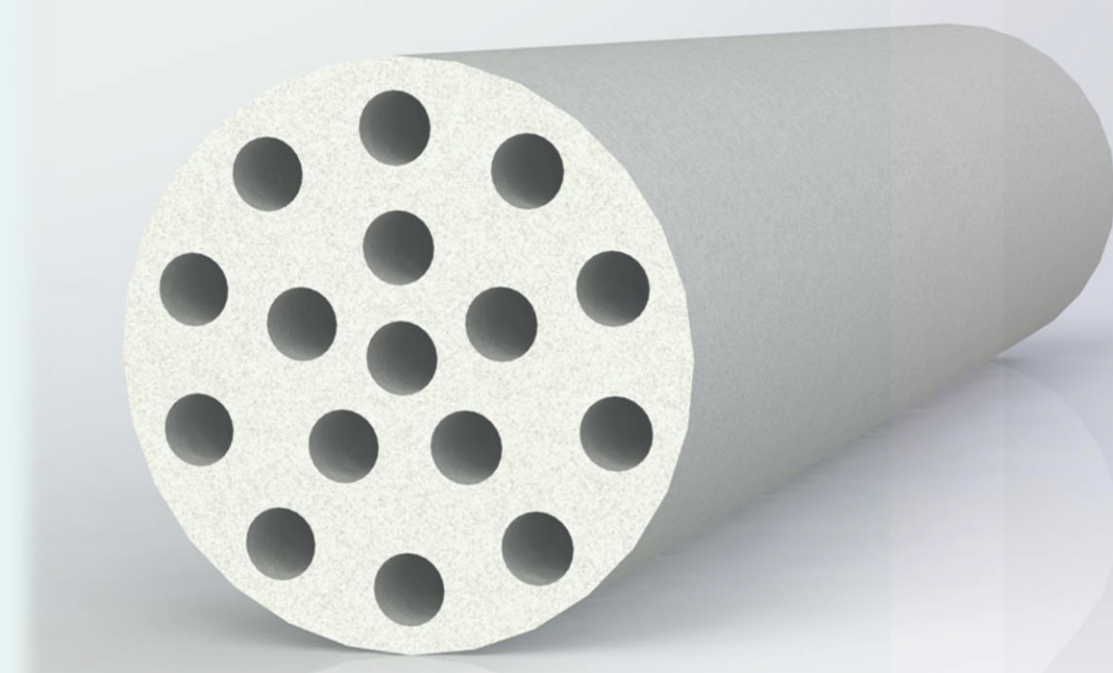


How does structured adsorbent channel heterogeneity influence the efficiency of adsorptive CO₂ capture?

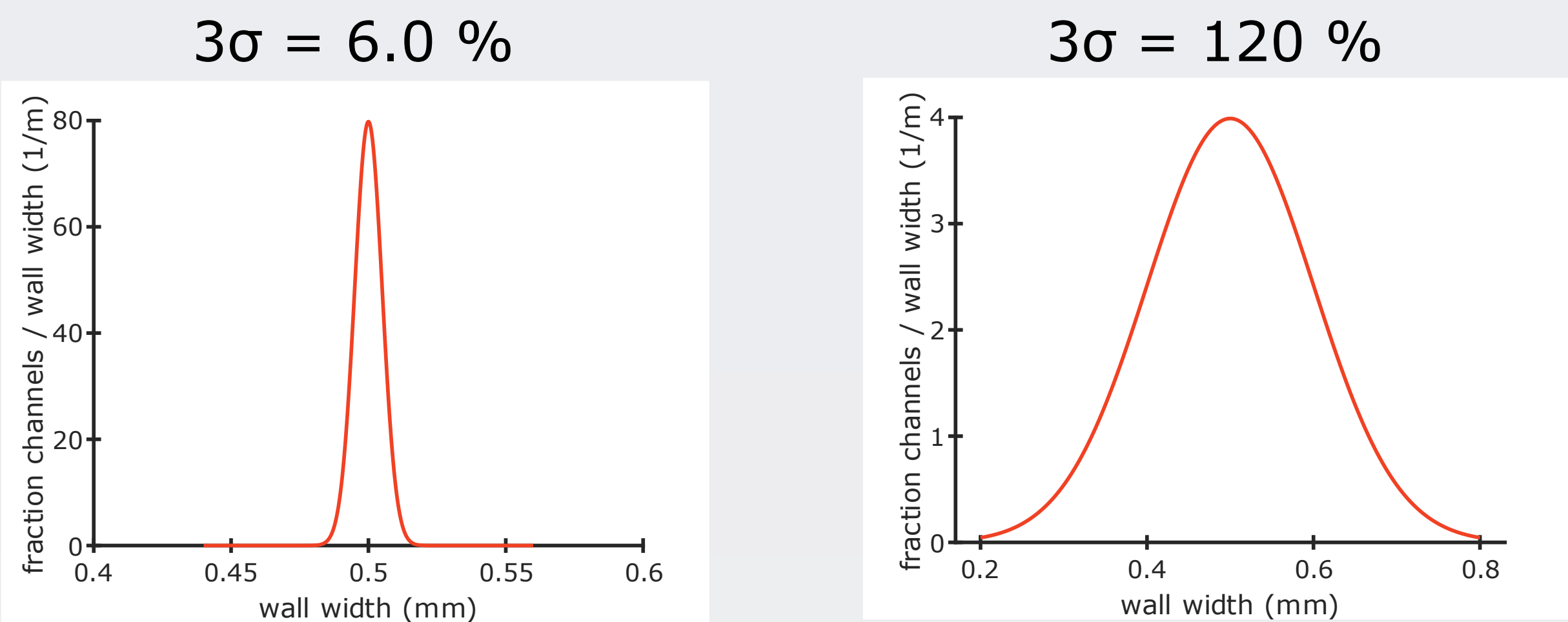
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Adsorbent Monoliths are Heterogeneous

Adsorbent monoliths are often used in carbon capture applications, due to their favorable pressure drop and mass transfer characteristics. Monoliths are often imperfect: they contain a distribution of channels, due to defects in the die, inhomogeneous drying or variations in the deposition of the active coating layer. Such wall and channel heterogeneity can have a profound impact on breakthrough profiles,¹⁻⁵ since the gas flow in each channel becomes different. The effect on process performance, however, is not well understood. Here we performed a theoretical study of the effect of a wall size distribution in a vacuum swing adsorption cycle for CO₂ capture from a model flue gas (15% CO₂).

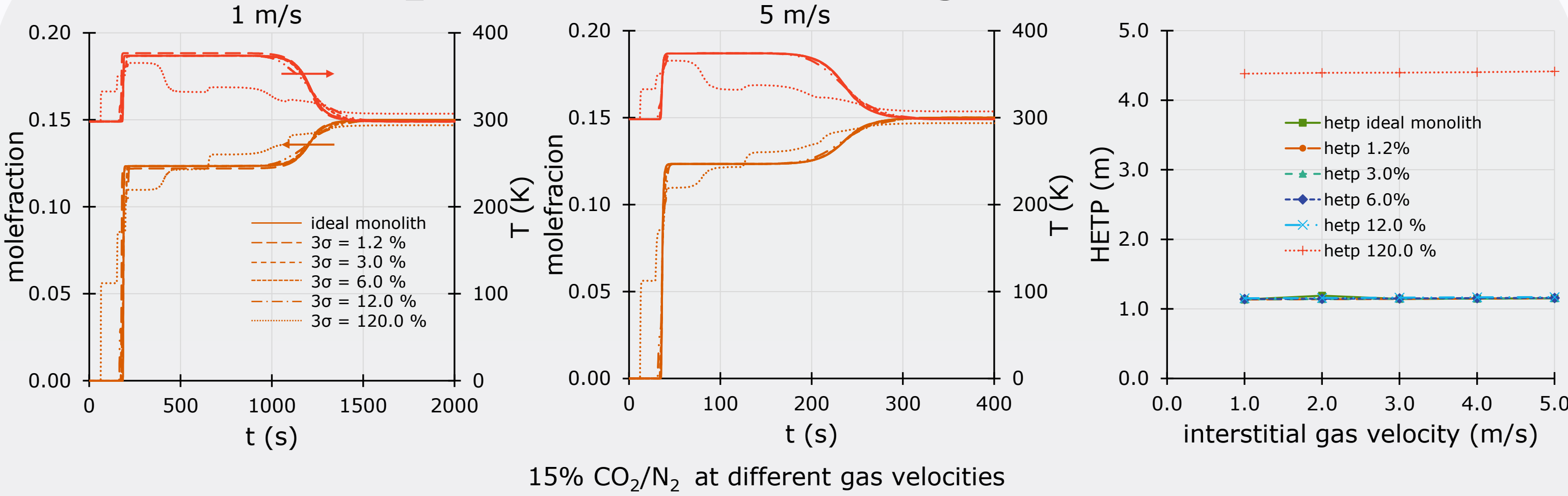


Methodology Incorporating Channel Heterogeneity



A Gaussian distribution of wall sizes was assumed, with standard deviation $3\sigma = 6\%, 12\%, 66\%, 120\%$. Each monolith was cut into 5 channels, with a wall size equal to the average of a 20% part of the distribution. Square channels were assumed.

Impact On Breakthrough Profiles



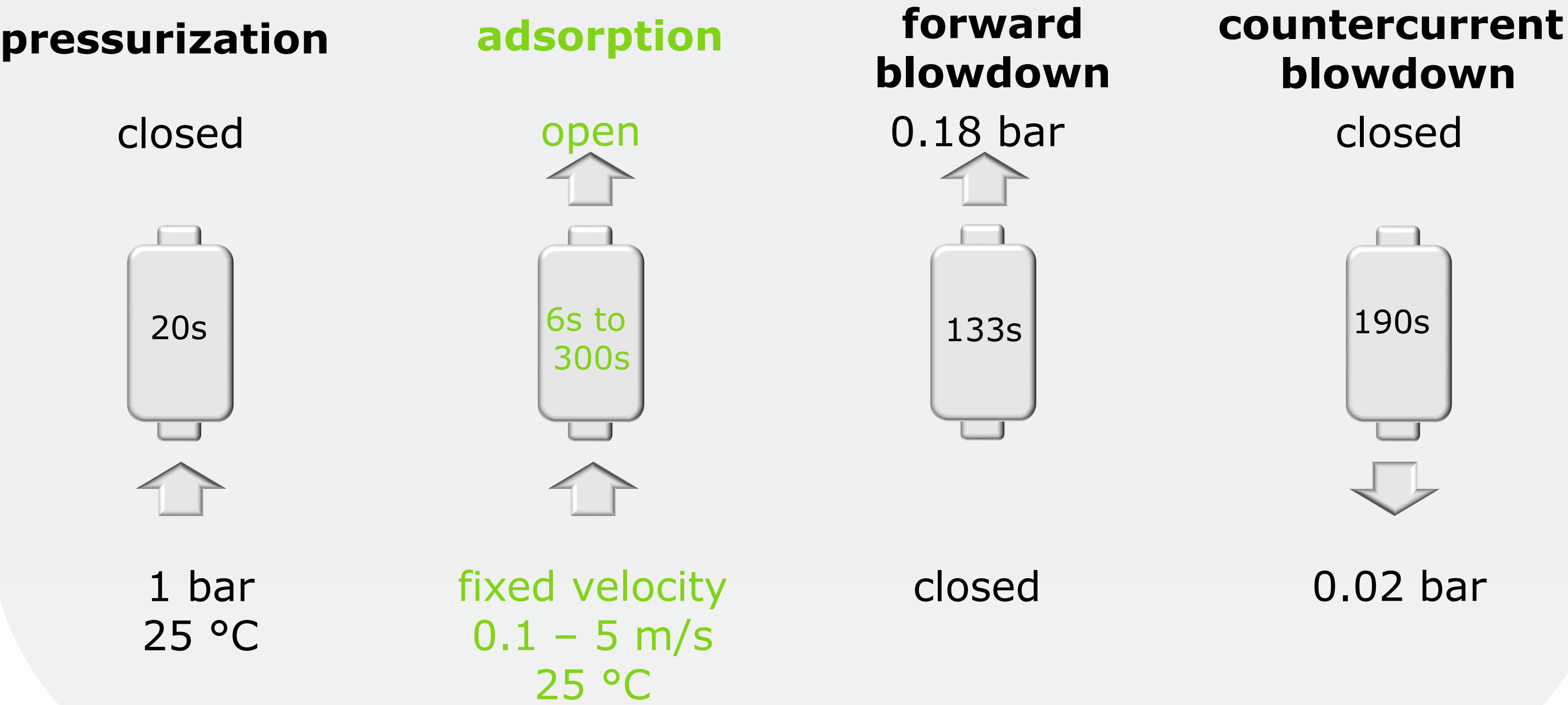
CO₂ breaks through in distinct steps, corresponding to each channel, different waves visible in temperature and concentration. Only small effect of gas velocity in studied ranges. HETP fairly independent of gas velocity.

Methodology Mass & Energy Balances

$$\frac{\partial(y_i)}{\partial t} = -\frac{(1-\epsilon)}{\epsilon} \frac{\rho_p}{\rho_f} \frac{\partial q_i}{\partial t} - \frac{1}{\rho_f} \frac{\partial(u \rho_f y_i)}{\partial x} \Big|_x + \frac{D_{ax}}{\rho_f} \frac{\partial \rho_f}{\partial x} \frac{\partial y_i}{\partial x} \Big|_x - \frac{y_i}{\rho_f} \frac{\partial(\rho_f)}{\partial t} \quad \text{component mass balance}$$
$$\frac{\partial \rho_f}{\partial t} = -\frac{(1-\epsilon)}{\epsilon} \rho_p \sum_{i=1}^{n_c} \frac{\partial q_i}{\partial t} - \frac{\partial(\rho_f u)}{\partial x} \Big|_x \quad \text{total mass balance}$$
$$\rho_f = \frac{P}{RT_g} \quad \text{ideal gas EOS}$$
$$\frac{\partial(q_i)}{\partial t} = k_{l,f,i} (q_{eq,i} - q_i) \quad \text{linear driving force kinetics}$$
$$\frac{\partial T_g}{\partial t} = -\frac{1}{\rho_f C_v} \frac{\partial(u \rho_f H_g)}{\partial x} - \frac{k_{heat} a' (T_g - T_s)}{\epsilon \rho_f C_v} - \frac{E_g}{\rho_f C_v} \frac{\partial \rho_f}{\partial t} \quad \text{gas phase energy balance}$$
$$\frac{\partial T_s}{\partial t} = \frac{k_{heat} a' (T_g - T_s)}{C_{v,s} \rho_p (1-\epsilon)} + \frac{1}{C_{v,s}} \sum_{i=1}^{n_c} \Delta H_i \frac{\partial q_i}{\partial t} \quad \text{solid phase energy balance}$$

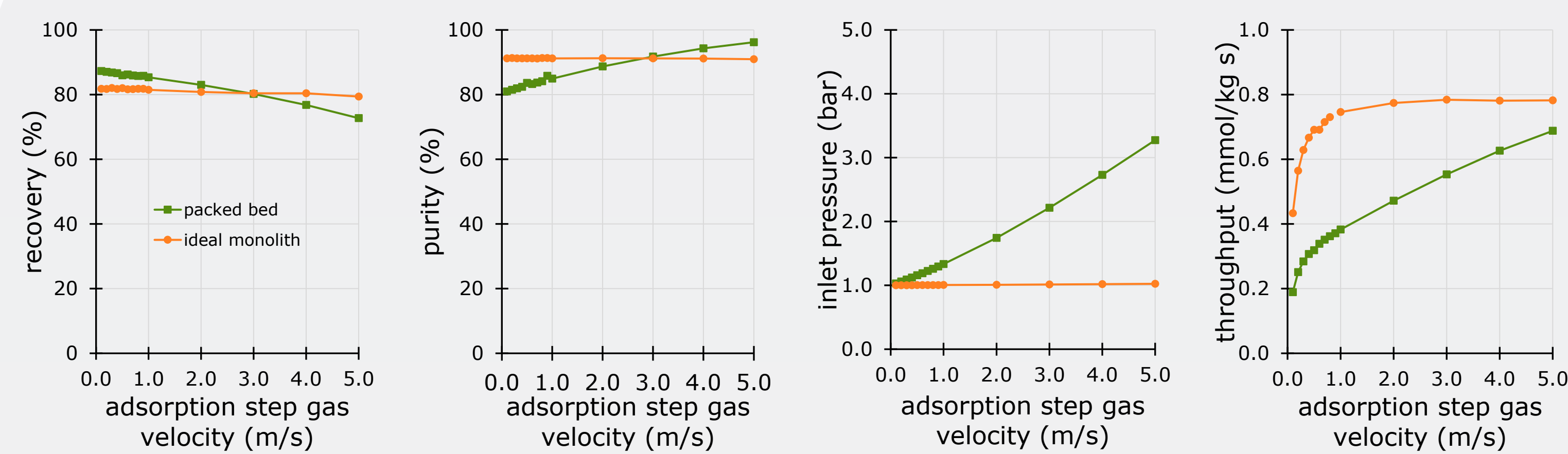
With parameters for zeolite 13X from the work of Wilkins *et al.*⁶ and Brandani *et al.*⁷ Solved using an *in-house* developed process simulator in MATLAB.

Methodology VSA cycle



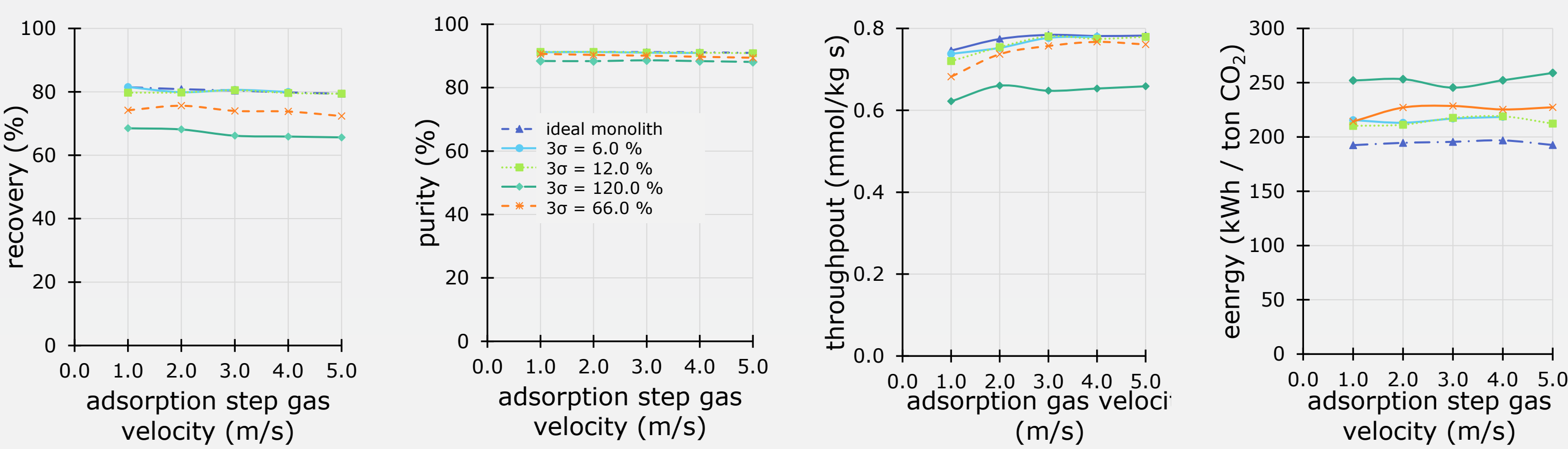
Cycle parameters from the work of Farooq.⁸

Ideal Monolith vs Fixed Bed



With a monolith, less dependence on gas velocity, higher productivity. Higher recovery & purity for a fixed bed is due to increase in pressure, increasing adsorbed amount. Energy demand lies much lower for a monolith (190 kWh/ton) vs a fixed bed (320 kWh/ton).

Ideal Monolith vs Imperfect System



All performance parameters decrease with broader distribution. Decrease in purity due to the larger amount of N₂ entrained in larger channels. Decrease in recovery and productivity due to the more difficult desorption of CO₂ from the smallest walls.

Conclusions

Using a monolith allows for a higher productivity (0.78 mmol/kg s) compared to a fixed bed (0.68 mmol/kg s) and a lower energy demand (190 kWh/ton CO₂ versus 320 kWh/ton CO₂). When the monolith contains a distribution of wall sizes, the process performance decreases. The recovery drops from 81% to 68%, the throughput drops from 0.78 mmol/kg s to 0.65 mmol/kg s and the energy demand increases from 190 kWh/ton CO₂ to 251 kWh/ton CO₂ for the widest distribution. Large defects can thus severely impact performance.



Claessens, B. How Does Structured Adsorbent Channel Heterogeneity Influence the Efficiency of Adsorptive CO₂ Capture? *Chemical Engineering Science* **2025**, 302, 120917. <https://doi.org/10.1016/j.ces.2024.120917>.