



### Improving on the CCSI model for MEA-based CO<sub>2</sub> capture

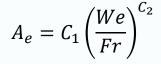
Ryan Cownden, Mathieu Lucquiaud, & Jon Gibbins University of Sheffield, UK

PCCC-8, 16 Sep 2025

This research was supported by funding from the University of Sheffield and the Natural Sciences and Engineering Research Council of Canada.

# Background

- Carbon Capture Simulation Initiative (U.S. DoE)
  - "gold-standard" MEA-CO<sub>2</sub> capture process model (2018)
  - O publicly available Aspen Plus source file
  - widely used
- Underreported issues/limitations
  - O interfacial area correlation Weber dependence, Froude omitted
  - simplified chemistry
  - single packing 250Y/252Y
  - regression based on limited dataset from lab-scale equipment





## **New model**

- Thermodynamic/chemistry model
- Widely applicable correlations
- Validated v. large-scale pilot plants
  - 5 datasets
  - 4 facilities
  - wide range of operating conditions and scale
  - $\circ$  0.1 78 tCO<sub>2</sub>/d



## Methodology

- Aspen Plus
  - O full system model
  - rate-based absorber/regenerator
- ELECNRTL framework
  - rigorous chemistry
  - custom parameter regression v. VLE
  - O 15-45%wt MEA, 40-120°C, 0.05-0.50 mol<sub>CO2</sub>/mol<sub>MEA</sub>
- Absorber CO<sub>2</sub> reaction kinetics
  - O Hikita et al.
  - Pinsent et al.

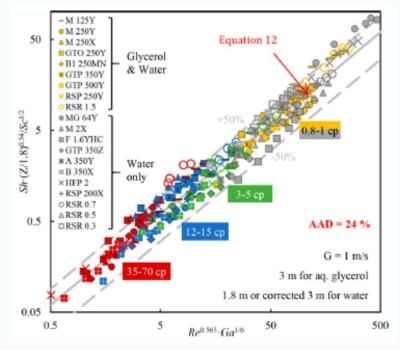
$$2H_2O \rightleftharpoons H_3O^+ + OH^ CO_2 + 2H_2O \rightleftharpoons H_3O^+ + HCO_3^ HCO_3^- + H_2O \rightleftharpoons H_3O^+ + CO_3^{2-}$$
 $MEAH^+ + H_2O \rightleftharpoons H_3O^+ + MEA$ 
 $MEACOO^- + H_2O \rightleftharpoons HCO_3^- + MEA$ 

$$MEA + CO_2 + H_2O \rightleftharpoons MEACOO^- + H_3O^+$$
  
 $CO_2 + OH^- \rightleftharpoons HCO_3^-$ 



## Methodology

- Mass transfer coefficients & A<sub>e</sub>
  - O Song et al. (2018)
- Liquid holdup
  - O Tsai (2010)
- Closed-loop model validation



 $k_L$  correlation v. experimental data from Song et al. (2018)



# Pilot plant data

	Stuttgart	NCCC	Haifeng	TCM
Captured CO <sub>2</sub> (tCO <sub>2</sub> /d)	0.11-0.16	4.9-7.8	38	49-80
Absorber liquid flux (m³/m²-h)	6.1-20	9.7-35	7.0	3.9-7.8
Inlet vapour CO <sub>2</sub> (%mol)	5.2-10.9	9.2-11	13	3.6-4.1
Rich loading (mol/mol)	0.30-0.42	0.28-0.39	0.50	0.48-0.53
CO <sub>2</sub> capture rate	75-91%	93-98%	98%	86-97%
Absorber height (m)	4.2	6.1-12.2	15.9	24
Regenerator height (m)	2.52	12.2	8.52	9.6

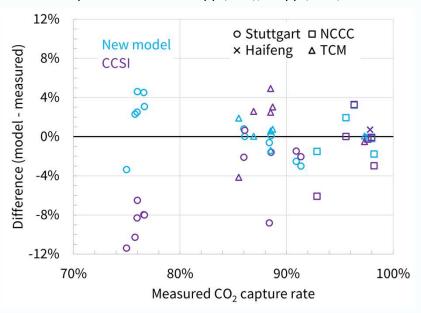


Stuttgart: Notz et al. (2012) – doi:10.1016/j.ijggc.2011.11.004 NCCC: Morgan et al. (2018) – doi: 10.1021/acs.iecr.8b01472 TCM: Faramarzi et al. (2017) – doi:10.1016/j.egypro.2017.03.1271

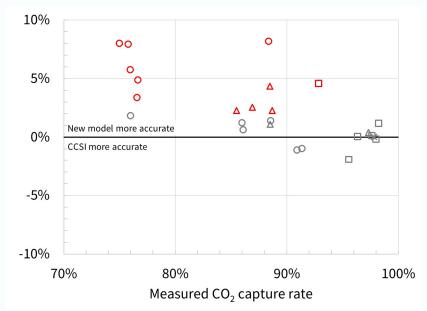
TCM: Bui et al. (2020) - doi:10.1016/j.ijggc.2019.102879

## **Capture rate predictions**

New model more accurately predicts capture rate RMSD v. experimental data: 2.2 pp (new), 5.2 pp (CCSI)



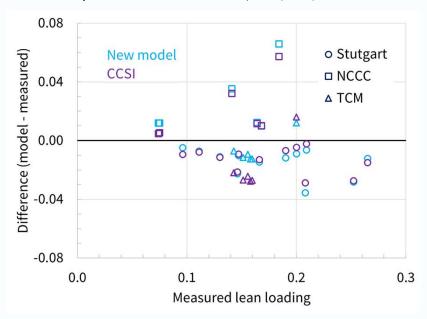
### Substantial improvements for some conditions Reduction in absolute deviation (pp) from experimental data v. CCSI



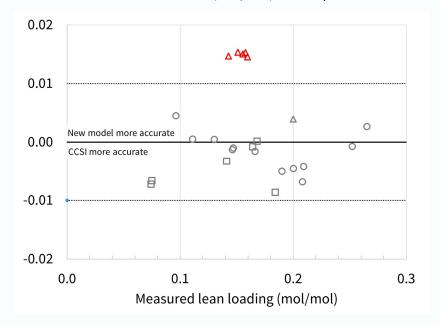


# Lean loading predictions

### New model & CCSI predict similar lean loadings RMSD v. experimental data: 0.021 mol/mol (both)



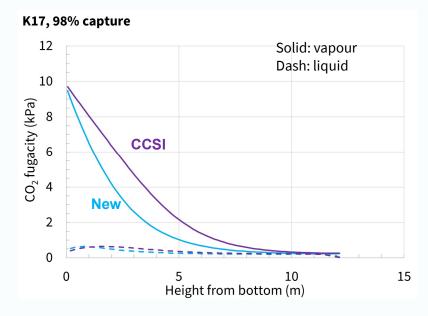
### Most cases within 0.01 mol/mol, some TCM outliers Reduction in absolute deviation (mol/mol) from experimental data v. CCSI





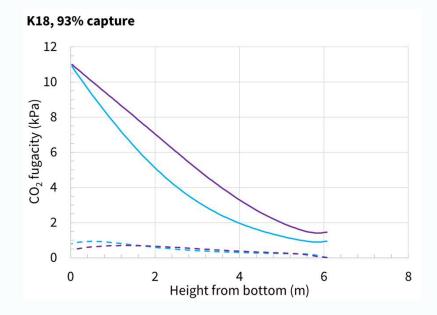
# Column height

12m absorber – similar predicted capture rate Loss of driving force constrains CO₂ capture



Capture: 97.5% v 97.4%

6 m absorber – new model more accurate CCSI mass transfer coefficients too low to predict CO<sub>2</sub> capture rate



Capture: 91.4% v. 86.8% Measured: 92.9%

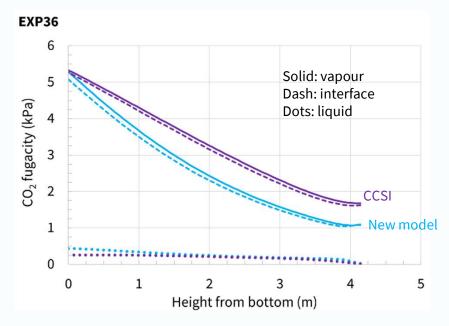


- ➤ NCCC, 9/10%mol CO₂ gas inlet
- lean loading: c. 0.18 mol/mol
- same gas/liquid flow rates



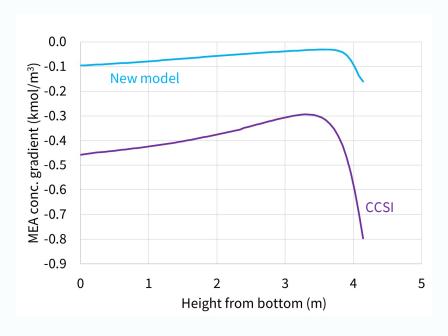
## Liquid side mass transfer resistance

CCSI liquid mass transfer coefficients much lower Leads to higher interface CO<sub>2</sub> fugacity, low capture rate predictions



- ➤ Stuttgart case 36: 5.3%mol CO₂ gas inlet
- lean loading: 0.224/0.225 mol/mol
- > CO<sub>2</sub> capture rate: 79.7%/68.6% v. 76.6%

### CCSI has larger liquid concentration gradients Relative depletion of MEA at the interface



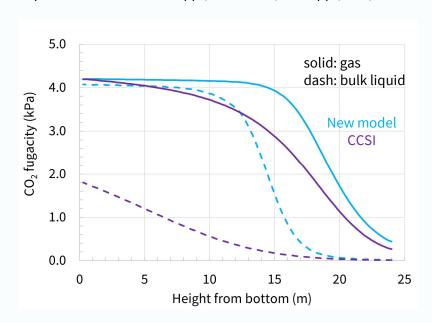
$$\Delta C = C_{interface} - C_{bulk}$$



## Low temperature absorption

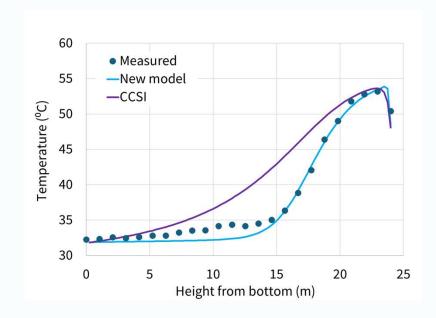
#### New model has slower reaction kinetics

Capture rate deviation: 0.6 pp (new model) v. 4.9 pp (CCSI)



#### Absorber temperature profile

Corroborates new model reaction kinetics

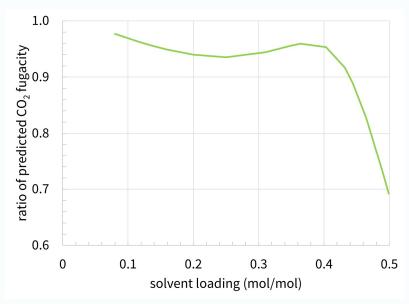




- TCM (Bui et al. ICL11)
- → 4.1%mol CO<sub>2</sub> gas inlet
- lean loading: 0.136/0.121 mol/mol
- CO<sub>2</sub> capture rate: 89.1%/93.4% v. 88.5%

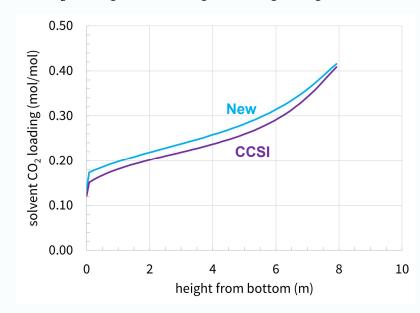
## Regeneration - high rich load/temperature

#### New model predicts lower CO<sub>2</sub> fugacity @ 120°C



CO<sub>2</sub>-MEA-water VLE 120°C, 30%wt MEA Ratio of predicted CO<sub>2</sub> fugacity (new model/CCSI)

#### More accurate lean loading prediction Less CO<sub>2</sub> flashing off at inlet, higher loading throughout



- TCM (Bui et al. ICL11)
- rich loading: 0.494/0.497 mol/mol
- lean loading: 0.136/0.121 mol/mol v. 0.143 (measured)



## **Concluding remarks**

- New model predicts capture rate more accurately than CCSI
  - O overall RMSD for CO<sub>2</sub> capture 2.2 pp v. 5.2 pp
- Substantial improvement for:
  - O high rich solvent CO<sub>2</sub> loading + low gas CO<sub>2</sub> concentration
  - O low absorber temperature
  - short columns
- Correlations more widely applicable
  - O unconstrained by small sample regression
- Intend to publish model



# **Questions?**

## racownden1@sheffield.ac.uk

#### connect:



