



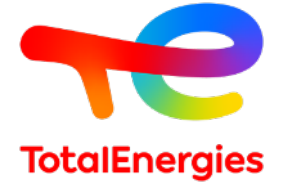
Whole CCU chain 3MWth demo project with detailed NOX measurements



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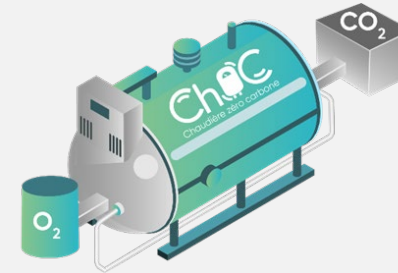
A french decarbonation initiative



• Partners



• Observing members & potential end-users



Ch0C : « Chaudière Oxycombustion bas Carbone »

- Oxycombustion fire-tube boiler
- CO₂ emissions reduction > 90%
- Capacity: 1MW_{th} < P < 25MW_{th}

Objectives

- Design, manufacturing & testing of a 3MW_{th} oxycombustion boiler on an industrial site (Villers-Saint-Paul)

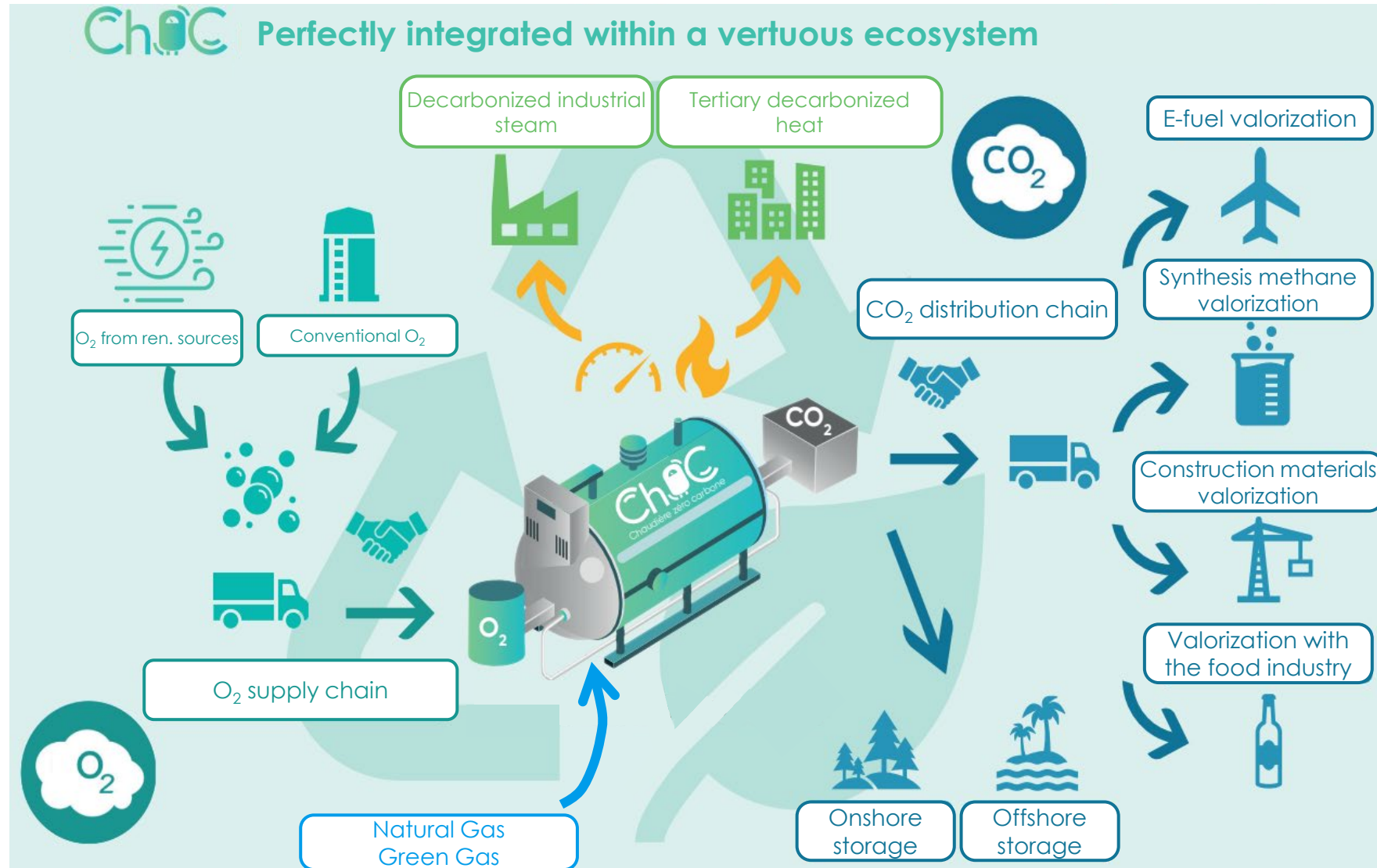
Technical challenges

- Low-NO_x oxyburner
- NO_x in purification unit



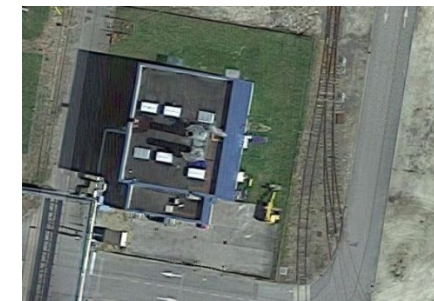
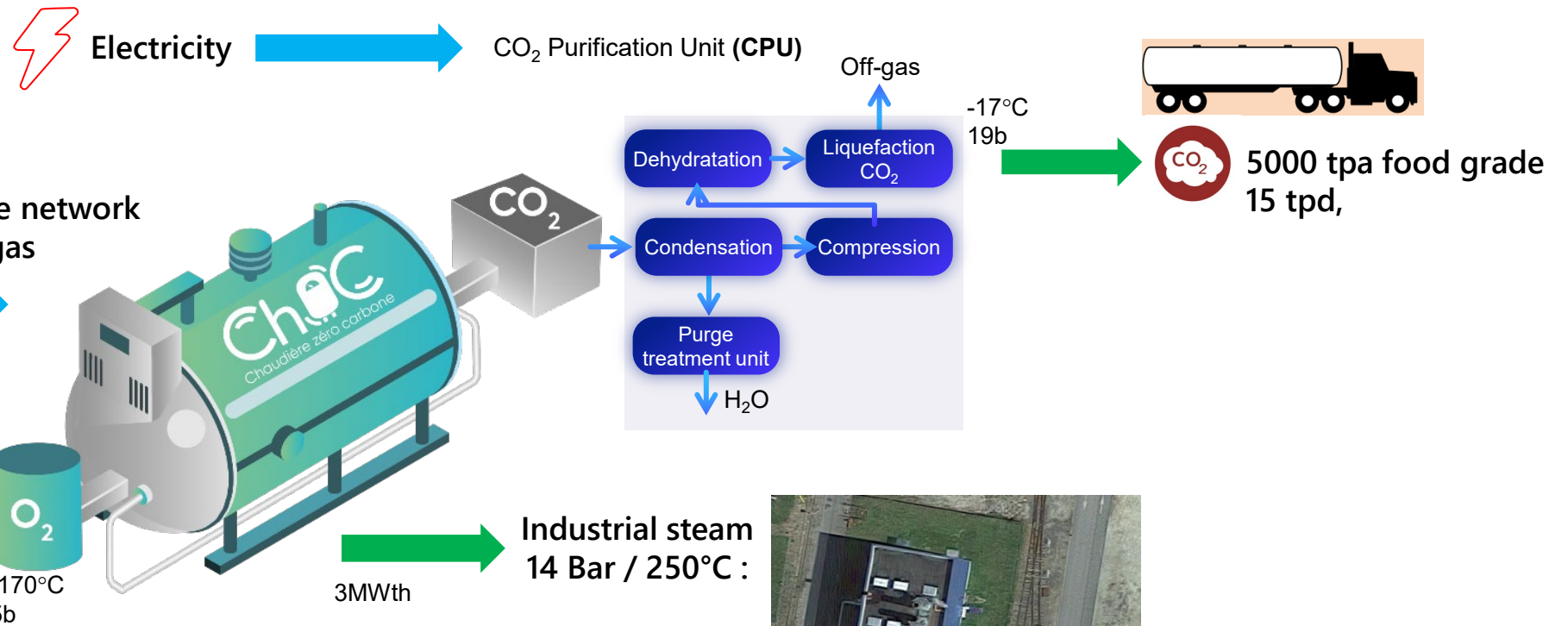


A virtuous ecosystem



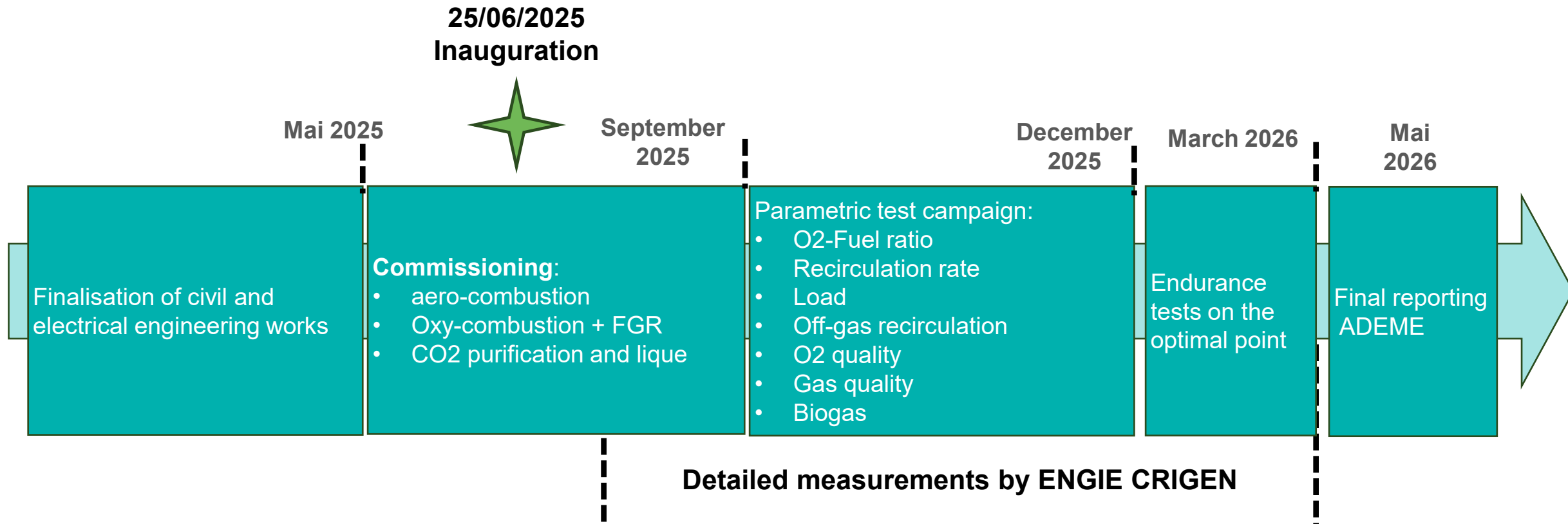


The demonstration project



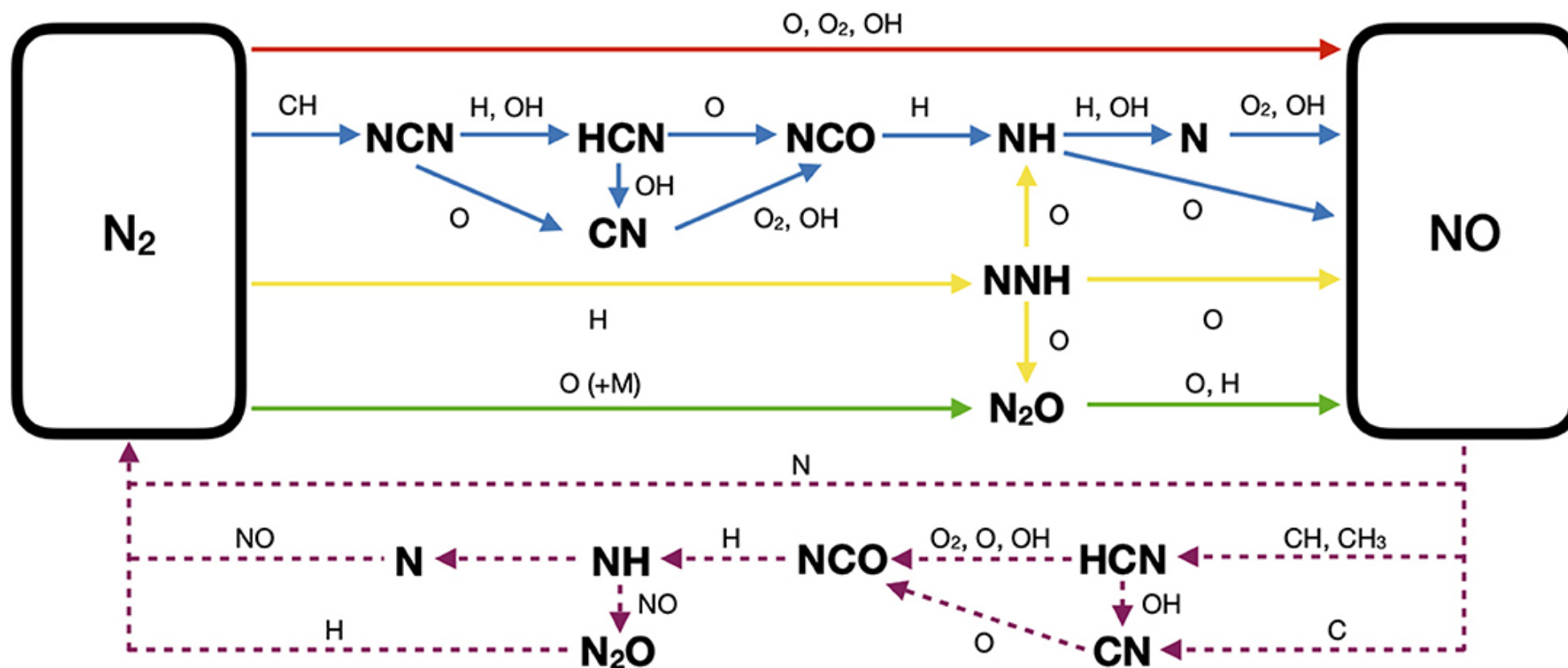


Project progress & planning





NOX complex formation

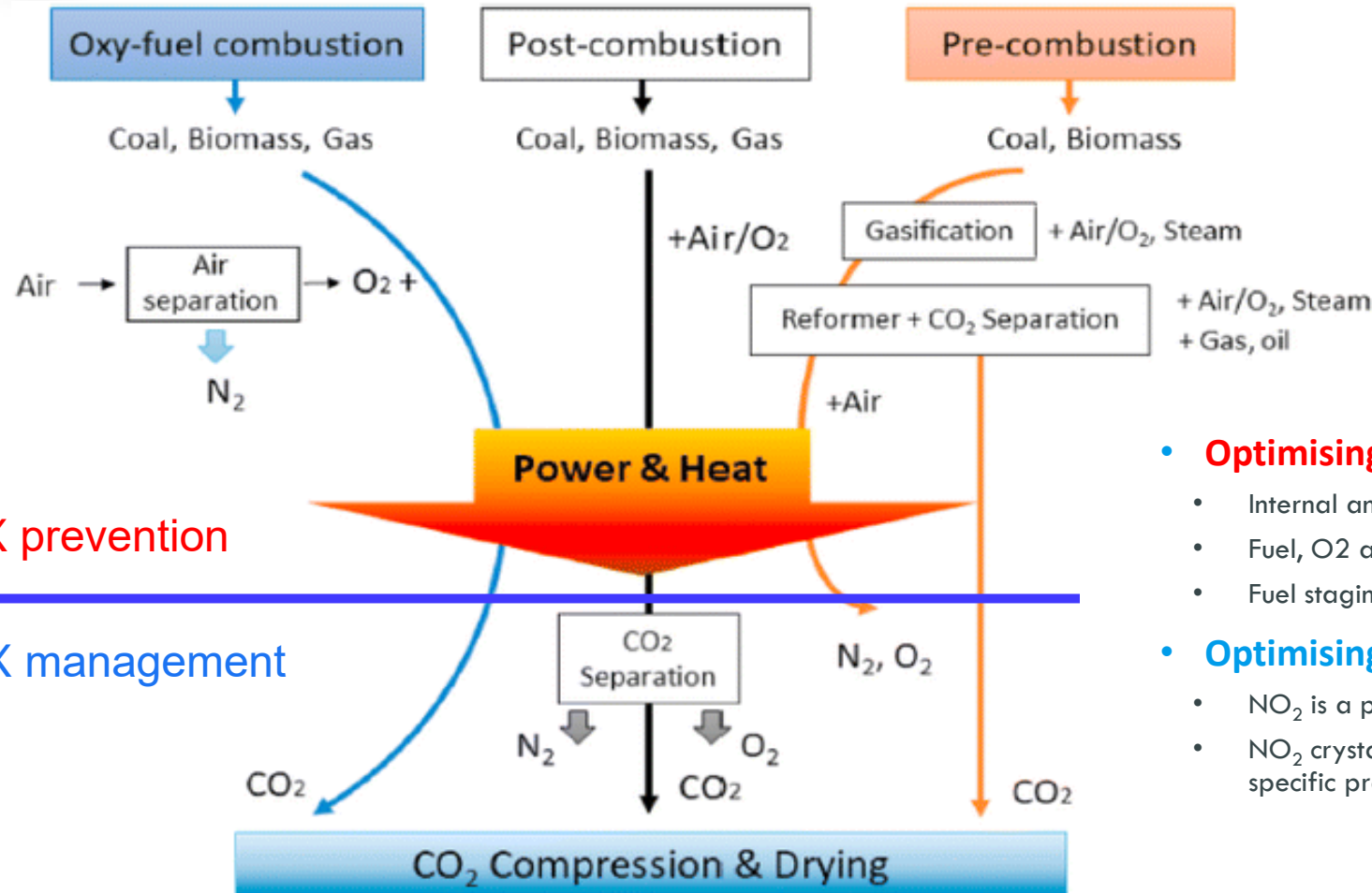


Légende :

- Thermal NOx
- Prompt NOx
- NOx fuel
- N2O intermediate
- Reburning



In all Combustion types



- **Optimising combustion**

- Internal and External recirculation
- Fuel, O₂ and FGR premixing
- Fuel staging

- **Optimising CO₂ capture process**

- NO₂ is a poison for amine and leads to an increase in amine consumption
- NO₂ crystalizes at higher temperature (-11 °C) than CO₂ liquefaction and requires specific pre-treatment for cryogenic CO₂ separation processes

- **Ultra low NO_x requirement for CO₂ transportation and storage**

It corrodes drastically compressors / piping and drastic limitation are given for transportation/storage :

Example: 1.5 ppm NO_x v in Northlight CO₂ capture project.



A challenge for the CCUS value chain



		Nortnen Ligths		
		2022	2024	2025
		Liquide	Liquide	Liquide
CO ₂	%v.		> 99.81	> 99.81
H ₂ O	ppm mol	≤ 30 ppm mol	≤ 30 ppm mol	≤ 30 ppm mol
H ₂	ppm mol	≤ 50	≤ 50	≤ 50
N ₂	ppm mol	-	≤ 50	≤ 50
Ar	ppm mol	-	≤ 100	≤ 100
CH ₄	ppm mol	-	≤ 100	≤ 100
CO	ppm mol	≤ 100	≤ 100	≤ 100
O ₂	ppm mol	≤ 10	≤ 10	≤ 10
H ₂ S	ppm mol	≤ 9	≤ 9	≤ 1
SO _x	ppm mol	≤ 10	≤ 10	≤ 10
NO _x	ppm mol	≤ 10	≤ 1.5	≤ 1.5
NH ₃	ppm mol	10	≤ 10	≤ 10
Amines	ppm mol	≤ 10	≤ 10	≤ 10
Méthanol	ppm mol	-	≤ 30	≤ 30
Ethanol	ppm mol	-	≤ 1	≤ 1
Total VOC	ppm mol	-	≤ 10	≤ 10
Glycol	ppm mol	-	TEG pas acceptable MEG ≤ 0.005 ppm mol	MEG < 0.2 TEG < 0.2
Ethylene	ppm mol		≤ 0.5	≤ 50
Ethane	ppm mol		≤ 75	≤ 75
Aliphatic (C3+)	ppm mol	-	≤ 1100	≤ 1100
BTEX	ppm mol	-	≤ 0.5	≤ 0.5
Total aldéhydes	ppm mol	Formaldehyde ≤ 20 Acetaldehyde ≤ 20	Formaldehyde ≤ 20 Acetaldehyde ≤ 20	Formaldehyde ≤ 20 Acetaldehyde ≤ 20
HCN	ppm mol	-	<100	<100
Hg	ppm mol	≤ 0.03	≤ 0.0003	≤ 0.0003
Cadmium + Thallium	ppm mol	≤ 0.03	moved to solids	-
Particule size	um	-	≤ 1	≤ 1

Food spec.:

▷ TABLEAU 1: CRITÈRES DE CONCENTRATION POUR LA NORME **EIGA** (CO₂ LIQUIDE)

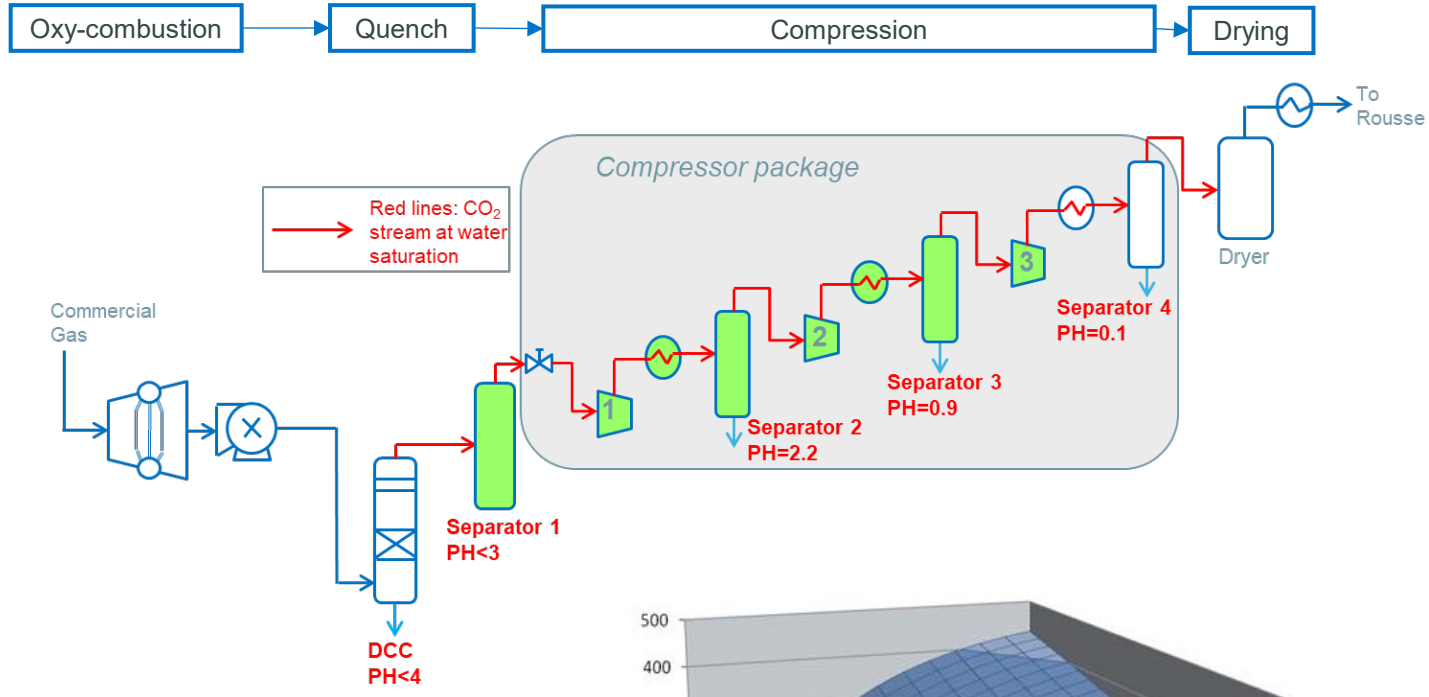
Composé	Concentration
CO ₂	▶ 99.9% v/v min.
Humidité	▶ 20 ppm v/v max
Ammoniac	▶ 2.5 ppm v/v max.
Oxygène	▶ 30 ppm v/v max.
Oxydes d'azote (NO/NO ₂)	▶ 2.5 ppm v/v max. de chaque
Particules	▶ 10 ppm m/m max.
Résidus organiques non volatils (huiles)	▶ 5 ppm m/m max.
Total des hydrocarbures volatils (correspondance méthane)	▶ 50 ppm v/v max. dont 20 ppm v/v max d'hydrocarbures non-méthaniques.
Acétaldéhyde	▶ 0.2 ppm v/v max.
Hydrocarbures aromatiques	▶ 0.02 ppm v/v max.
Monoxyde de carbone	▶ 10 ppm v/v max.
Méthanol	▶ 10 ppm v/v max.

Les critères de la qualité technique (pour usage en froid ou chimie) varient selon les procédés.

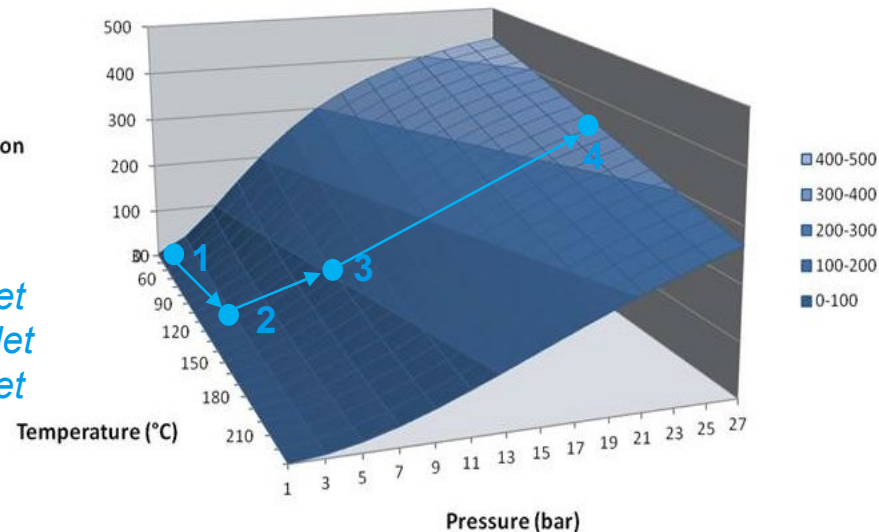
Standardization efforts are underway within CEN/TC 474's WG1 group to establish a European specification for CO₂ quality.



Lacq experience



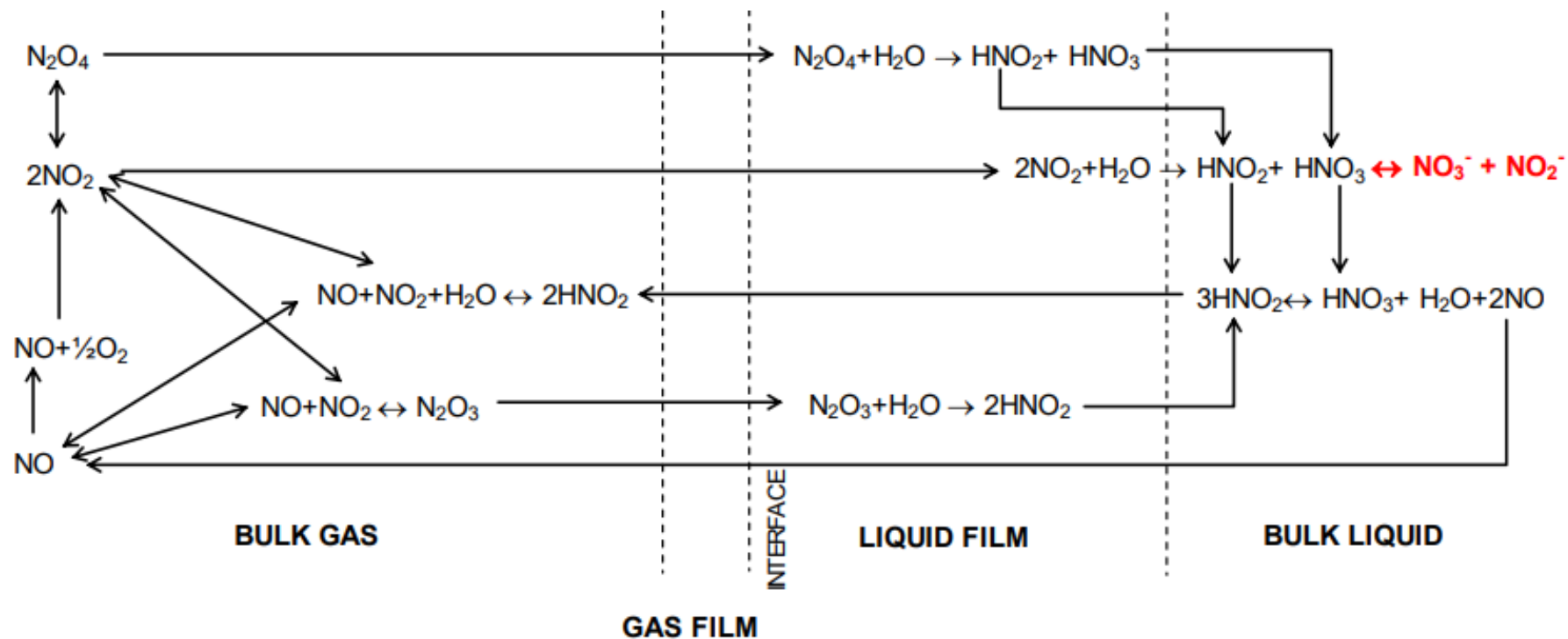
1. DCC outlet
2. Compressor 1st stage outlet
3. Compressor 2nd stage outlet
4. Compressor 3rd stage outlet



3rd stage compressor (14/01/2010)



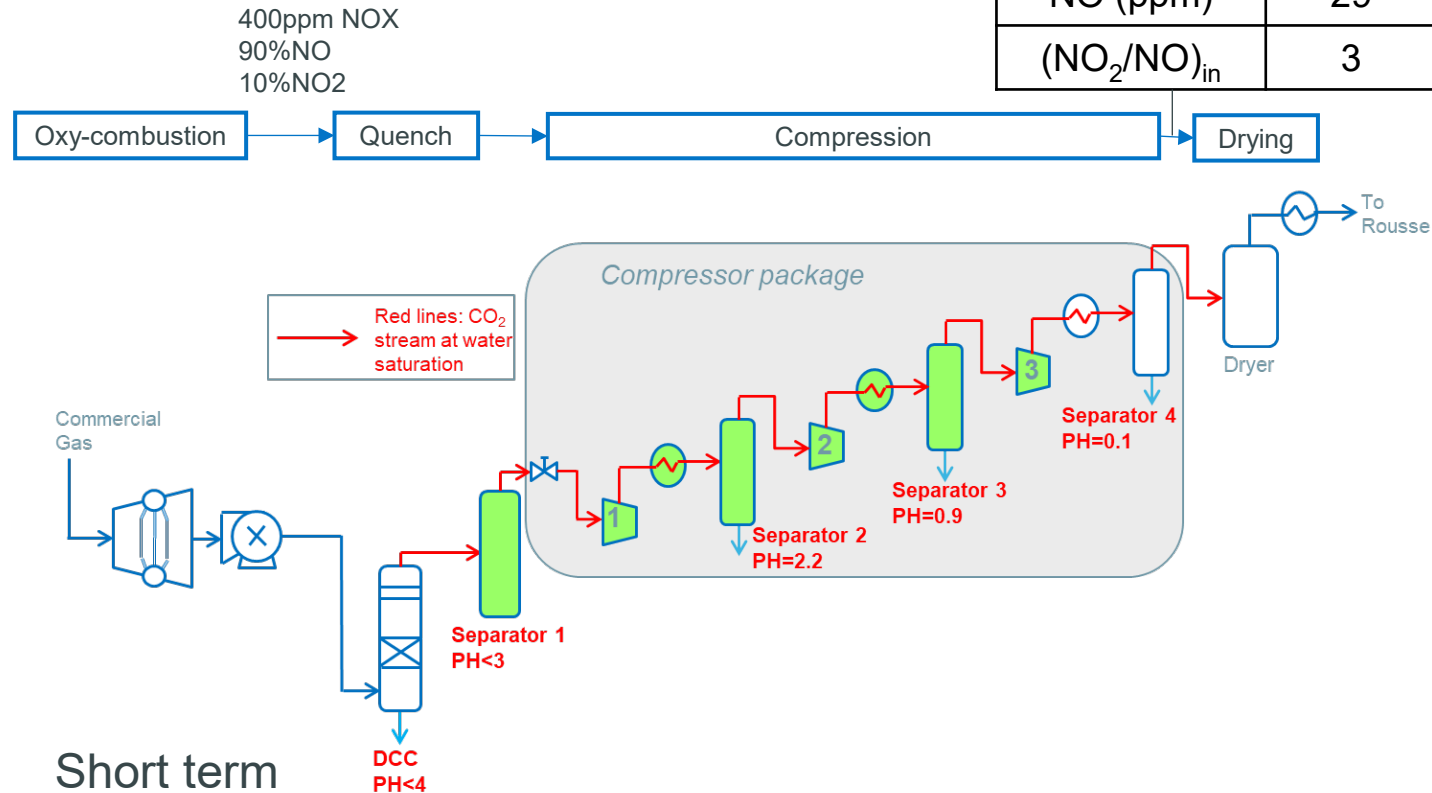
Lacq experience



NO oxydation into corrosive products



Lacq experience



NO _x (ppm)	113
NO ₂ (ppm)	84
NO (ppm)	29
(NO ₂ /NO) _{in}	3



Short term

- Reduce liquid carry over from DCC
- To stay always above dew point

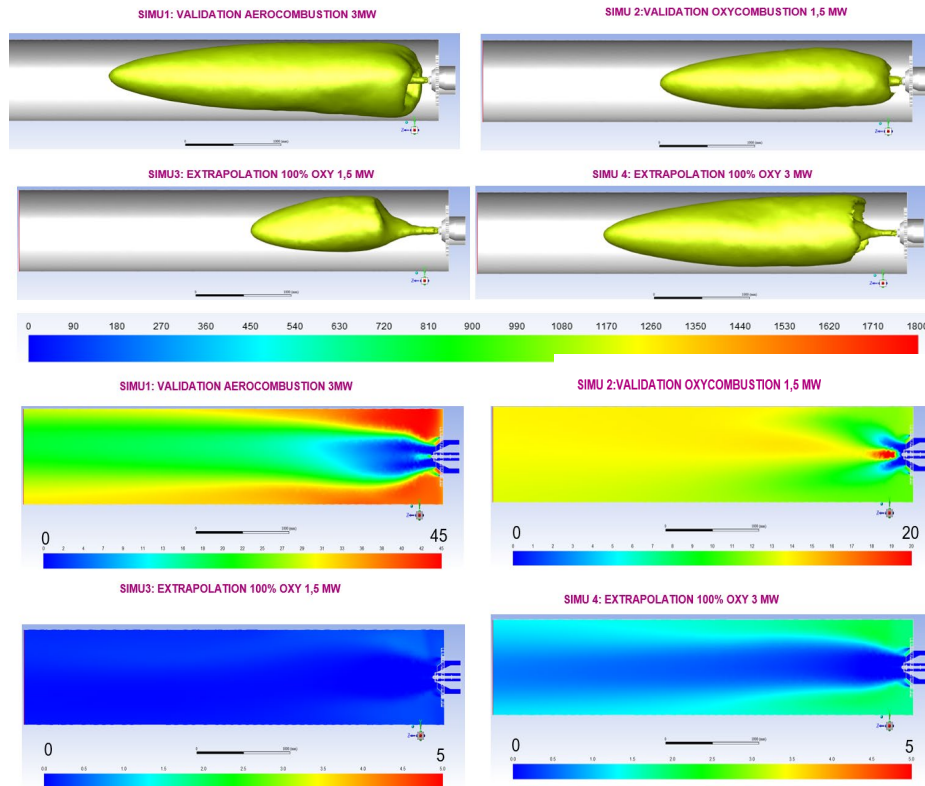
Long term

- To select the right metallurgy for compressor
- **To encourage ultra low NOX burner dev.**



- CFD

17 equations EDC model - NO_x in post treatment (thermal, prompt: NO/NO₂)
ISO TEMPERATURE =1200 °C



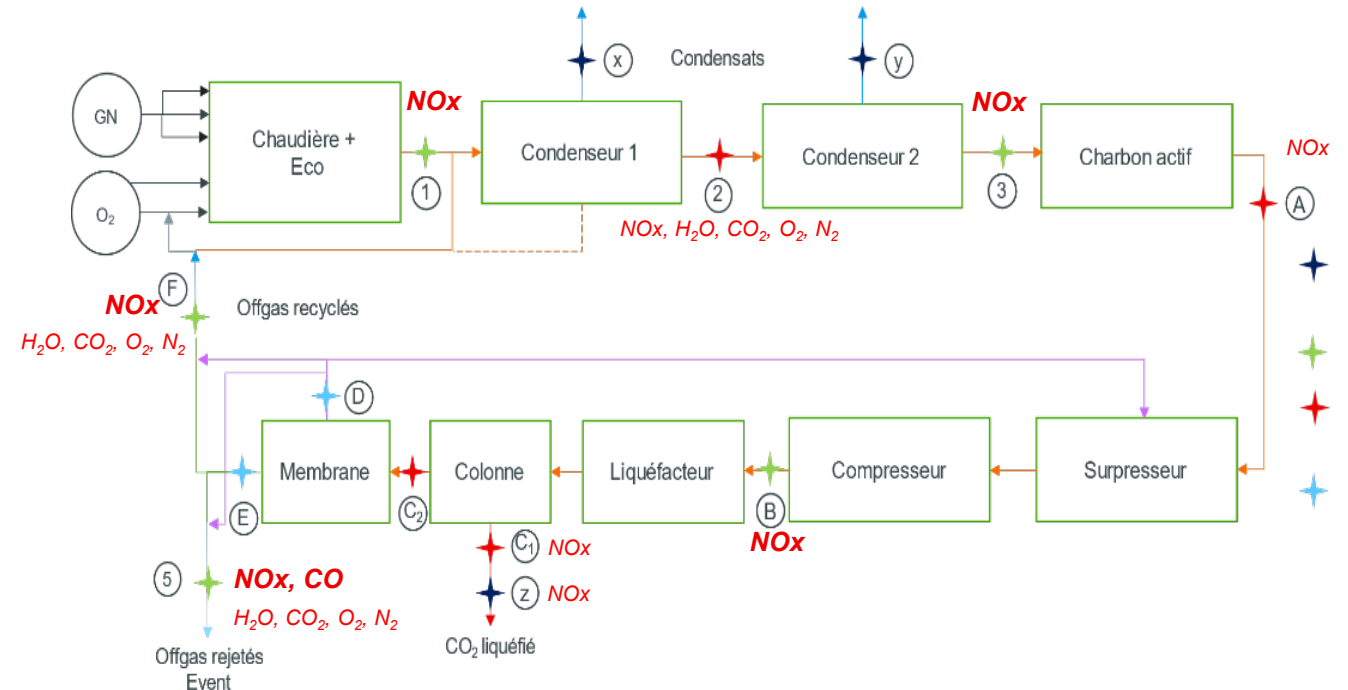
SIMULATION	NOx (ppm) mesure	NOx (ppm) CFD
SIMU 1: base case aerocombustion 3 MW	25	29
SIMU 2: base case oxycombustion 50% 1.5 MW	16.5	14
SIMU 3: extrapolation oxycombustion 100% 1.5 MW	NA	1
SIMU 4: extrapolation oxycombustion 100% 3 MW	NA	2

- N₂ variation in oxygen and natural gas

ChOC pilot includes N₂ injection for testing various composition in natural gas (0 to 8%) and in oxygen (0 to 5%)

- NO_x measuring campaign

A specific N₂ / NO / NO₂ measurement chain will be implemented to validate NO_x formation/reduction on each of the process phases.





11 points throughout the entire process



CHOC boiler project : Operating conditions, gas type matrices and expected NOx contents												
Measurement identification		1	2	3	A	B	C1	C2	D	E	F	5
Location of the measuring spots		Outlet BW economizer	Outlet BW economizer	Outlet VMB condenser	VMB post activated carbon bed	VMB Downstream compressor	Liquified CO2 from column	Gas from column's outlet	Process VMB (4) Membrane outlet	Membrane outlet	Recycling offgas	VMB final Event
Measurement frequency		Permanent	Permanent	Permanent	Occasionally	Permanent	Occasionally	Occasionally	Occasionally	Occasionally	Permanent	Permanent
Piping : DN — Schedule Internal Diameter (mm)		CORTEN steel sheathed tube : diam 300 mm	CORTEN steel sheathed tube : diam 300 mm	existing tapping for measurement with GC (DN15 with 15x21 inox valve)	existing tapping for measurement with GC (DN15 with 15x21 inox valve)	existing tapping for measurement with GC (DN15 with 15x21 inox valve)	existing tapping for measurement with GC (DN15 with 15x21 inox valve)	existing tapping for measurement with GC (DN15 with 15x21 inox valve)	existing tapping for measurement with GC (DN15 with 15x21 inox valve)	existing tapping for measurement with GC (DN15 with 15x21 inox valve)	1 measuring tap for GC to add (DN15 with 15x21 inox valve)	1 measuring tap for GC to add (DN15 with 15x21 inox valve)
Available space		~ 1m above the economizer outlet	Close to internal wall (volume ~ 0,5m each side)	VMB	VMB	VMB	VMB	VMB	VMB	VMB	VMB	VMB
Accessibility		height ~ 2,5 m (A above boiler)	Height ~ 3.5m (possible with)	VMB	30 cm from ground	VMB	VMB	VMB	VMB	VMB	VMB	VMB
Support		existing support to use for probe	existing support to use for probe	VMB	VMB	VMB	VMB	VMB	VMB	VMB	VMB	VMB
Temperature (°C)		85 - 105	20 - 70	4	40	40	-25	0	15	15	15	15
Pressure into process (bar)		Patm +/- 10mbar	Patm +/- 10mbar	Patm +/- 10mbar	Patm +/- 10mbar	20 barg	20 barg	20 barg	20 barg	20 barg	Patm +/- 10mbar	Patm +/- 10mbar
Flow measurement ranges expected	kg/h	0 - 5350	0 - 1000	0 - 1000	0 - 1000	0 - 1000	0 - 600	0 - 400	0 - 400	0 - 400	0 - 400	0 - 400
	Nm3/h	0 - 3500	0 - 600	0 - 600	0 - 600	0 - 600	0 - L00	0 - 200	0 - 200	0 - 200	0 - 200	0 - 200
Adapted Flowmeter to identify				X							X	X
Compounds to analyze		Expected raw compositions in % by mass and target measurement ranges in relation to mass flow rates										
H2O	Expected rate	11,5% — 42,9%	1,8 - 13%	< Point 2	< Point 2	< Point 2	0.0%	0.0%	0.0%	0.0%	0.0%	0.0%
	Range considered	0% - 100%	0 - 20%	0 - 20%	0 - 20%	0 - 20%	-	-	-	-	-	-
CO2	Expected measurement rate	54,7% — 85,8%	84,1% — 95,2%	> Point 2	> Point 2	> Point 2	99,9% environ	71,8% — 91,9%	81,3% — 95,5%	46,5% — 91,9%	81,3% — 95,5%	46,5% — 91,9%
	Range considered	0% - 100%	0% - 100%	0% - 100%	0% - 100%	0% - 100%	0% - 100%	0% - 100%	0% - 100%	0% - 100%	0% - 100%	0% - 100%
N2	Expected rate	0,7% - 7,8%	0,9% — 8,6%	similar than point 2	similar than point 2	similar than point 2	qq ppm	4% — 15,6%	1,8% — 9,2%	0,8% - 43,2%	1,8% - 9,2%	0,8% — 43,2%
	Range considered	0% - 10%	0% - 10%	0% - 10%	0% - 10%	0% - 10%	< 0,1%	0 - 20%	0% - 20%	0% - 50%	0% - 20%	0% - 50%
O2	Expected rate	1,2% — 1,8%	1,3% — 2,7%	similar than point 2	similar than point 2	similar than point 2	qq ppm	2,5% — 12,9%	1,7% — 12,9%	1,5% — 26,9%	1,7% — 12,9%	1,5% — 26,9%
	Range considered	0% - 10%	0% - 10%	0% - 10%	0% - 10%	0% - 10%	< 0,1%	0% - 20%	0% - 20%	0% - 30%	0% - 20%	0% - 30%
NOx compounds analysis : (NO, NO2 > NOx)	Expected rate	0,0013% - 0,0019%	0,0015% - 0,0031%	similar than point 2	similar than point 2	similar than point 2	qq ppm	0,0017% - 0,0834%	0,0017% - 0,0834%	0,0017% - 0,0834%	0,0017% - 0,0834%	0,0017% — 0,0834%
	Range considered	0 - 0,01%	0 - 0,01%	0 - 0,01%	0 - 0,01%	0 - 0,01%	<0,1%	0 - 0,1%	0 - 0,1%	0 - 0,1%	0 - 0,1%	0 - 0,1%
SOx analysis	Expected rate	To be defined		To be defined	-	To be defined	-	-	-	-		-
	Range considered	To be defined	-	To be defined	-	To be defined					-	-



260m sampling lines

30 measuring devices

5 hubs

Sampling lines: From process (tap) to the analysis systems



sampling rod +
heated filter



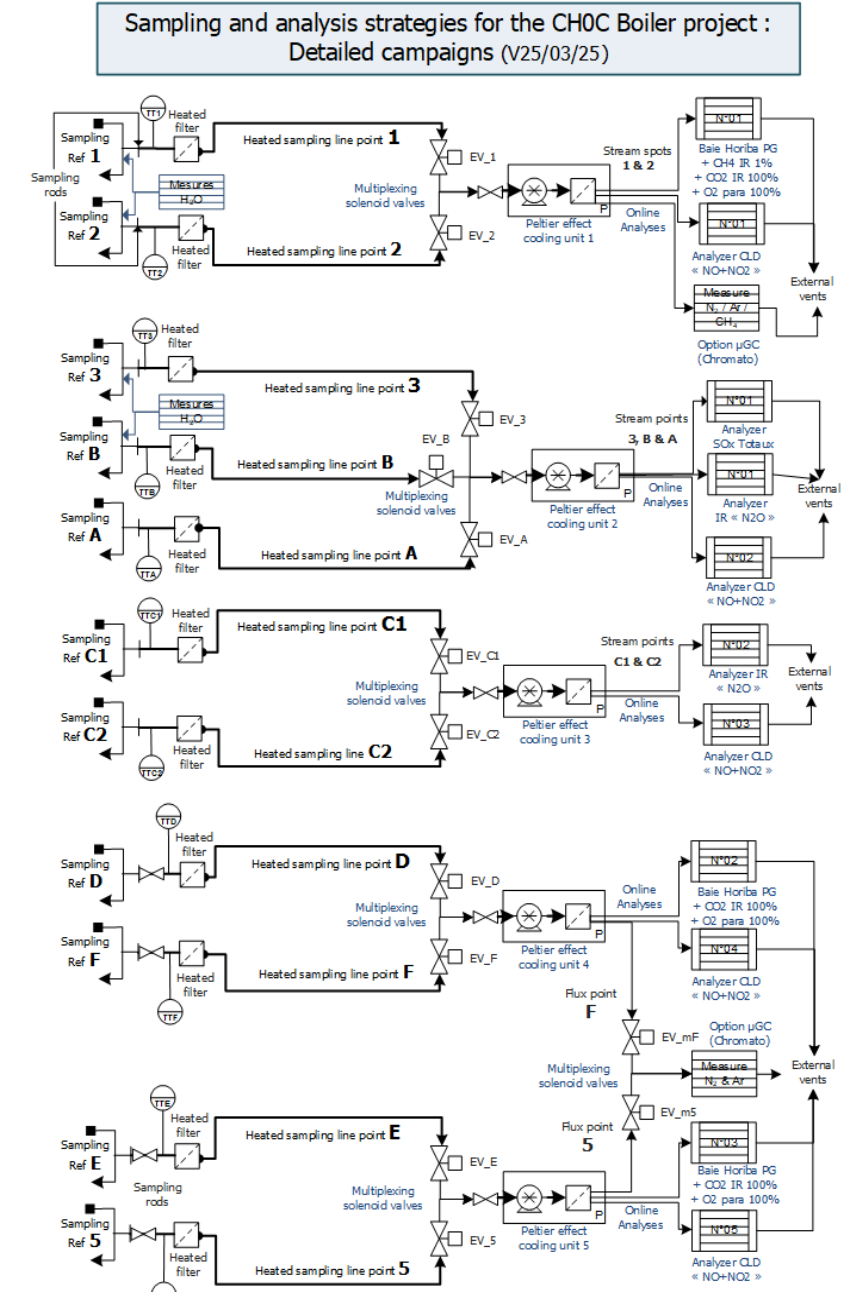
Regulated
heated line



Moisture condensation
system (cooling unit)



CHOC Project: Multiplexed analytical strategy for reference & detailed campaigns							
Measurement systems deployed into the CHOC Project	Brand	Model	Measured Gases	Technologies	Quantity	Additional Equipment	Quantity
	Vaisala	HMS	H2O	Thin-film capacitive	4	Heated filter	4
	Horiba	PG250 (+2 PG350)	O2, CO, CO2, SOX, NOx eq NO	Paramagnetical NDIR, CLD	4	Heated sampling line	19
	EcoPhysics	CLD700	NO, NO2, NOx	Chemiluminescence CLD	6	Sampling Line total lenght	260 m
	Megatec	42i	NO, NO2, NOx	Chemiluminescence CLD	1	Sampling Rod	6
	M&C	GEN-TWO	CO2 (100%)	NDIR	2	Peltier Cooling unit	5
	Siemens	Ultramat 22	CO2 (100%)	NDIR	3	T°K (sensor)	11
	Siemens	Ultramat 22	CH4	NDIR	1	Electrovalves	13
	Servomex	Model 572	O2 (100%)	Paramagnetical	4	Industrial PC	2
	Inficon	Fusion	N2, Ar, CO2	-Gas Chromatograph	1	Webserver	1
	Megatec	42C	N2O	IR Correlation	2	Data acquisition module	2
	Multiplexing carried out on 5 groups: points (1 & 2) ; points (3, A & B) ; points (C1 & C2) ; points (D & F) ; points (5 & E)						





126 condensate samplings

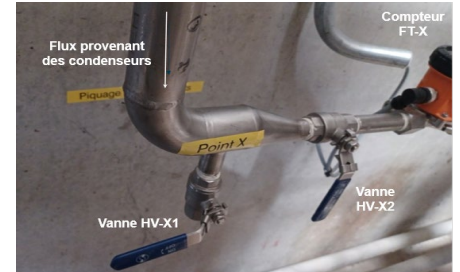


1. Referenced sampling point **X**: 1 measurement created on the condenser collection line, downstream the boiler.
2. Referenced sampling point **Y**: 1 measurement implemented downstream of the VMB activated carbon bed.

Condensates analyses strategy																	
CH0C Project	Media : Natural Gas																BG
	Essais MSI			Parametrical tests										Essais LD		Essais MSI	
	Aéro	Oxy + Liq	Qualif/réception	FA1	FA2	Ox1	GN2	VAP1	VAP2	VAP3	FGR1	Rec1	Liq1	Liq2	Charge fixe	Charge variable	Qualif/réception
M1-A	0																
M1-B		0															
M2-A		0															
M2-B			4x + 4y														
M3-A				3x + 3y	0												
M3-B						3x + 3y	0										
M4-A								2x+2y	1x+1y	1x+1y	0						
M4-B												3x + 3y	0	0			
M5-A														0	0		
M5-B														0	0		
M6-A														0	0		
M6-B														0	0		
M7-A																	4x + 4y
M7-B																	
M8-A																	
M8-B																	

Analyse 1	pH, hardness, conductivity, NO^{2-} , NO^{3-} , $\text{NO}^{3-\text{N}}$, $\text{NO}^{2-\text{N}}$, HNO_2 , HNO_3 , CO_3^{2-} , Total Organic Carbon (COT), metals (Cr^{3+} , Ni^{2+} , Al^{3+} , Fe^{3+}), dissolved gases (CO_2 , O_2), MES & SO_3^{2-} , SO_4^{2-} , H_2SO_4 , only in case of SO_x identified into the flue gas
Analyse 2	pH, NO^{2-} , NO^{3-} , $\text{NO}^{3-\text{N}}$, $\text{NO}^{2-\text{N}}$, HNO_2 , HNO_3
Analyse 3	pH, NO^{2-} , NO^{3-} , $\text{NO}^{3-\text{N}}$, $\text{NO}^{2-\text{N}}$, HNO_2 , HNO_3 : only in case of no ability to establish a model within the results from previous tests.

Analyses 1+2+3	
Total : ~ 42 samples	Flacons to be analyzed
Analyses 1 (16)	48
Analyses 2 (12)	36
Analyses 3 (14)	42
TOTAL (3)	126



To provide accurate physico-chemicals measurement, all the aqueous samplings standardly led in the CH0C process are integrating a complementary step by filling all the container dedicated for each species to determine (between 6 & 10 according to the analysis). All analyses will be achieved by an external specialized laboratory.

Containers dedicated to a full analysis





Photos





**The demo project is open
for visit and collaborations.
Results will be published**



Key take away



-Setting-up a full
NOX measurement
along the CCU
chain



- Testing a
promising **ultra low**
NOX burner



-**Agile and**
Collaborative Team
from various
companies



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