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350

Modelling CO₂ capture with AMP in NMP

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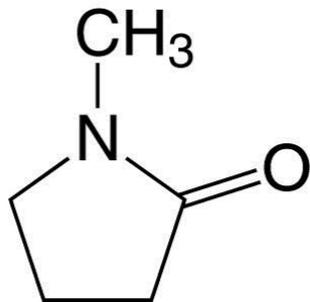


Outline

- Background of our research
- Model
 - Work so far / Shortcomings / Proposed improvements
- Remaining properties
 - Gaps: data in aqueous medium (literature)
 - Gaps: data in NMP medium (experimental)
 - Properties of precipitate
 - Properties of transfer
- Future work

The system

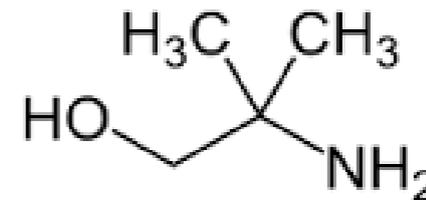
Solvent:



NMP

(N-methyl-2-pyrrolidone)

Amine:

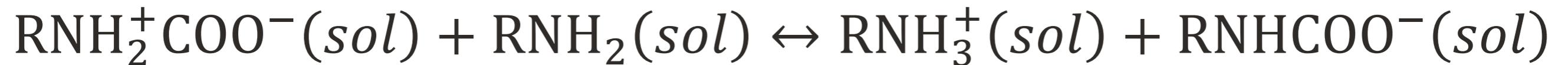


AMP

(2-amino-2-methyl-1-propanol)

*Note: AMP is
sterically hindered*

Reaction mechanism



Model: What we want to do?

- Predict the lean and rich stream loading
- Energy requirements for the plant
- Test different plant configurations

Model vs experimental

Energy requirement (25w% AMP in NMP)

Model	Experiment
8.1 GJ/ton CO ₂	14.4 GJ/ton CO ₂
1.01 bar a T _{abs} =50 °C T _{reg} =75 °C	7 bar a T _{abs} =45 °C T _{reg} =75 °C
No crystallisation	Crystallisation Heating of the reactor

Total pressure at 85 °C, AMP in NMP

Solution	Model (bar a)	Experiment (bar a)*
15w% AMP in NMP	0.022	0.037
25w% AMP in NMP	0.025	0.075

* "Regeneration of Non-Aqueous Precipitating Amine Solvents"
by Hanna K. Karlsson at PCCC-4, Birmingham, Alabama

Assumed binary NRTL
parameters

Outlet of regeneration

	Unit	Model
Temperature	°C	85
Pressure	bar a	2.52
H ₂ O	kmol/hr	1.00E-10
CO ₂	kmol/hr	0.014465
AMP	kmol/hr	0.1261
NMP	kmol/hr	0.8586
AMP+COO ⁻	kmol/hr	1.73E-34
AMP ⁺	kmol/hr	0.0211
AMPCOO ⁻	kmol/hr	0.0211
SOLID	kmol/hr	0

Inlet:
15w% AMP in NMP
CO₂ loading=0.2

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Species in the liquid phase
(about 60 mole% CO₂)

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SOLID	kmol/hr	0

Inlet:
15w% AMP in NMP
CO₂ loading=0.2

Experiment:
At the same conditions,
the solution has much
lower CO₂*

Species in the liquid phase
(about 60 mole% CO₂)

* "Regeneration of Non-Aqueous
Precipitating Amine Solvents" by Hanna K.
Karlsson at PCCC-4, Birmingham, Alabama

Approximations

- Dielectric constant of NMP is constant with temperature
- Properties of $\text{RNH}_2^+\text{COO}^-(aq) \approx \text{H}^+\text{PZCOO}^-(aq)$, $\text{RNHCOO}^-(aq) \approx \text{PZCOO}^-(aq)$
- Binary NRTL parameters approximated
- Henry constant for CO_2 in AMP assumed same as CO_2 in NMP
- No solid or ternary data
- Approximated infinite dilution heat capacity of the ions for our system

Improvements

Property	Method
Heat of vaporization	Vapor pressure of pure solvents
Binary parameters	Vapor pressure of mixtures – loaded and unloaded
Henry's constant	Measured in NMP, will be measured in AMP with N ₂ O
Heat capacity of solid	Measure with solid calorimetry
Molar volume of solid	Density of a whole crystal

What would still be missing?

- Properties of $\text{RNH}_2^+ \text{COO}^-$, RNHCOO^-
- Properties of the precipitate
- Dielectric constant of NMP with temperature
- Ternary data
- Infinite dilution heat capacity of the ions for our system

Simplifications



Assumptions:

- Zwitterion concentration and impact is negligible
- The precipitate completely dissociates to ions
- Single solid phase

Pure component properties (aq)



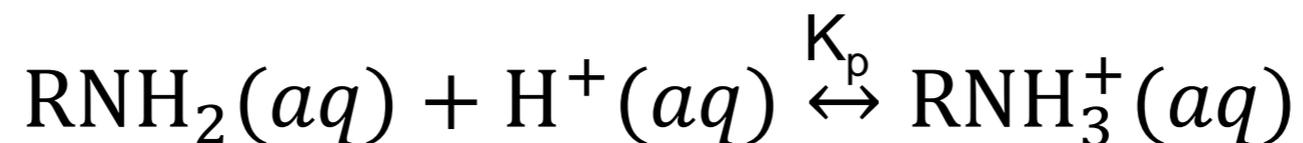
Pure component properties (aq)

Pure component
data available



Pure component properties (aq)

Pure component
data available

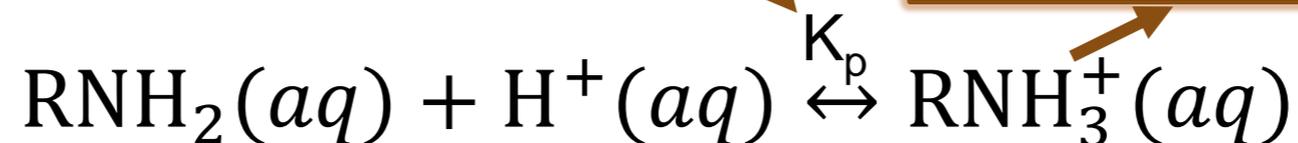


Pure component properties (aq)

Pure component
data available

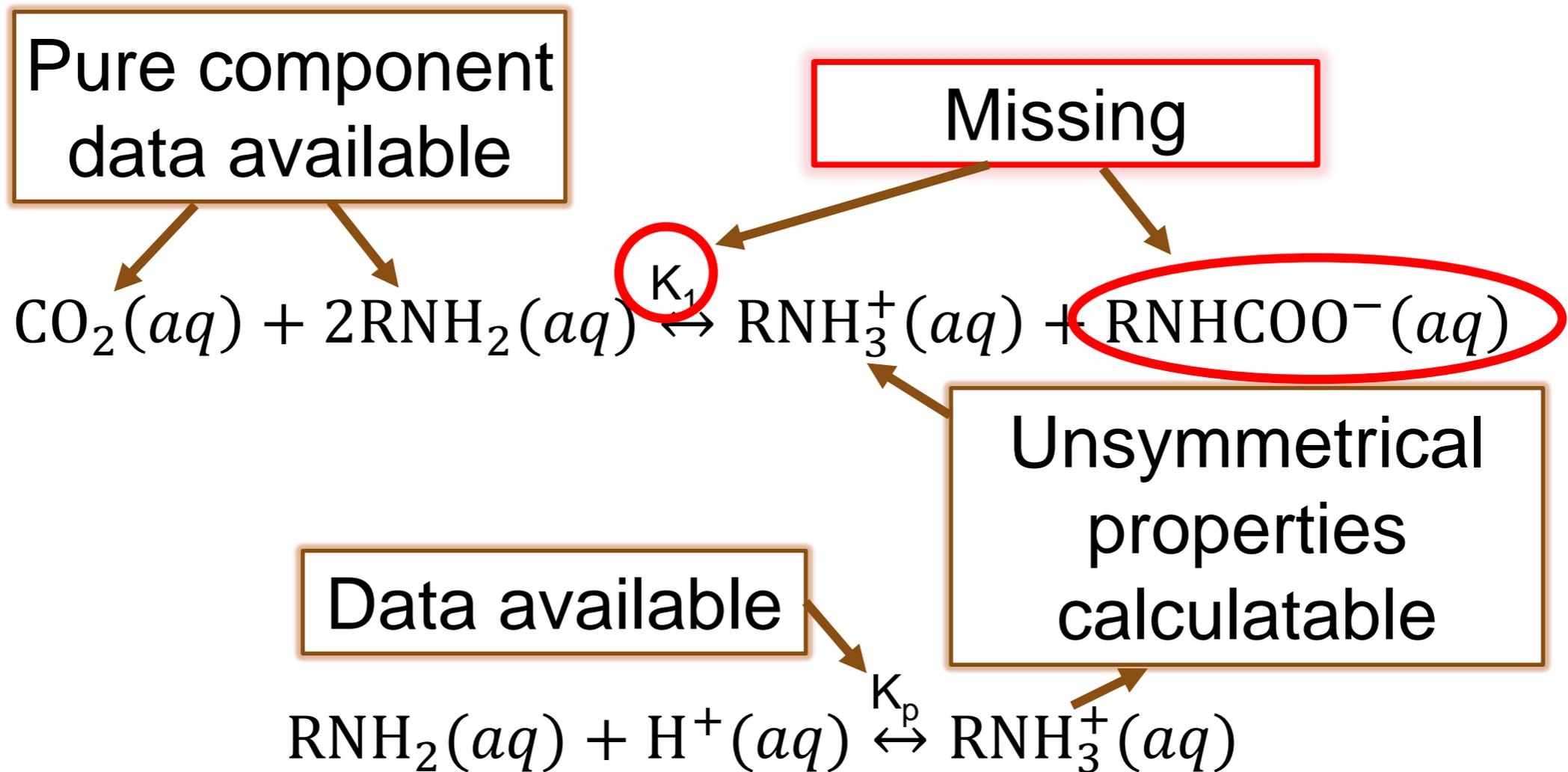


Data available

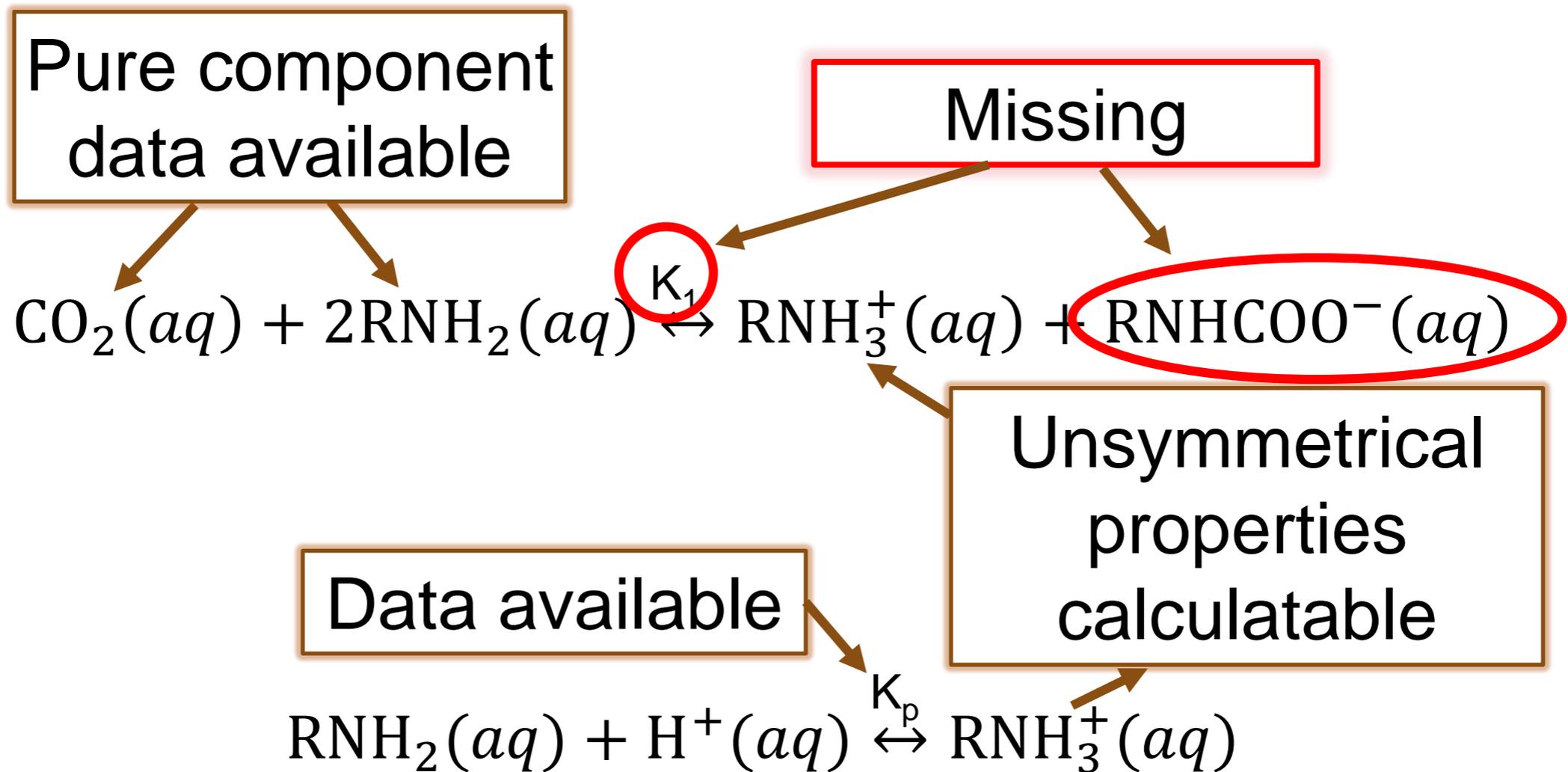


Unsymmetrical
properties
calculatable

Pure component properties (aq)

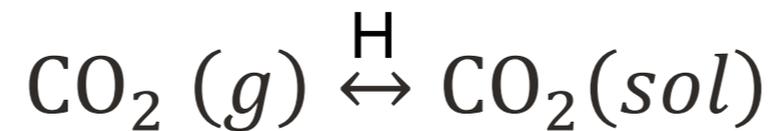


Pure component properties (aq)



Note: aqueous medium

Pure component properties (NMP)



$$\Delta H_r = \Delta H_{\text{CO}_2} + \Delta H_{r1}$$

Experiments: without
precipitation

Pure component properties (NMP)

Without precipitation

Measured separately



Measured

$$\Delta H_r = \Delta H_{\text{CO}_2} + \Delta H_{r1}$$

Pure component properties (NMP)

Without precipitation

Measured separately



Measured

$$\Delta H_r = \Delta H_{\text{CO}_2} + \Delta H_{r1}$$

Calculatable

Pure component properties (NMP)

Without precipitation

Measured separately



Measured

$$\Delta H_r = \Delta H_{\text{CO}_2} + \Delta H_{r1}$$

Calculatable

$$\frac{d \ln K_1}{dT} = \frac{\Delta H_{r1}}{RT^2} \text{ at constant pressure}$$

Properties of
 RNHCOO^- (NMP)

Missing: $\ln K_1$ at any T

Properties of CO_2 ,
 RNH_2 , RNH_3^+ in NMP

Pure component properties (NMP)

Without precipitation

Measured separately



Measured

$$\Delta H_r = \Delta H_{\text{CO}_2} + \Delta H_{r1}$$

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Properties of
 RNHCOO^- (NMP)

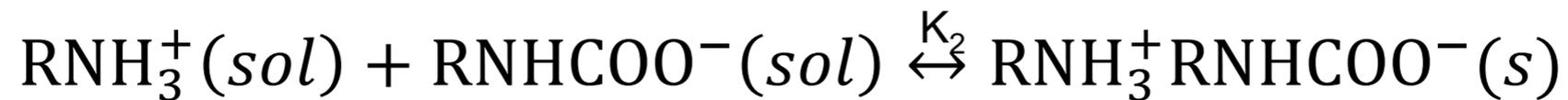
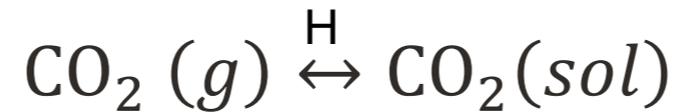
Properties of CO_2 ,
 RNH_2 , RNH_3^+ in NMP

Assumptions:

$\text{CO}_2(sol)$ in the solution is same as in the absence of AMP

$\text{CO}_2(sol)$ in AMP will be measured

Properties of the solid

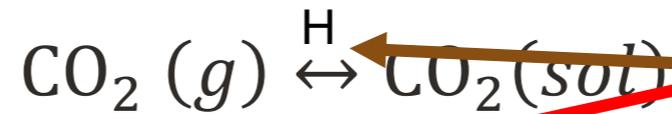


$$\Delta H_r = \Delta H_{\text{CO}_2} + \Delta H_{r1} + \Delta H_{r2}$$

Experiments with
precipitation

Properties of the solid

With precipitation



Measured separately



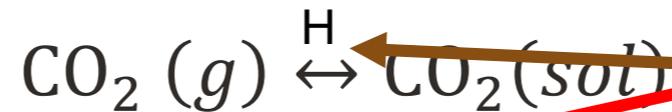
Measured

$$\Delta H_r = \Delta H_{\text{CO}_2} + \Delta H_{r1} + \Delta H_{r2}$$

Calculatable

Properties of the solid

With precipitation



Measured separately



Measured

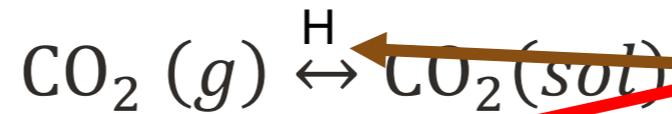
$$\Delta H_r = \Delta H_{\text{CO}_2} + \Delta H_{r1} + \Delta H_{r2}$$

Calculatable

$$\frac{d \ln K_2}{dT} = \frac{\Delta H_{r2}}{RT^2} \text{ at constant pressure}$$

Properties of the solid

With precipitation



Measured separately



Measured

$$\Delta H_r = \Delta H_{\text{CO}_2} + \Delta H_{r1} + \Delta H_{r2}$$

Calculatable

Missing: $\ln K_2$ at any T

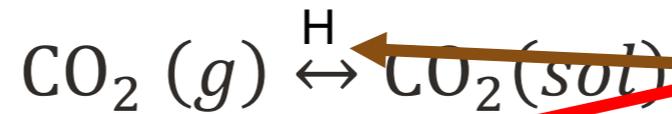
$$\frac{d \ln K_2}{dT} = \frac{\Delta H_{r2}}{RT^2} \text{ at constant pressure}$$

Properties of
 RNH_3^+ , RNHCOO^- in NMP

Properties of
 $\text{RNH}_3^+\text{RNHCOO}^-(s)$

Properties of the solid

With precipitation



Measured separately



Measured

$$\Delta H_r = \Delta H_{\text{CO}_2} + \Delta H_{r1} + \Delta H_{r2}$$

Calculatable

Missing: $\ln K_2$ at any T

$$\frac{d \ln K_2}{dT} = \frac{\Delta H_{r2}}{RT^2} \text{ at constant pressure}$$

Properties of
 RNH_3^+ , RNHCOO^- in NMP

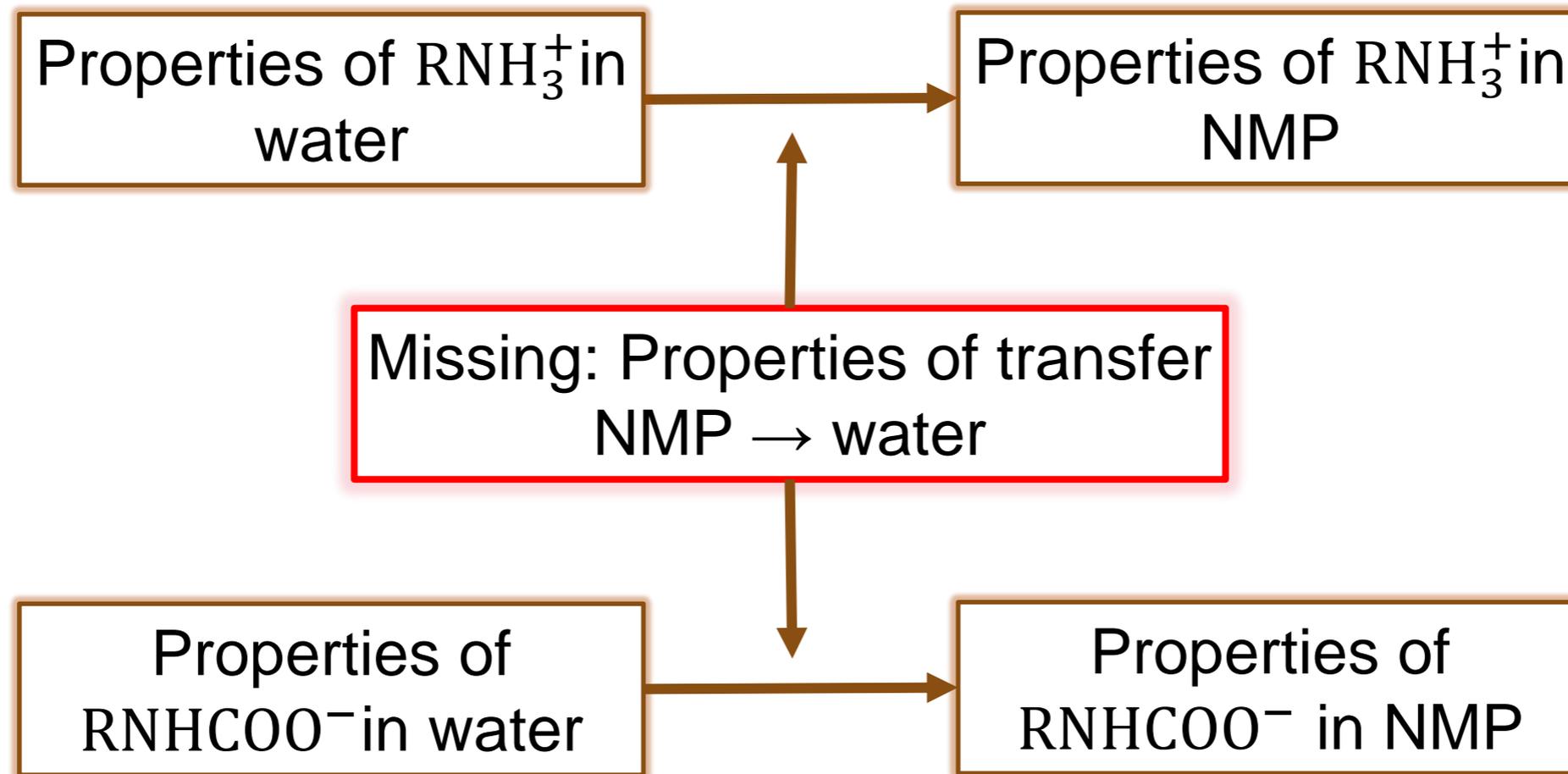
Properties of
 $\text{RNH}_3^+\text{RNHCOO}^-(s)$

Note: AMP-NMP heat of mixing not in heat of reaction

Summary of missing properties

- Properties of transfer
- $\ln K_2$ at any T
- $\ln K_1$ at any T

Properties of transfer



Aspen plus requires
properties in water

Evaluation of
experimental data needs
properties in NMP

Properties of CO₂ and AMP in NMP

- Directly measured
- CO₂ in NMP: Using Henry's constants & enthalpy for CO₂ physical absorption
- AMP in NMP: Enthalpy of mixing & vapor pressure of mixtures

How to get Properties of transfer

Molality scale

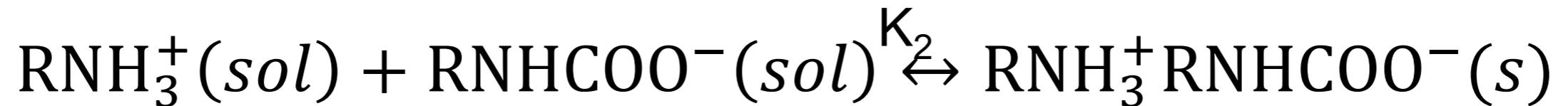
$$\ln \gamma_{i,t}^m \equiv \frac{\mu_{i,NMP}^m - \mu_{i,water}^m}{RT}$$

Solute i Transfer

Transfer properties of the salt

- Solubility product
- Properties of ions separately and then combine
- Born equation

How to get properties of transfer?



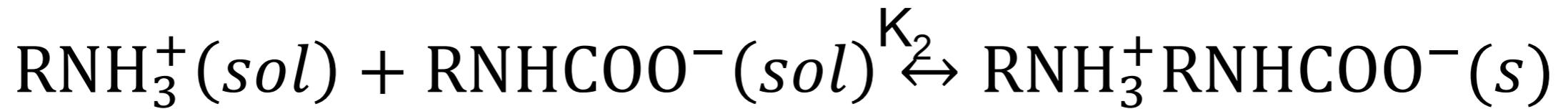
$$\ln \gamma_{\pm,t}^m = \ln \frac{K_{2,\text{water}}}{K_{2,\text{NMP}}}$$



Transfer properties of the salt

- Solubility product
- Properties of ions separately and then combine
- Born equation

How to get properties of transfer?



$$\ln \gamma_{\pm,t}^m = \ln \frac{K_{2,\text{water}}}{K_{2,\text{NMP}}}$$

In water, the salt forms
bicarbonate!

Transfer properties of the salt

- Solubility product
- Properties of ions separately and then combine
- Born equation

How to get Properties of transfer

Not enough data

Transfer properties of the salt

- Solubility product
- Properties of ions separately and then combine
- Born equation

How to get Properties of transfer

$$\ln \gamma_{\pm,t}^* = \frac{q^2}{2} \left\{ \left(\frac{1}{R_{c2}D_2} - \frac{1}{R_{c1}D_1} \right) + \left(\frac{1}{R_{c1}} - \frac{1}{R_{c2}} \right) \right\}$$

Radius of cavity

Dielectric constant

Transfer properties of the salt

- Solubility product
- Properties of ions separately and then combine
- Born equation

“Reevaluation of the Born model of ion hydration” by
Rashin and Honig *J. Phys. Chem.*, 1985, 89 (26), pp 5588–5593

How to get Properties of transfer

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Radius of cavity

Dielectric constant

Missing

Measurable

Transfer properties of the salt

- Solubility product
- Properties of ions separately and then combine
- Born equation

“Reevaluation of the Born model of ion hydration” by
Rashin and Honig *J. Phys. Chem.*, 1985, 89 (26), pp 5588–5593

Missing data

- Measuring or estimating radius of cavity
- $\ln K_2$ at any T
- $\ln K_1$ at any T

Future work

- Equilibrium constants at one temperature
- Further studies on estimating radius of cavity
- Experimental determination of the mentioned properties
- Infinite dilution heat capacity of the ions for our system
- Ternary data
- Tweaking binary data to better fit the ternary data
- Accounting for two solid phases
- Using ENRTL-RK or extended-UNIQUAC
- Validation of properties, plant simulation with continuous setup and batch calorimetry



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