



PILOT PLANT TESTING OF PIPERAZINE WITH THE ADVANCED FLASH STRIPPER AT 3.5 TO 20% CO2

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C2P3 & UT PZ Pilot Plant Testing



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Current Pilot Facilities & Equipment

- SRP 0.1 MW, 16.8-inch ID
- 200-450 lb CO_2 /hr removal
- Synthetic Flue Gas: Air/CO₂
 - Enthalpy, 1-2 % H₂O, 30-40 °C
 - 3-20% inlet CO₂
 - Air max. oxidative degradation
- 30 feet (6.1 m) absorber packing
- Absorber intercooling
- 0.1-0.2 MW 10" AFS skid
 w/cold and warm rich bypass





April/May 2017 Pilot Plant Campaign

- 20% CO₂ Parallel hybrid membrane-amine process (MTR-DOE Project)
- 12% CO₂ Coal benchmark
- 3.5% CO₂ Natural gas conditions
- 4 weeks, 24 hr day, weekend shutdown
- 29 runs
- 5 m PZ
- Absorber w/intercooling
 - 30 ft (3 x 10 ft beds)
 - 20 ft (2 x 10 ft bed) + 10 ft water wash
- 10" Advanced flash stripper



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DOE-MTR Hybrid Membrane Project



- 90% Capture Rate for the Capture System
- Absorption process removes 95%+ CO₂ from a split flue gas stream



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MTR Low Pressure Drop Plate-and-Frame Membrane Contactor



Polaris plate-and-frame sweep modules (designed in DE-NT007553)

500 m² R&D Skid: 5 elements bundled in one vessel.





2017 AFS Campaign Configuration





Absorber Conditions





Stripper Conditions







Absorber Performance



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Cold Cross Exchanger Performance





CO₂ Capture Pilot Plant Program

Cross-Exchanger Performance





PZ Management Results

- Precipitation minimized by 5 m PZ
 - Instr air loss + chilled water to IC = precipitation
 - Melted at 80 °C with heat gun
- Foaming
 - Moderate unexpected absorber DP at high gas rate (600 cfm)
 - Reduced to normal by addition of antifoam
- Oxidation is acceptable
 - NH₃ emissions of 3 to 10 ppm, could still be reduced
- Aerosol requires high SO₃ (Beaudry/Akinpelumi)
 - PZ emissions doubled with 10 -100 ppm SO₃
- Corrosion of CS could be acceptable for stripper shell (Fischer)
 - 175 (SS), 325 (CS) mm/yr in hot lean PZ



2017 PP Conclusions

- Absorber & stripper performed well with 20% CO₂
- Absorber predicted acceptably by "Independence" Aspen process model (Zhang)
 - Absorber model most accurate for 4% and 12% CO_2
 - Liquid distribution poor at high L/G
- Energy requirement independent of inlet CO₂
 - Heat loss needs more analysis
- Exchangers provide 4-8 °F pinch with 5 to 10% cold rich bypass
- Hot flashing P&F exchanger provides reliable heat transfer



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