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## Design and optimisation of intensified carbon capture for natural gas power plants using rotating packed bed (RPB) technology

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## **Abstract**

The rotating packed bed (RPB) technology offers a transformative solution for enhancing the efficiency and cost-effectiveness of post-combustion carbon capture (PCC) processes[1,2]. By utilizing RPBs as absorbers and strippers, we can significantly reduce the size and footprint of the systems involved. With the ability to operate at monoethanolamine (MEA) concentrations exceeding 55 wt%, RPBs present an opportunity to achieve superior absorption performance while also diminishing the energy demands associated with solvent regeneration [3]. However, despite its promise, the comparative evaluation of multiple RPB absorber-based CO<sub>2</sub> capture process designs (Figure 1) considering several absorber arrangements, exhaust gas recirculation (EGR) for CO<sub>2</sub> enrichment of the incoming flue gas stream and monoethanolamine (MEA) concentrations has not been explored. Furthermore, the optimisation of this multiple RPB absorber-based CO<sub>2</sub> capture process incorporating an intercooling system between absorbers is yet to be reported.

This study presents a rigorous process simulation and optimization of rotating packed bed (RPB) absorbers for post-combustion CO<sub>2</sub> capture (PCC) ) of a natural gas combined cycle (NGCC) power plant. It explores different RPB absorber designs options using 55 wt% and 75 wt% MEA solvent [2]. Four design options (which included Option 1—One RPB absorber with 55 wt% MEA and 75 wt% MEA, Option 2—Two RPB absorbers in parallel with only 75 wt% MEA, Option 3— EGR with One RPB absorber at 75 wt% MEA, and Option 4— EGR with two RPB absorbers in parallel at 75 wt% MEA.

A systematic comparison of the four design options based on footprint (packing volume), energy consumption and pressure drop provides insights into optimal RPB absorber design. The best-performing design (Option 4) significantly reduces absorber size (2–4 times smaller) and achieves a lower pressure drop (8.6 kPa) compared to other options. It also has a moderate rotor energy consumption of 402 kW which is lower than all the other options. Furthermore, incorporating an intercooling system between the absorbers in the best-performing design (Option 4) lowers the liquid phase temperature and facilitate enhanced CO<sub>2</sub> absorption performance by up to 12% compared to designs without intercooling.

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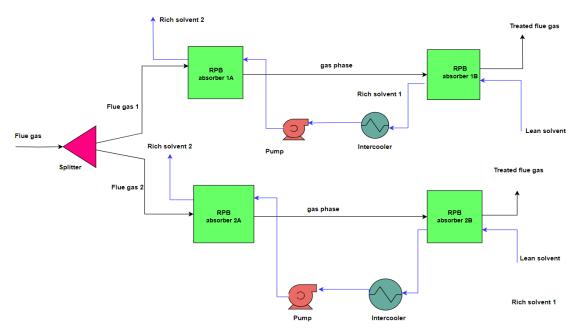


Figure 1: Two trains of RPB absorbers in series with external coolers between the RPB absorbers

An optimisation of the operating parameters to minimise the CO<sub>2</sub> capture cost of the multiple RPB absorbers based CO<sub>2</sub> capture process designs was conducted. Preliminary results indicate that the optimal operating conditions for the RPB absorbers include a rotor speed of 275–300 RPM, which provides the best balance between energy consumption and cost. An optimal liquid-to-gas (L/G) ratio of 0.9–1.0 kg/kg effectively minimizes CO<sub>2</sub> capture expenses while ensuring high efficiency. Furthermore, a strategic reduction in MEA solvent make-up by 10–20% could yield impressive annual savings. This is a striking contrast to the benchmark MEA-based PCC process using packed beds absorption columns, which incurs a much higher cost Our goal is to determine the set of operating parameters that will maximize CO<sub>2</sub> capture efficiency while minimising CO<sub>2</sub> capture costs for the whole RPB-based CO<sub>2</sub> capture process. Employing a multiple RPB absorber designs and cost-focused approach for the RPB-based CO<sub>2</sub> capture process, could bridge the gap between technical performance and economic viability, thus advancing sustainable carbon capture solutions.

Keywords: Post-combustion carbon capture; chemical absorption; rotating packed bed; intercooling system,; Natural Gas power plant; optimisation

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