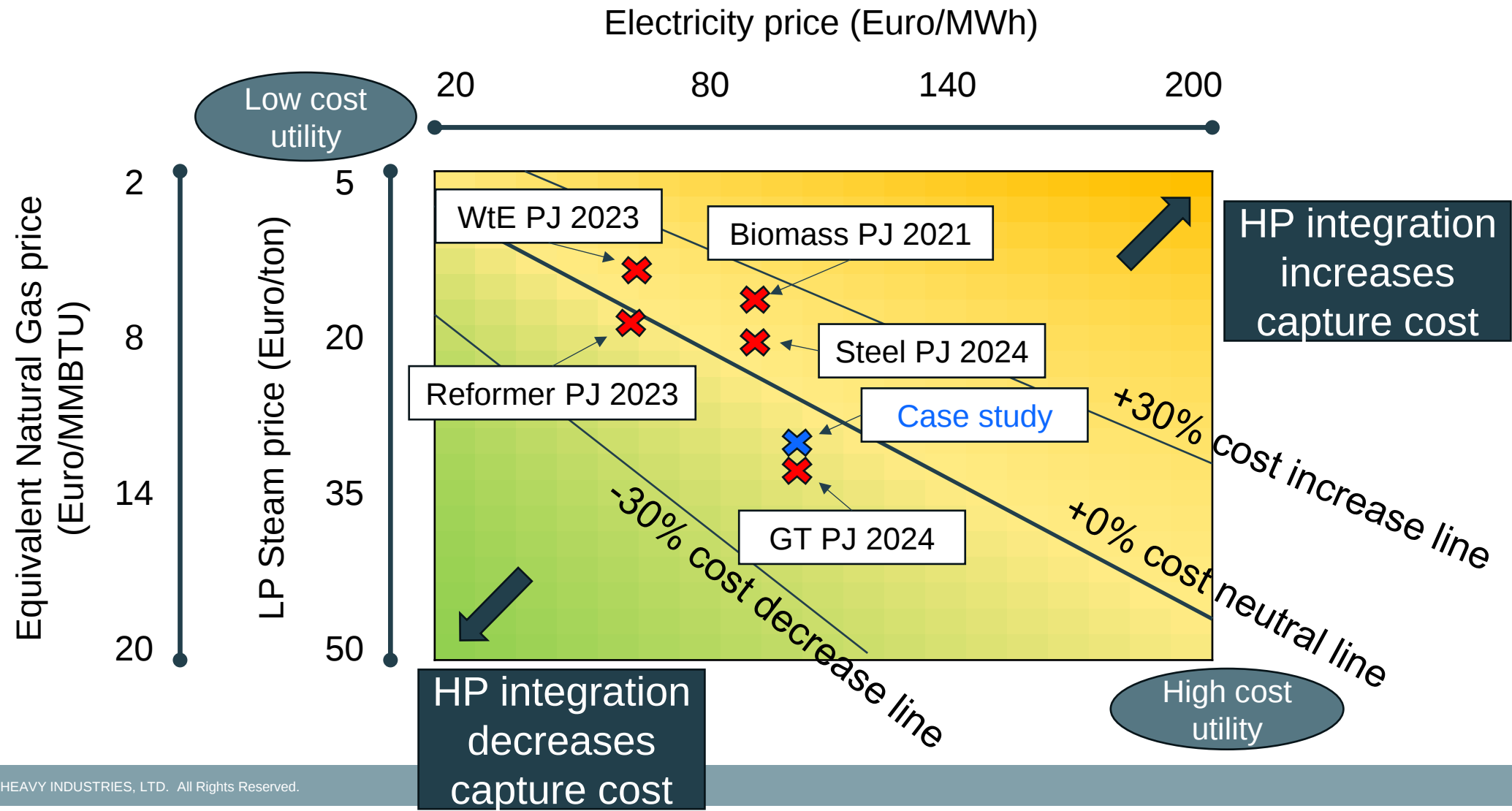
Availability	90%
Redundancy	10%
Discount rate	6.8%
Evaluation period	25 years
→Capital charge factor	0.084 1/yr

In this case study with Project A, capture cost decreases due to OPEX.

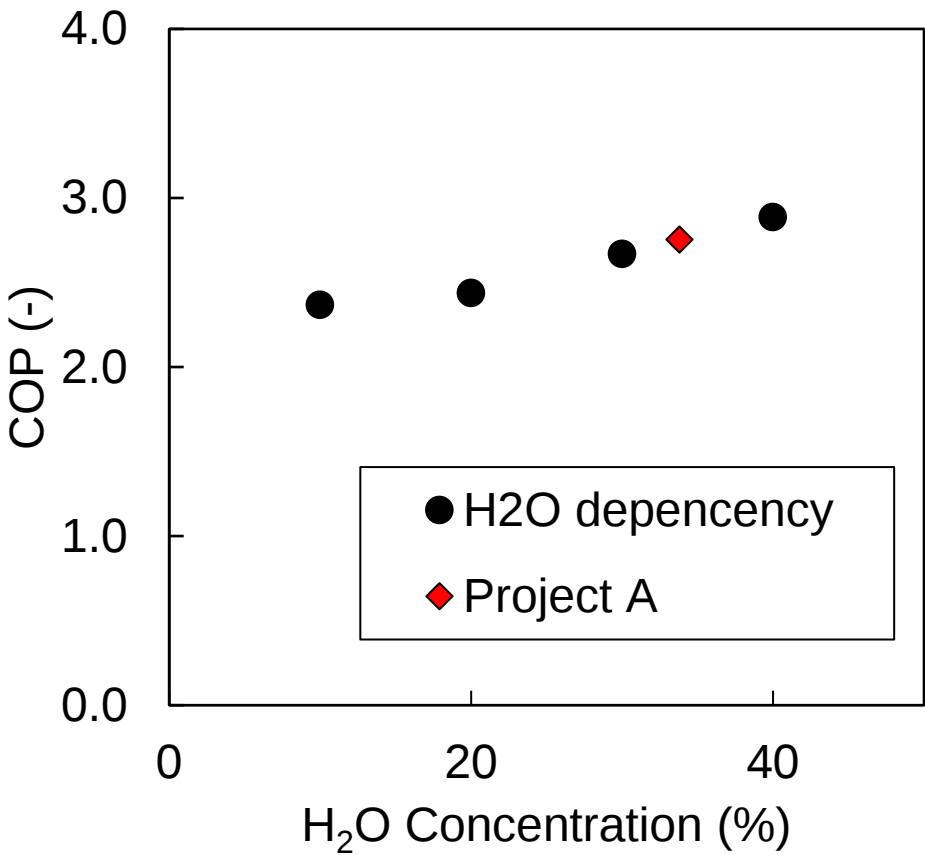


PJ A basis cost matrix (COP=2.8)

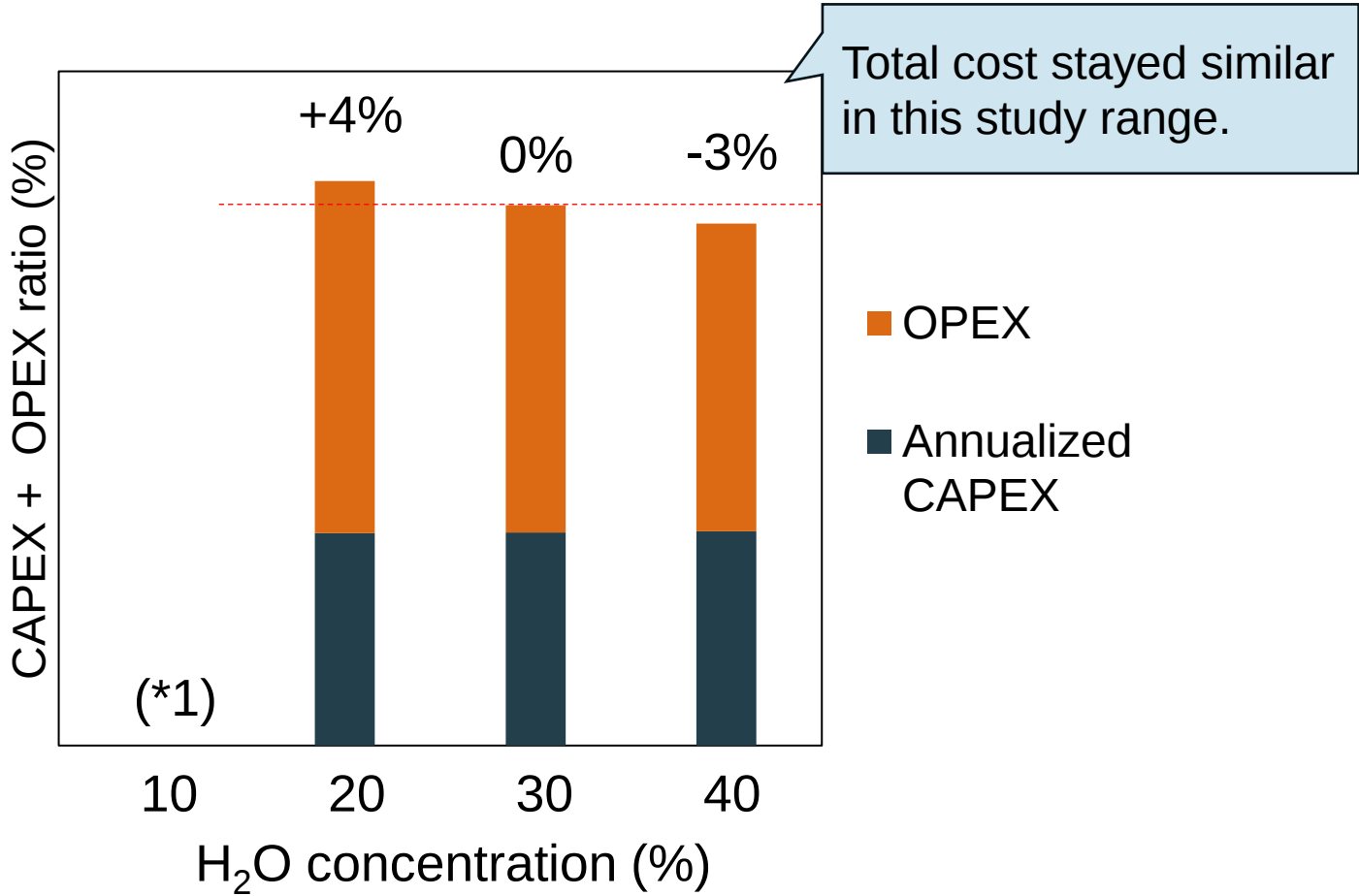
Initial assessment of $\frac{\text{Capture Cost of HP case}}{\text{Capture Cost of Boiler case}}$ (%) using utility price



COP vs H₂O concentration



Capture cost vs H₂O concentration



(*) Not enough heat to generate required steam amount.

Techno-economic study

- Electricity vs Steam price setting has big impact on effectiveness of HP integration.

CAPEX + OPEX study

- Cost matrix is useful for initial assessment of HP effectiveness.

NEXT STEP

- Confirm effects of parameters on COP and cost matrix:
 - H₂O conc. in FG dependency: done, limited effect in study range
 - CO₂ conc. in FG dependency: next
 - Inlet FG temperature dependency: next

