



# DMX DEMONSTRATION IN DUNKIRK (3D): RELIABILITY ANALYSIS OF EXPERIMENTAL DATA

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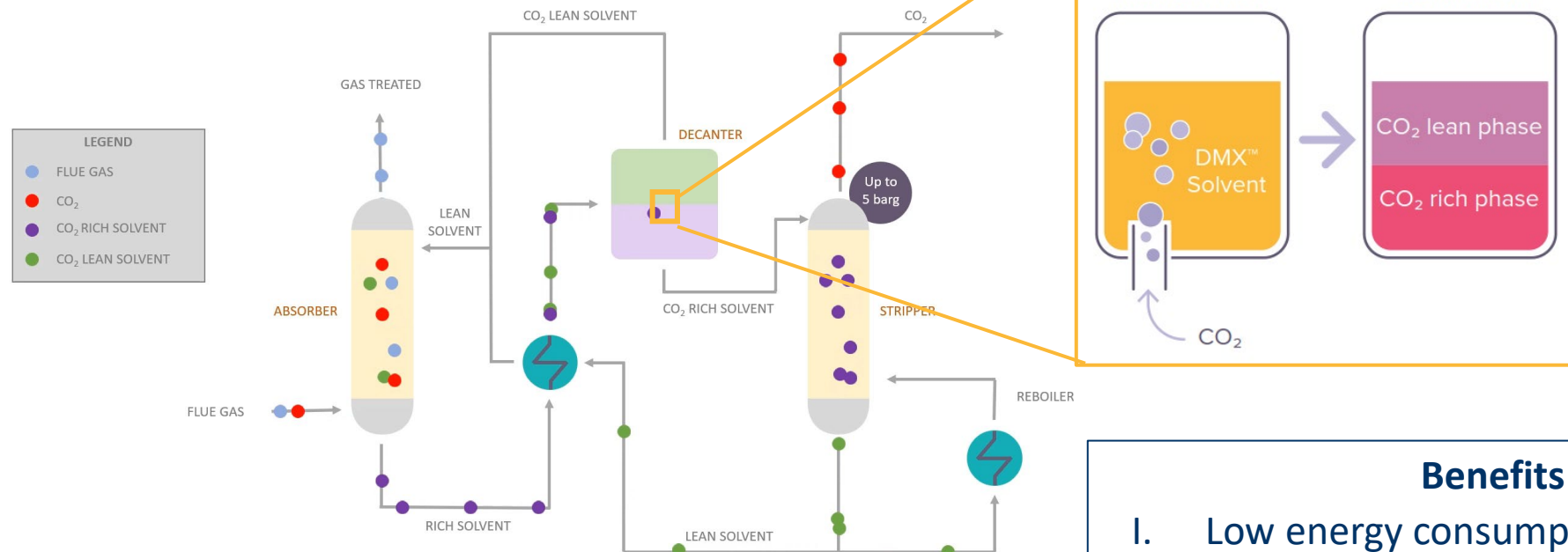


# PLAN

- ❑ DMX technology
- ❑ 3D demonstrator
- ❑ Experimental plan of 2024 campaign
- ❑ Energy penalty uncertainty sources:
  - ❑ Reconciling mass balance discrepancies
  - ❑ Reconciling heat balance discrepancies
- ❑ Evaluation with inhouse simulator
- ❑ Conclusions

# POST-COMBUSTION - FLUE GAS - DMX™ PROCESS

## Flue Gas CO<sub>2</sub> capture - DMX™ Process

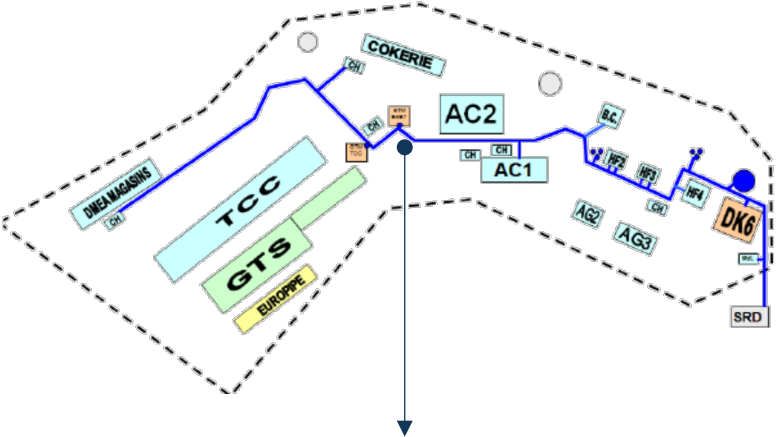


### Benefits of DMX Solvent

- Low energy consumption for capture rate > 90%
- Thermally stable solvent with low sensitivity to oxygen
- High purity of CO<sub>2</sub> produced at high pressure

# THE 3D DEMONSTRATOR (1/2)

ArcelorMittal France (AMF) Blast Furnace Gas Network



Treating actual blast furnace gases to evaluate the solvent stability over time

| Component       | Unit     | Value |
|-----------------|----------|-------|
| CO              | dry mol% | 24    |
| CO <sub>2</sub> | dry mol% | 25    |
| H <sub>2</sub>  | dry mol% | 4     |
| N <sub>2</sub>  | dry mol% | 47    |
| Others          | dry mol% | <0.3  |
| Total           | dry mol% | 100.0 |

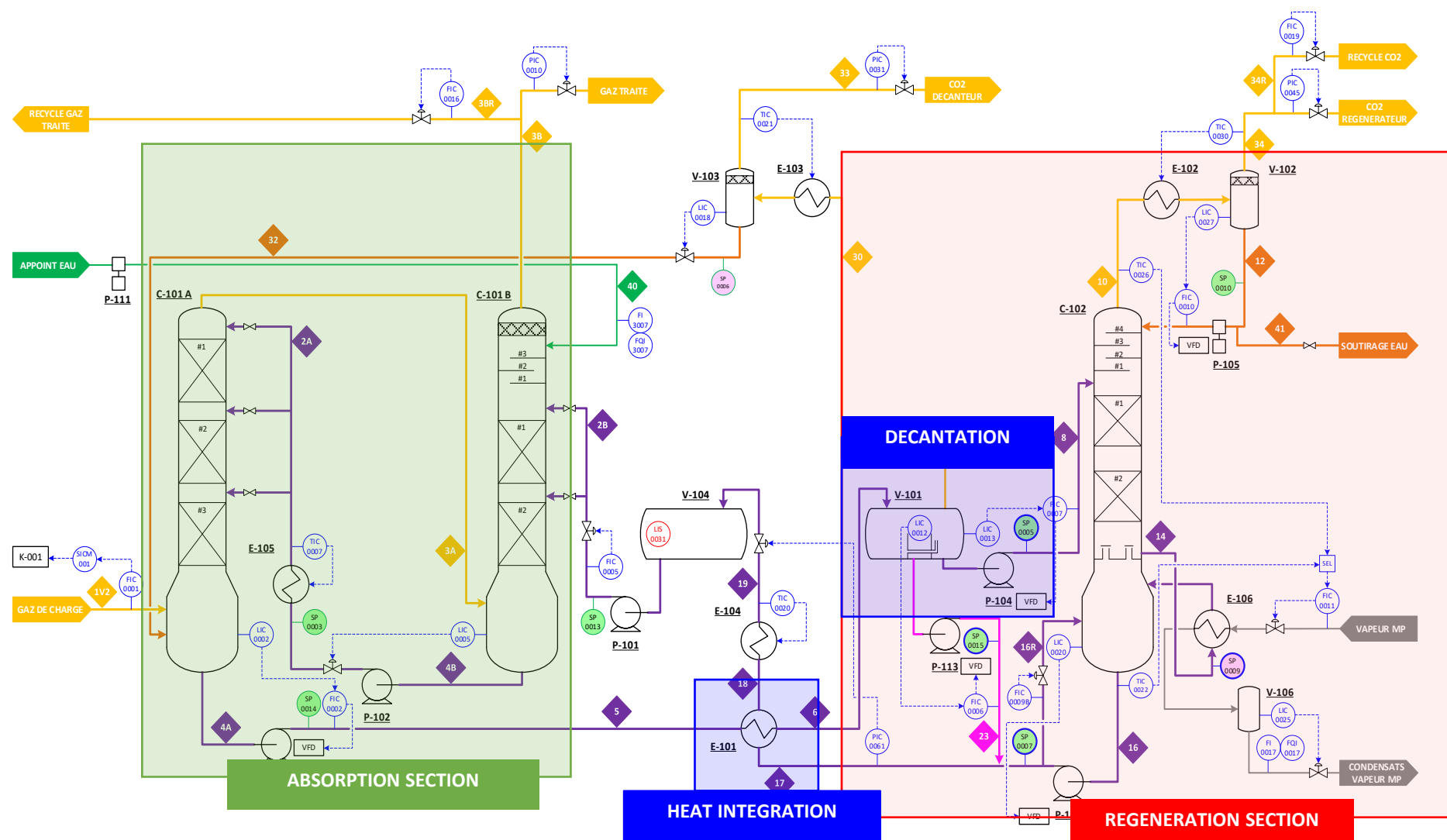


Large enough to be representative for industrial scaling-up

| Key values            |                         |
|-----------------------|-------------------------|
| Columns height        | 30 m                    |
| Columns diameter      | 350 - 450 mm            |
| Absorption pressure   | 0.1 – 1.8 barg          |
| Regeneration pressure | 2 – 5 barg              |
| Gas flowrate          | 200 – 1100 Nm3/h        |
| Solvent flowrate      | 2500 – 7500 kg/h        |
| Design capacity       | 0.5 tCO <sub>2</sub> /h |

| Small enough to not perturb industrial activity |      |
|-------------------------------------------------|------|
| Ratio 3D/AMF                                    |      |
| BF Gas                                          | 0.1% |
| MP steam                                        | 0.6% |

# THE 3D DEMONSTRATOR (2/2)



# THE 3D DEMONSTRATOR (2/2)

## Utilities from AMF :

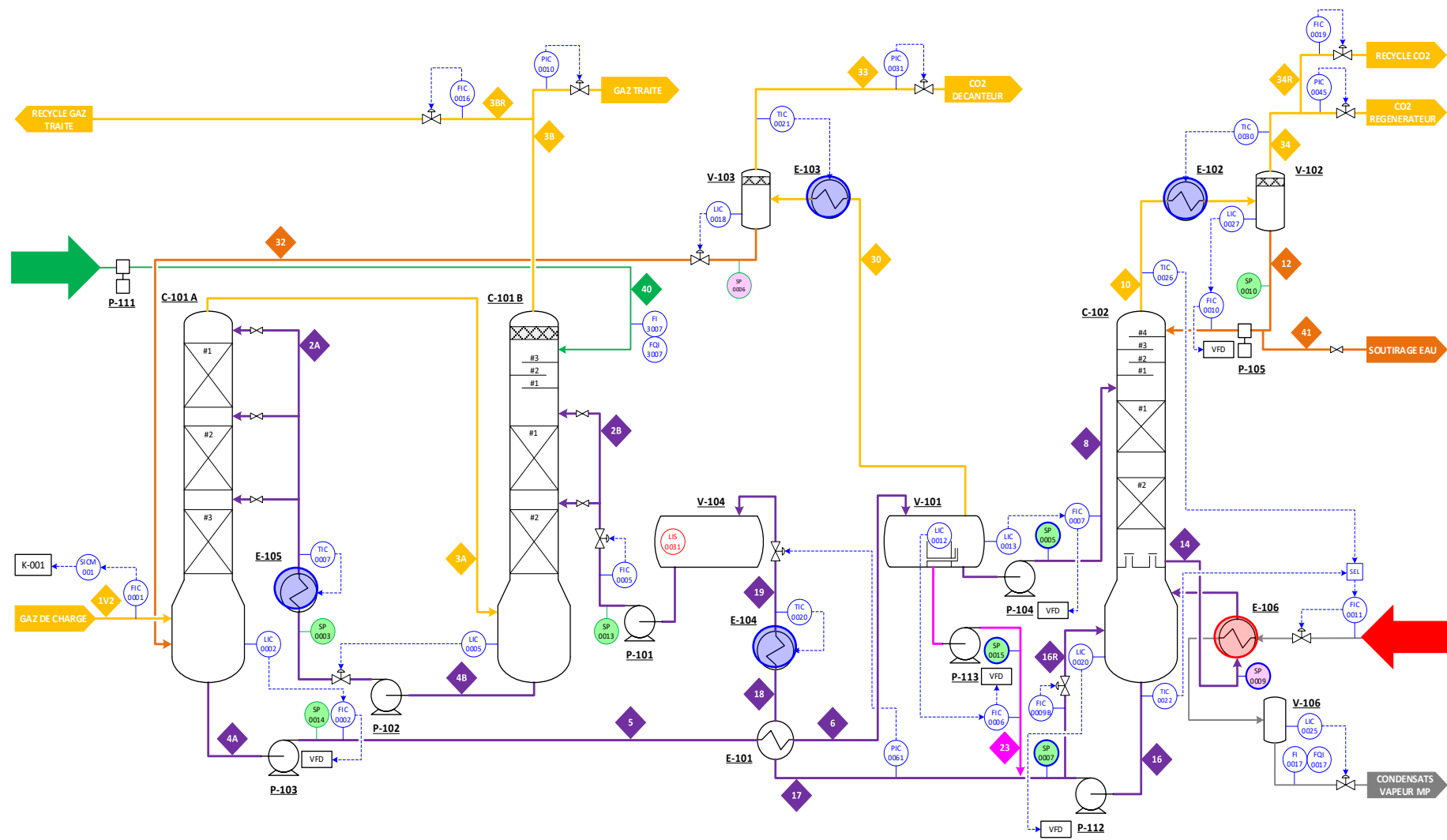
- Steam
- Water
- Electricity
- Nitrogen
- Air instrument

## Demineralized water production package

## Cooling water package (closed loop)

## Auxiliaries

- Solvent filtration
- Closed solvent drain network
- Anti-foam injection



Steam from  
AMF network

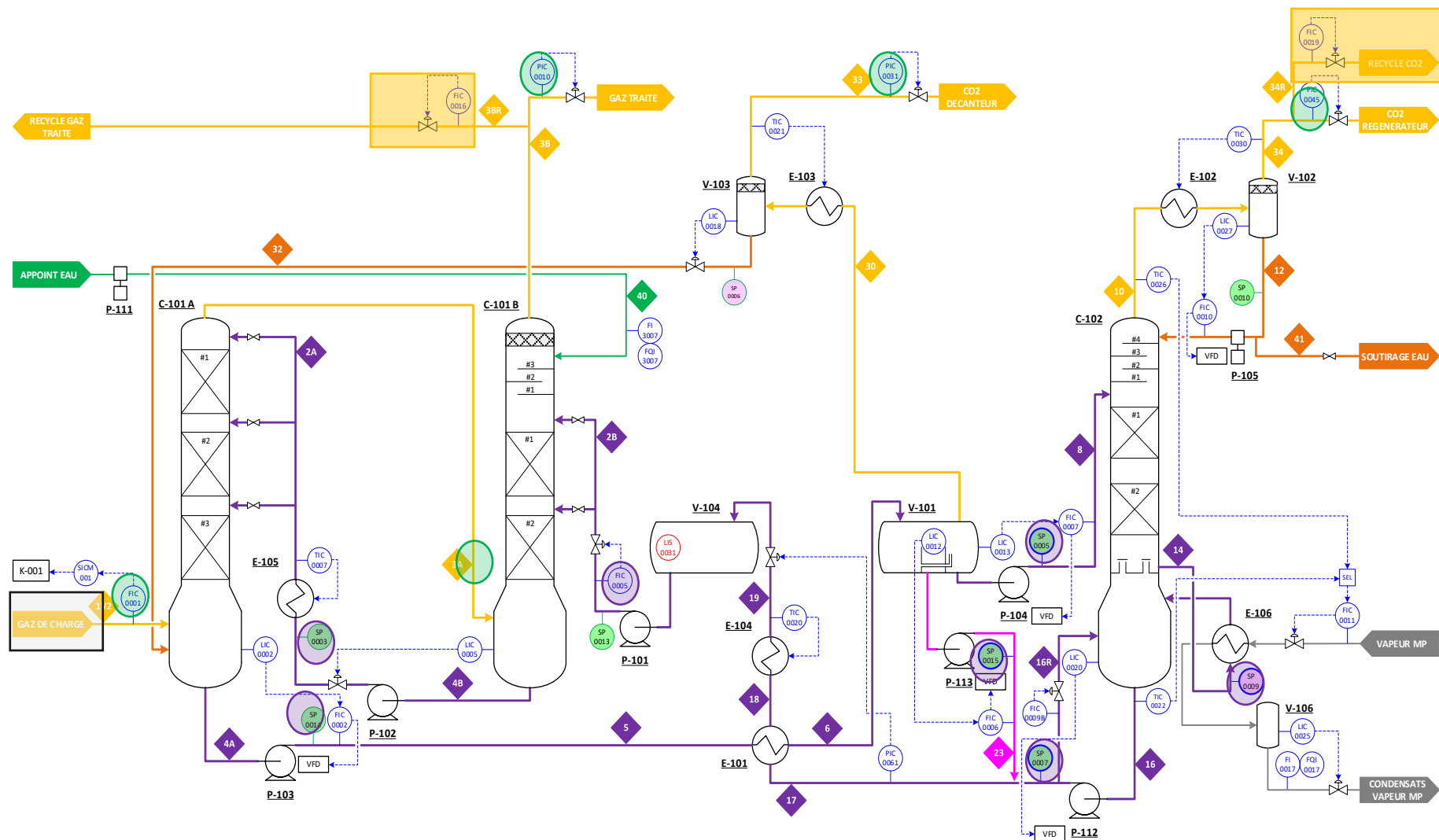
# THE 3D DEMONSTRATOR (2/2)

**Compressor:**  
To study different  
absorption pressures

**Gas recycling lines:**  
To study different CO<sub>2</sub>  
concentrations in the  
feed gas

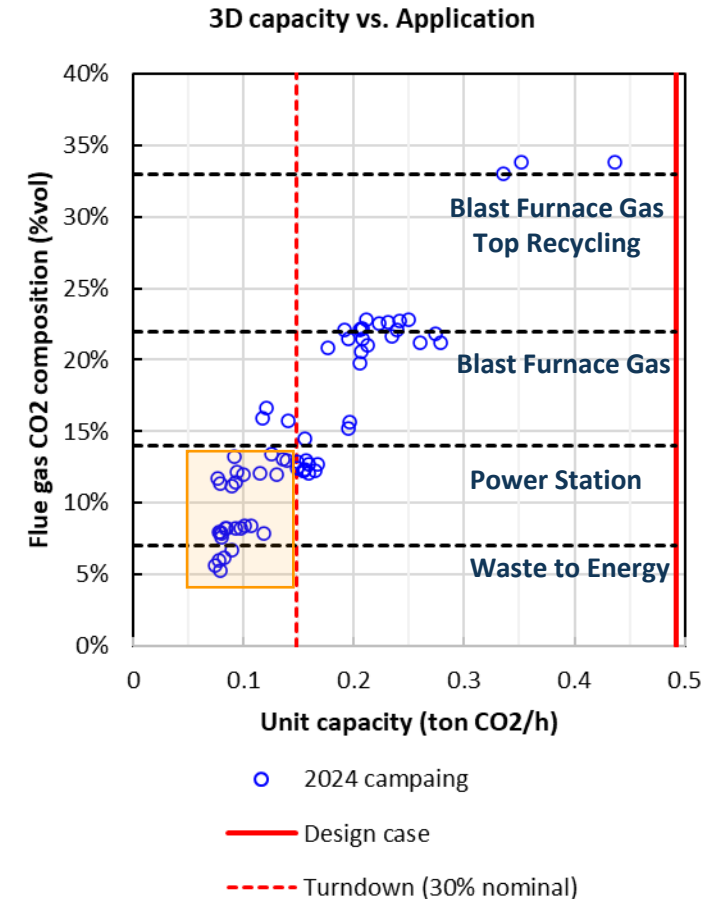
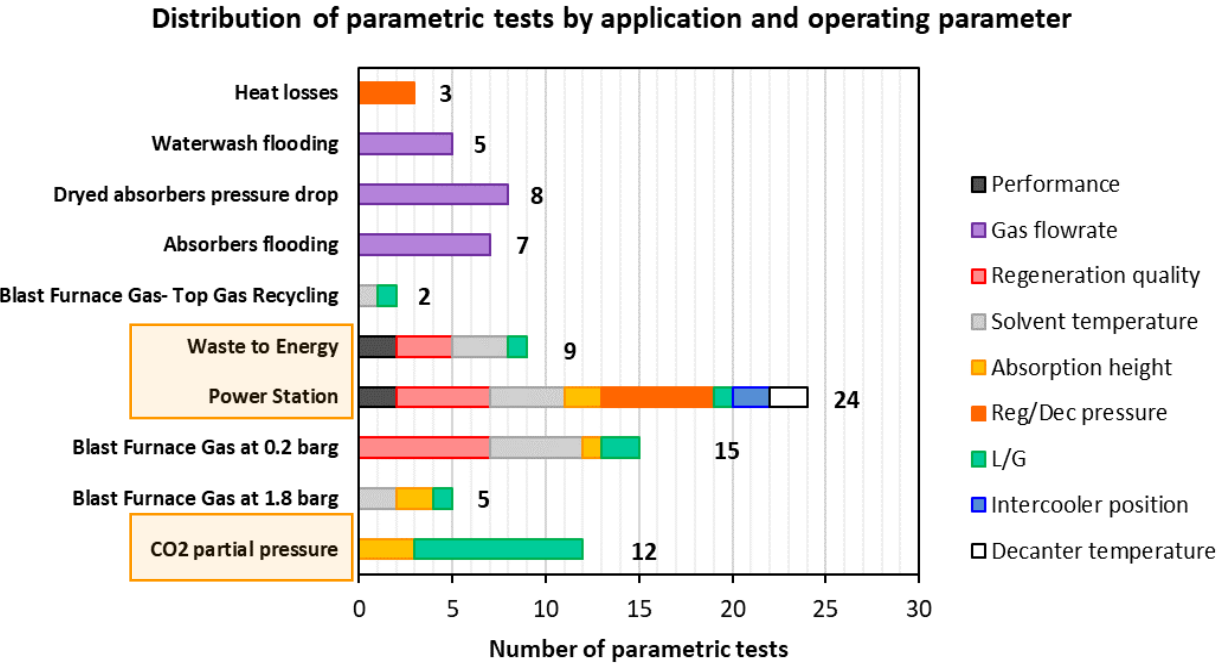
**Online Gas follow-up:**  
Flowmeter (vortex)  
Composition  
(FTIR &  $\mu$ GC)

**Liquid follow-up:**  
Flowmeter (Coriolis)  
Liquid sampling and  
on-site lab. analysis :  
▪ Amine content  
▪ CO<sub>2</sub> loading



# TOPOLOGY OF EXPERIMENTAL CAMPAIGN IN 2024

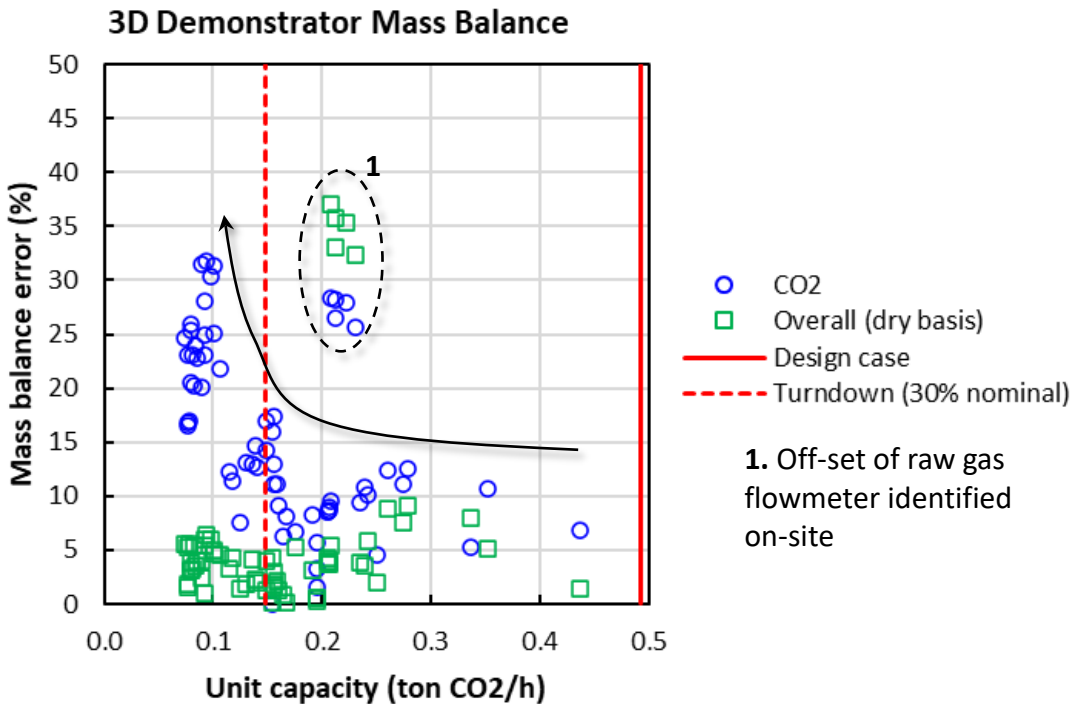
- Over 90 Test-Runs performed in which several operating parameter studied. Regeneration quality, L/G ratio and solvent temperature being the most important. **CO<sub>2</sub> capture** ratio and **energy penalty** amongst the most relevant performance indicators
- Motivation to enlarge DMX validation for low CO<sub>2</sub> content emitters, leading to operate at very low capacities (below turndown capacity, 30% of design capacity)



# ENERGY PENALTY UNCERTAINTY SOURCES

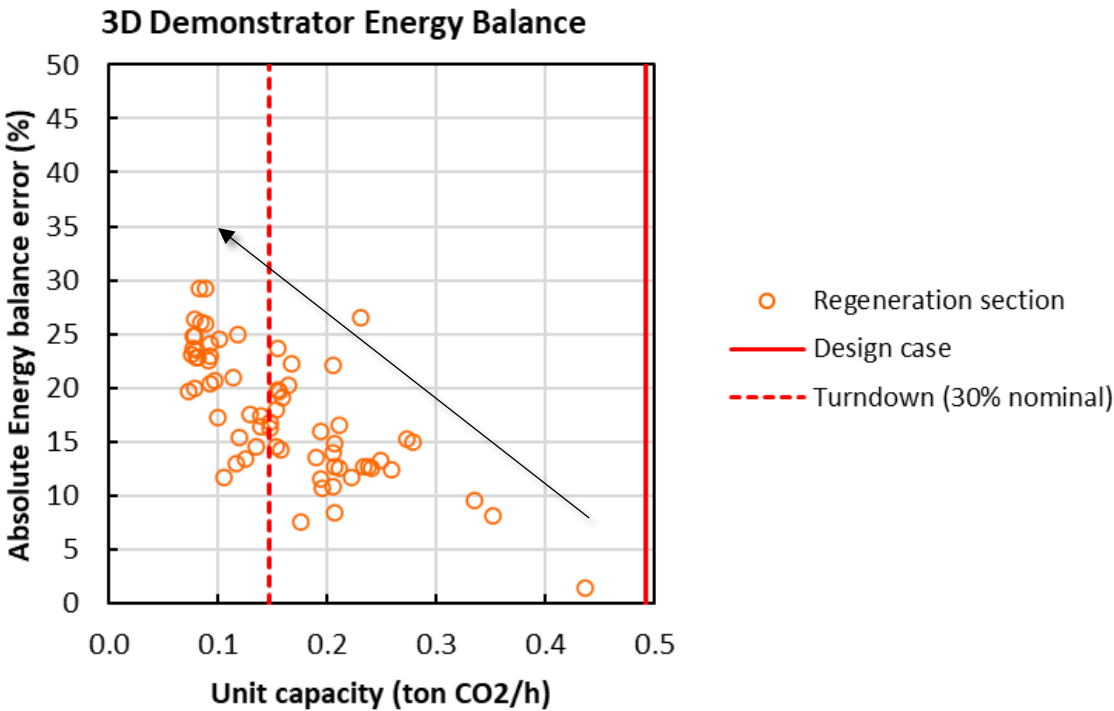
$$\text{Specific Reboiler Duty} = \frac{\text{Effective Reboiler Duty}}{\text{Captured CO}_2 \text{ capacity}}$$

## CO<sub>2</sub> capacity uncertainty evaluation through mass balances



Trend matches with CO<sub>2</sub> gas flowrate measurements falling below 10 % of full scale

## Effective Reboiler duty uncertainty evaluation through energy balance



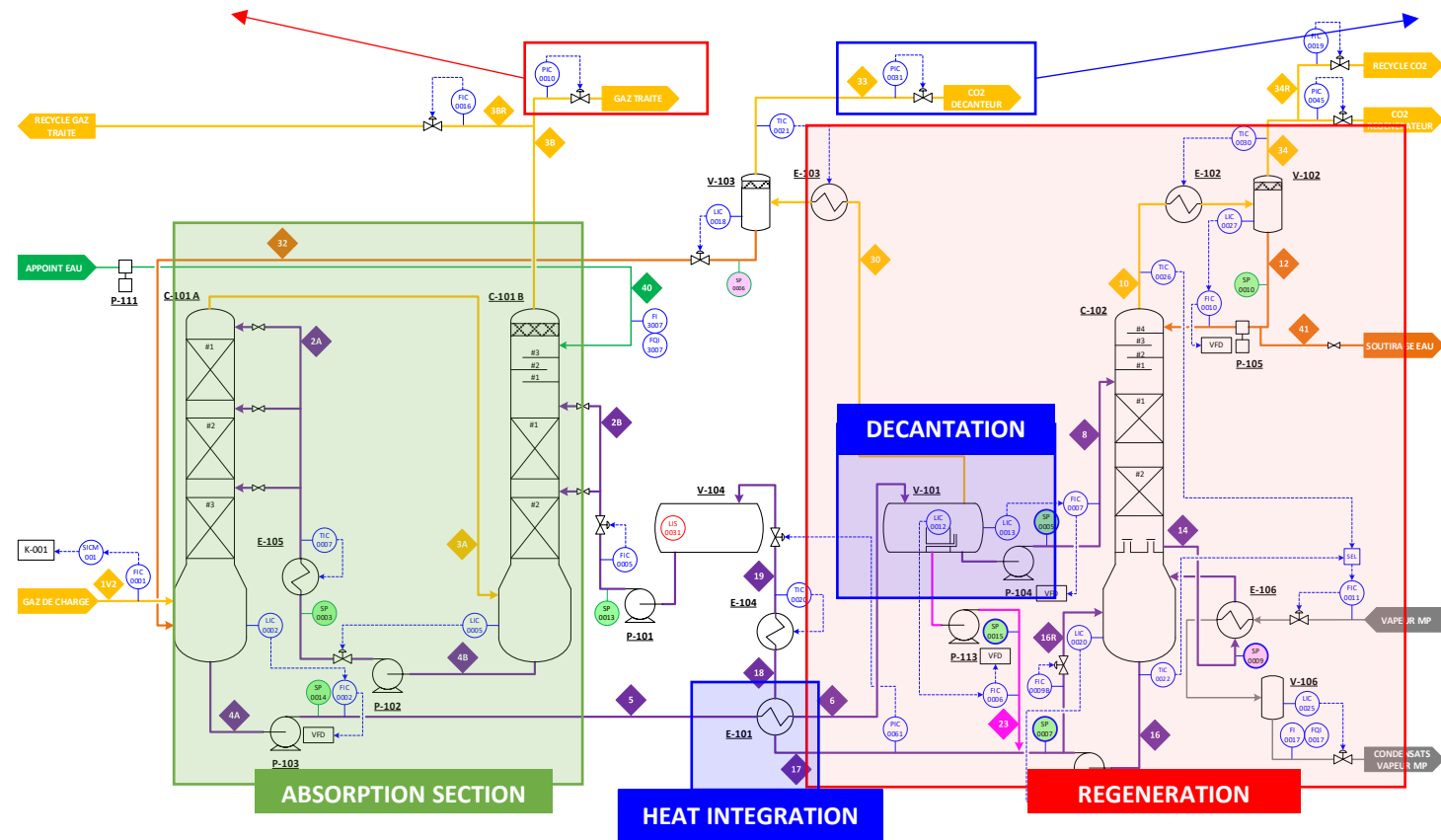
Trend matches with thermal losses from the facility to the environment

# RECONCILING MASS BALANCE DISCREPANCIES (1/2)

❑ Closing material balances loops leads to two alternatives :

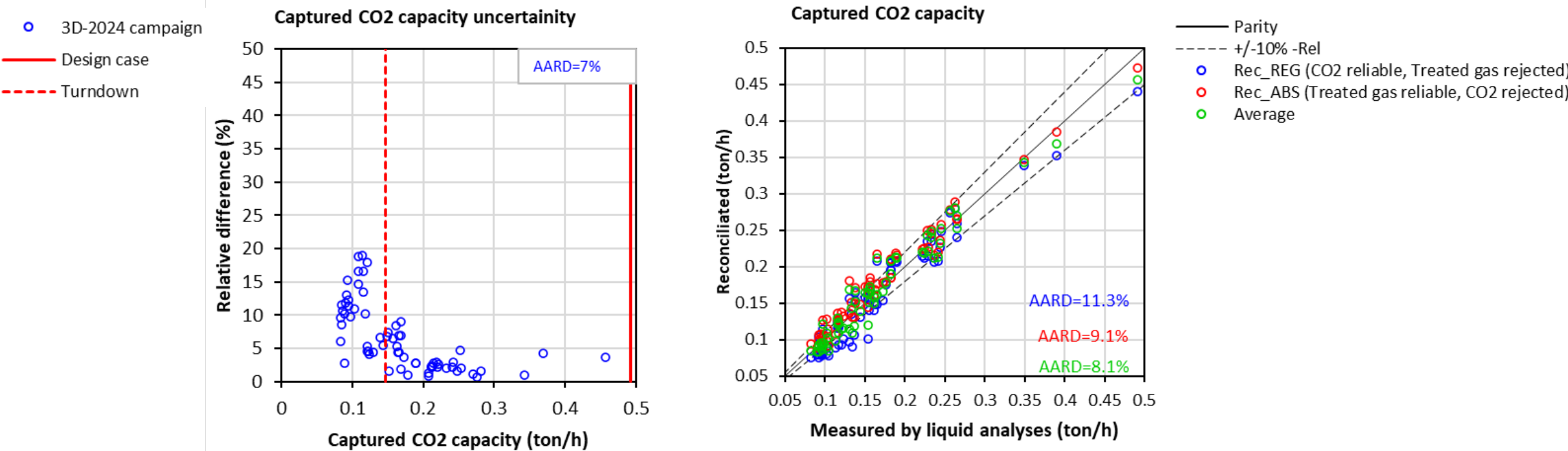
Treated gas flowrate measure reliable,  
CO<sub>2</sub> flowrate measure rejected  
**(Rec\_ABS)**

CO<sub>2</sub> flowrate measure reliable,  
Treated gas flowrate measure rejected  
**(Rec\_REG)**



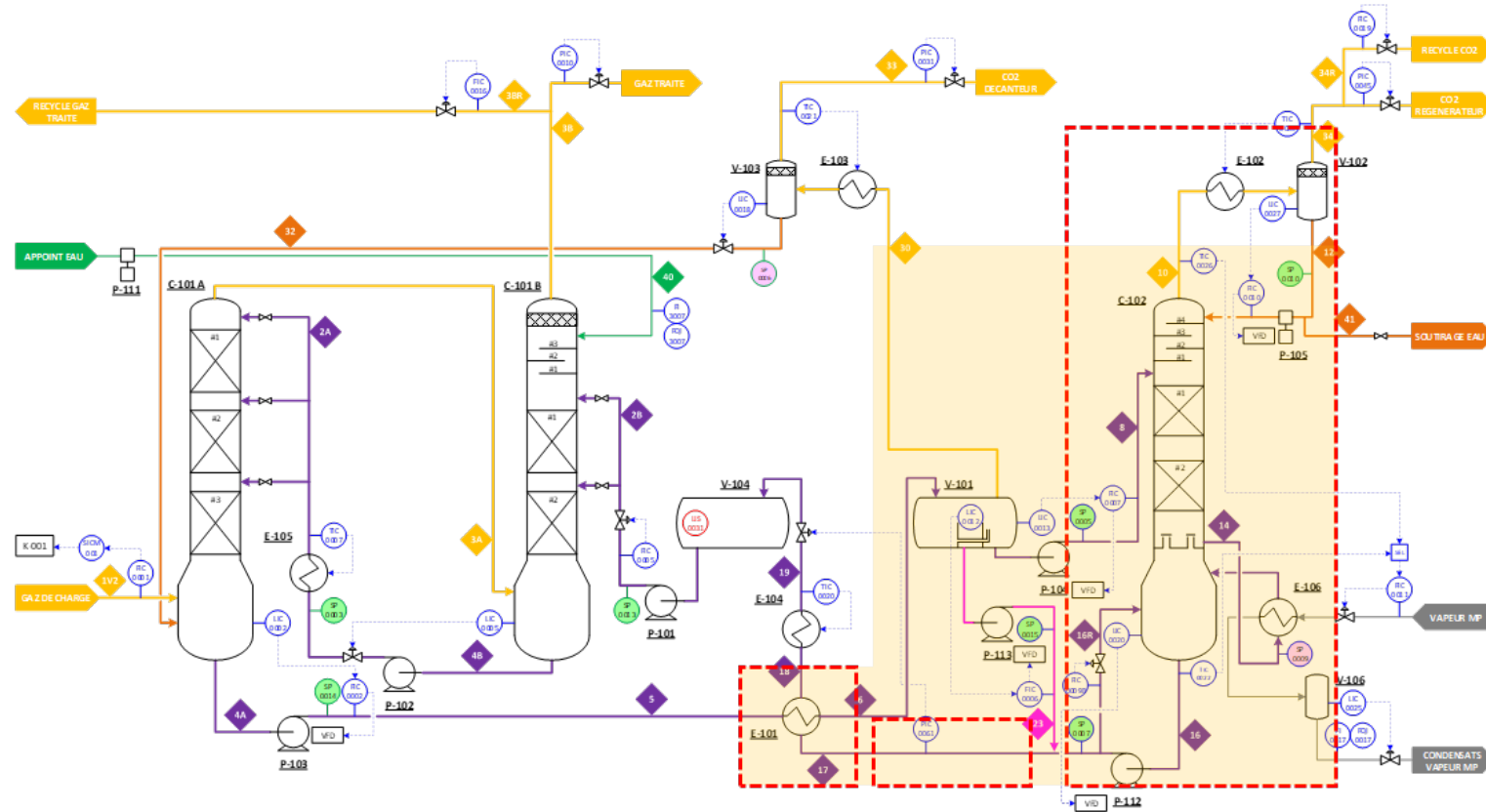
# RECONCILING MASS BALANCE DISCREPANCIES (2/2)

- ❑ Relatively good quality of operation with an average relative uncertainty of  $\pm 7\%$  of the CO<sub>2</sub> capacity (below 5% for the test-runs operated above the turndown capacity)
- ❑ For test-runs with high uncertainty ( $>10\%$ ), an average reconciled capacity leads to better agreement with experimental measures from liquid analyses



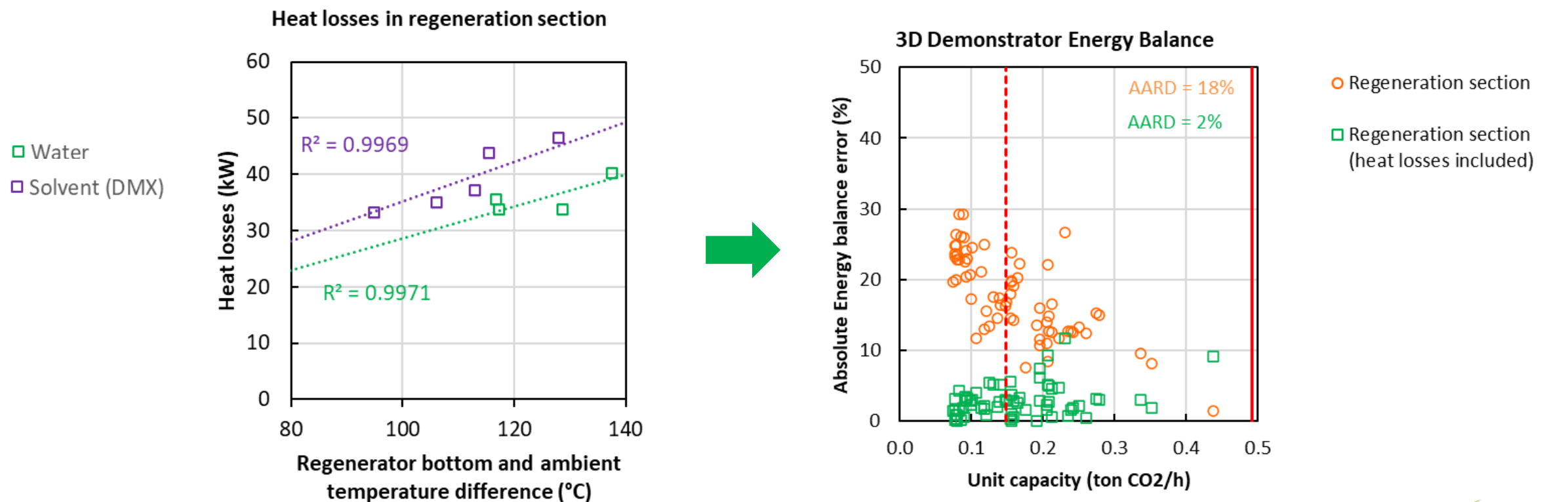
# RECONCILING ENERGY BALANCE DISCREPANCIES (1/2)

- ❑ Specific campaigns for heat loss accounting were performed without gas circulation and for DMX solvent and water, to avoid uncertainties related to CO<sub>2</sub> (mass balances, thermodynamics...)
- ❑ Only heat balances around the regeneration section were performed (highest temperatures of the demonstrator)



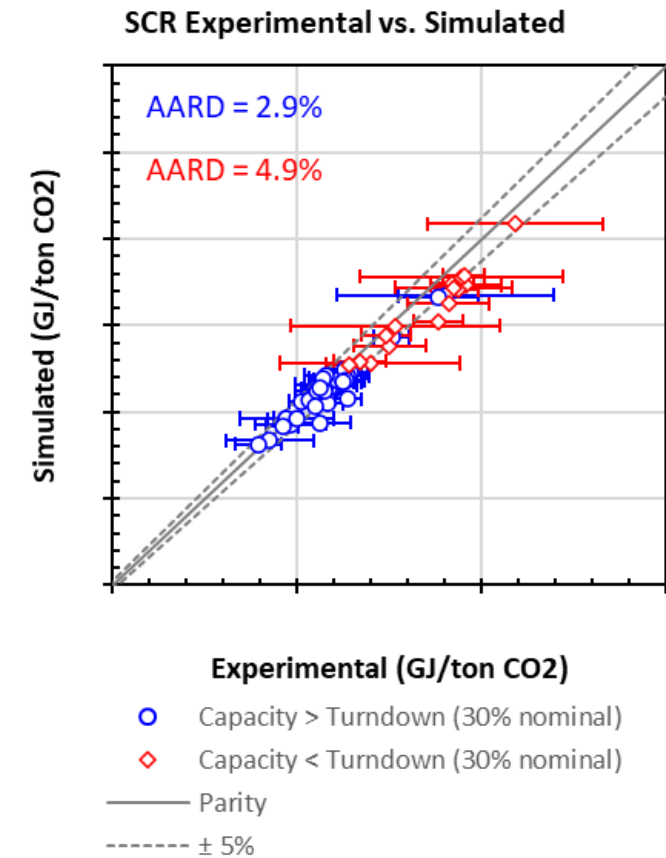
# RECONCILING ENERGY BALANCE DISCREPANCIES (2/2)

- Results of both campaigns were consistent. The outcome from water campaign was prioritized to avoid any uncertainty related to the thermodynamic model of the DMX solvent.
- Accounting for thermal losses reduces heat balance uncertainty from 18 % to 2 % overall
- Mass balance reconciliation has a small influence on energy balance



# SIMULATOR PREDICTION OF 3D DEMONSTRATOR DATA

- ❑ Simulations with in-house model led to good agreement with experience in overall
  - ❑ Very good agreement for TR with low uncertainty ( $\pm 3\%$ ), demonstrating the high performance of the simulator
  - ❑ Good agreement for TR with high uncertainty ( $\pm 5\%$ ), supports the consistency of the selected reconciliation strategy



# CONCLUSIONS

- ❑ DMX technology for low CO<sub>2</sub> content emitters has been validated
- ❑ Uncertainties of mass and heat flows for the 2024 campaign at 3D were identified and quantified:
  - ❑ The most preponderant source of uncertainty was to operate below 10 % of full scale of one of the CO<sub>2</sub> gas flowmeters.
  - ❑ Overall relative uncertainty of  $\pm 7$  % of the CO<sub>2</sub> capacity (below  $\pm 5$ % for the TR operated above the turndown capacity, 30% nominal)
  - ❑ It is not very misleading to consider an uncertainty of 5 to 10% on the energy penalty for the 3D operation
- ❑ The high confidence we have on the 3D experimental data relies on :
  - ❑ Reconciliation offers good agreement with liquid analysis
  - ❑ Good prediction by in-house simulator
- ❑ Take away messages :
  - ❑ Reconciling mass balances is a relevant step to evaluate the experimental data consistency
  - ❑ When varying the operating CO<sub>2</sub> capacity...
    - ❑ Do not forget flowmeters metrology !
    - ❑ Do not underestimate thermal losses !

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