

PZ pilot campaign at TCM – oxidation due to O₂ and NO₂ in flue gas

PCCC8, Marseille, France

The University of Texas at Austin and Honeywell
Texas Carbon Management Program
September 18, 2025



Presentation outline

- Pilot scale
- TCM flue gases
- Liquid solvent degradation data
 - LC/MS (measured at TCM)
 - Amino acids (measured at UT)
- Gas phase evidence of oxidation
- Modeling NH₃ evolution due to oxidation
- Oxygen measurements
- Conclusions



Pilot facilities scale

Parameter	SRP (UT Austin)	NCCC (Southern Co.)	TCM (Mongstad, Norway)
Size equivalent (MW _{eq})	0.1	1.0	12 (RFCC f.g. at 40,000 kg/hr)
Abs packing height (ft)	20	40	60
Flue gas source	Synthetic	Nat gas boiler	RFCC, MHP (fuel gas boiler)
Flue gas rate (kg/hr)	1,350	3,630	35,800 (RFCC)/45,800 (MHP)
CO ₂ capture rate (MT/d)	1.5	6	180 (RFCC)/234 (MHP) @ 96%

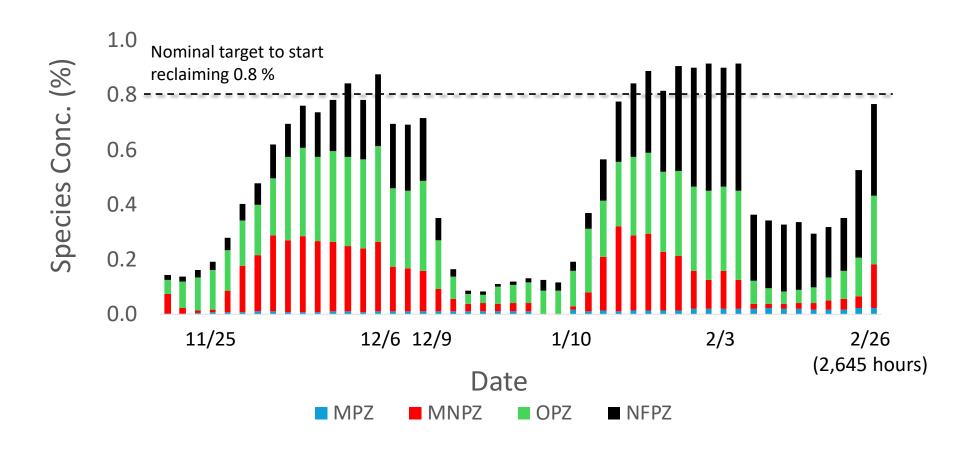


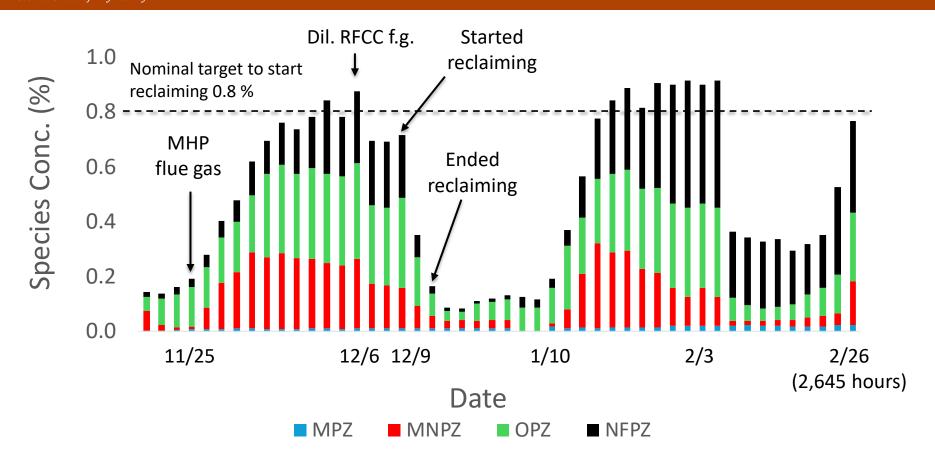
Flue gases at TCM

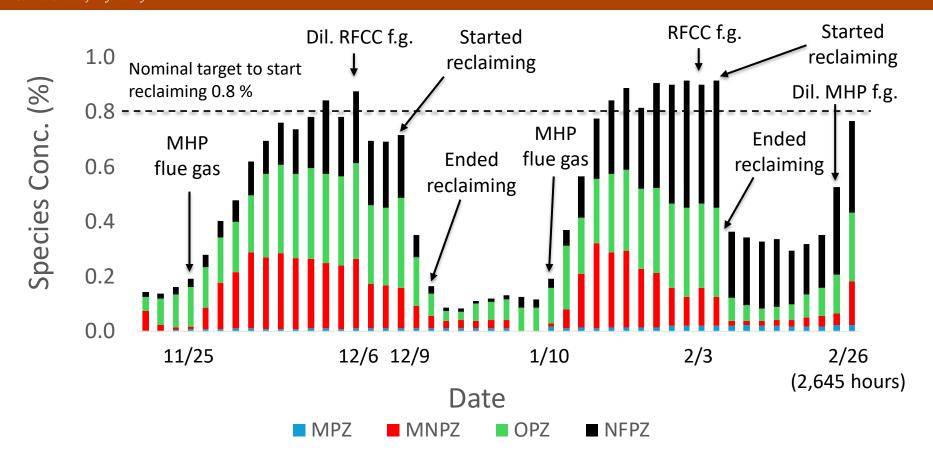
Component	RFCC	МНР
CO ₂ (%)	15.7	9.9
O ₂ (%)	2.5-3.5	3.8
NO ₂ (ppmv)	0.5-1.5	15.7
Total particle no. (TN) (#/cm³)*	7.9 - 9.5 X 10 ⁴	-

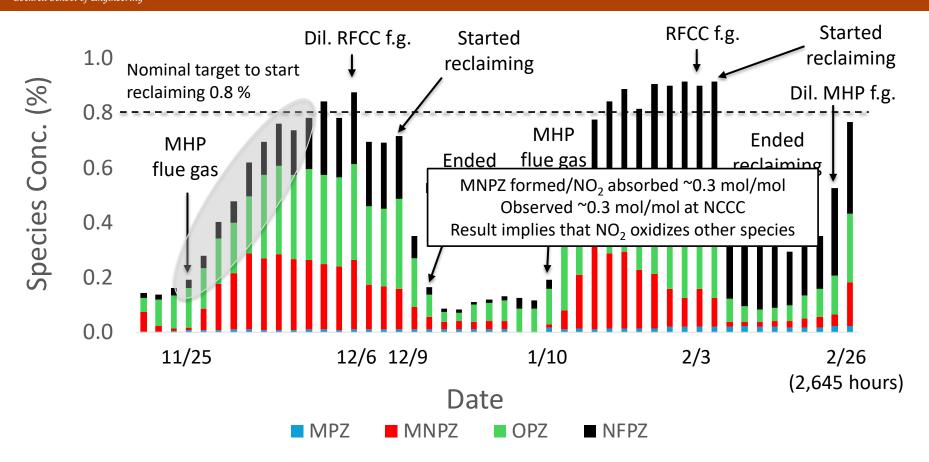
^{*}From Laborelec report (2025).

Degradation data - liquid phase











Reactions in the absorber and stripper

Table 1. PZ oxidation by NO2 at absorber temperature

Type of reactions	Reactions	Numbers
NO ₂ absorption	$NO_2 + PZ \rightarrow PZ \cdot + NO_2^-$	(1)
Radical propagation	$PZ \cdot + O_2 \rightarrow PZOO \cdot$	(2)
	$R \cdot +PZ \rightarrow PZ \cdot +P$	(3)
	$R \cdot= PZOO \cdot, PZO \cdot, and \cdot OH$	
	$P = PZOOH, PZOH, and H_2O$	
Radical termination	$2PZ\cdot +H_2O \to PZOH + PZ$	(4)
Organoperoxy dissociation	$PZOOH + PZ \rightarrow 2PZOH$	(5)
	$PZOOH \rightarrow PZO \cdot + \cdot OH$	(6)
Nitrosamine/nitramines generation	$NO + PZ \rightarrow MNPZ$	(7)
	$NO_2^- + PZ \rightarrow MNPZ$	(8)
	$NO_2 + PZ \rightarrow m - nitro PZ$	(9)

Ref: Chen, C. and Rochelle, G.T. Amine Oxidation Catalyzed by NO₂, 16th International Conference on Greenhouse Gas Control Technologies, Lyon, France, October 23-27, 2022.

Reactions in absorber and abs packing; plenty of O₂

Table 2. MNPZ generation and decomposition in the stripper (high temperature)

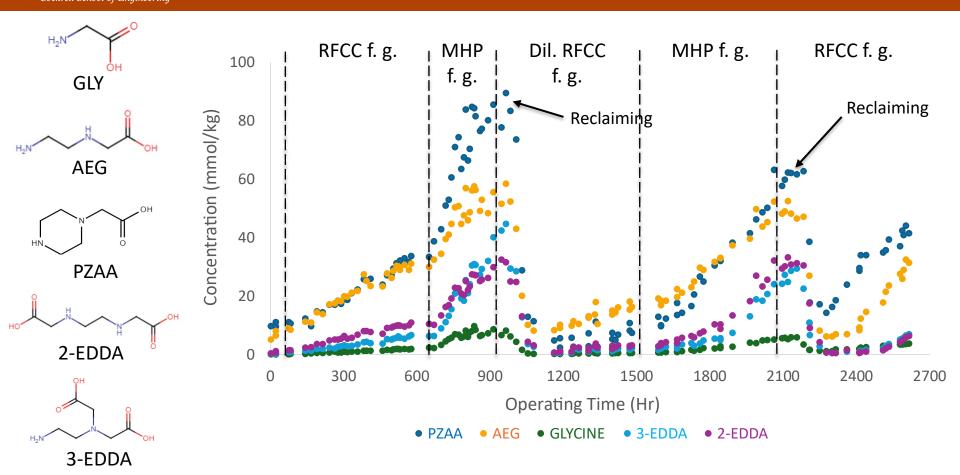
Type of reactions	Reactions	Numbers
Nitrosation	$NO_2^- + H^+ + PZ \rightarrow MNPZ$	(10)
MNPZ thermal decomposition	$MNPZ + 0.5 H_2O \xrightarrow{base, \Delta} PZOH + 0.5 N_2O$	(11)

Reactions in stripper; absence of O₂

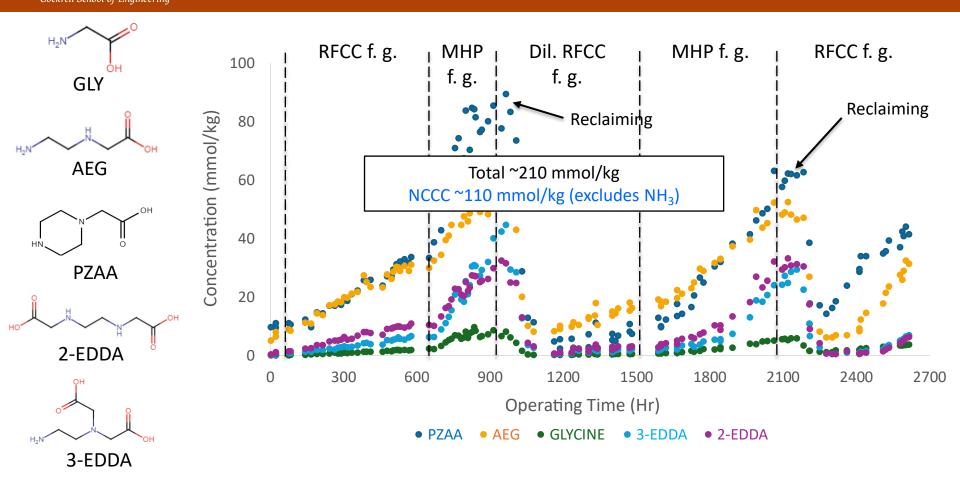


Amino acids

of Chemical Engineering TCM lean sample (hydrolyzed) total amino acids

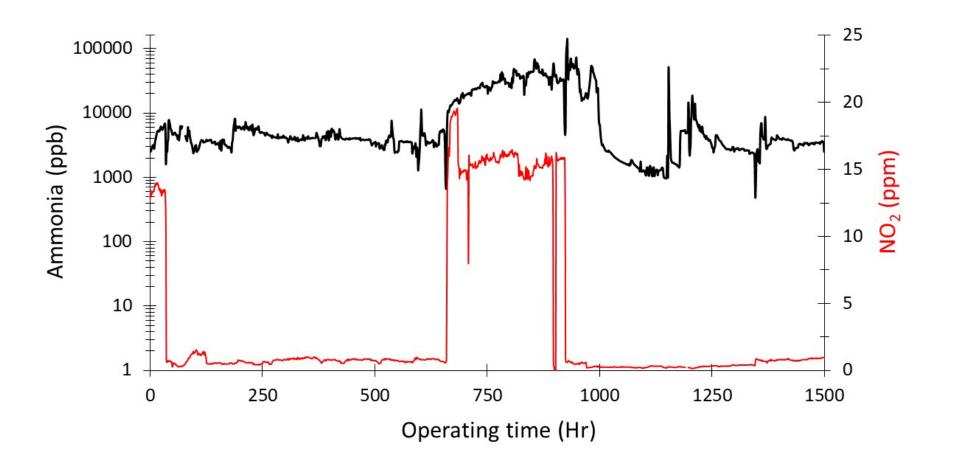


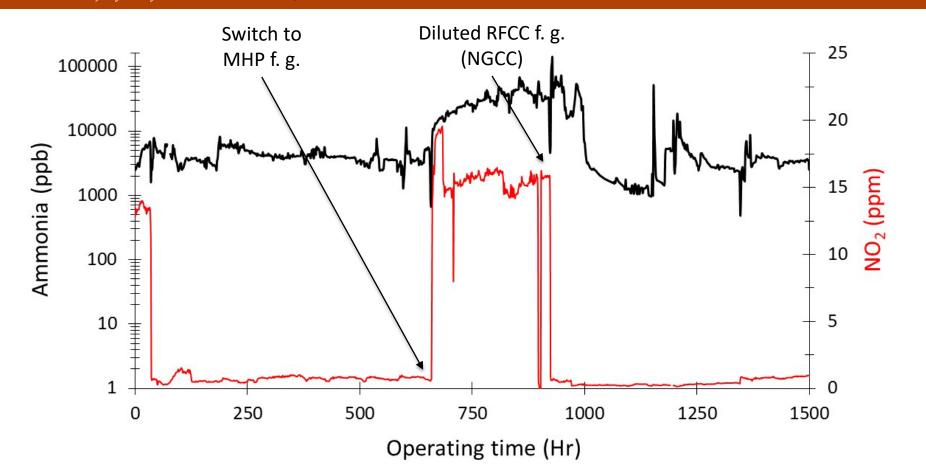
TCM lean sample (hydrolyzed) total amino acids





Gas phase evidence of oxidation







Modeling NH₃ response to NO₂

Steady state run periods modeled

			•			
Gas	Start Time	End Time	Total time (d)	Avg O ₂ (%)	Avg NO_2 (ppm)	Mols NH ₃ /Mols NO ₂
RFCC	11/5	11/14	10	3.1	0.7	5.2
RFCC	11/18	11/25	8	3.1	0.8	3.7
RFCC	12/30	1/7	8	2.9	0.9	3.8
MHP	11/25	12/6	12	3.8	15.3	1.7
MHP	2/26	2/26	2	3.7	17.0	1.0
Dil-RFCC	12/20	12/24	5	16.0	0.4	7.6
Dil-RFCC-2	12/24	12/30	7	9.4	0.8	4.0
Dil-MHP	1/7	1/21	15	13.8	5.5	1.2
Dil-MHP	2/20	2/22	3	13.4	6.3	1.1

- (a) Data sets represent steady state conditions
- (b) No weighting based on run duration in model
- (c) Included NH₃ in CO₂ stream; <5% but ~9% when P_{str} lowered for reclaiming

Modeling NH₃ response to NO₂

$$\frac{mols\ NH_3}{mols\ NO_2} = 0.01[O_2]_{avg} + 4.4[NO_2]_{avg}^{-0.48} - 0.44$$

Where: [O₂] (%) & [NO₂] (ppm)

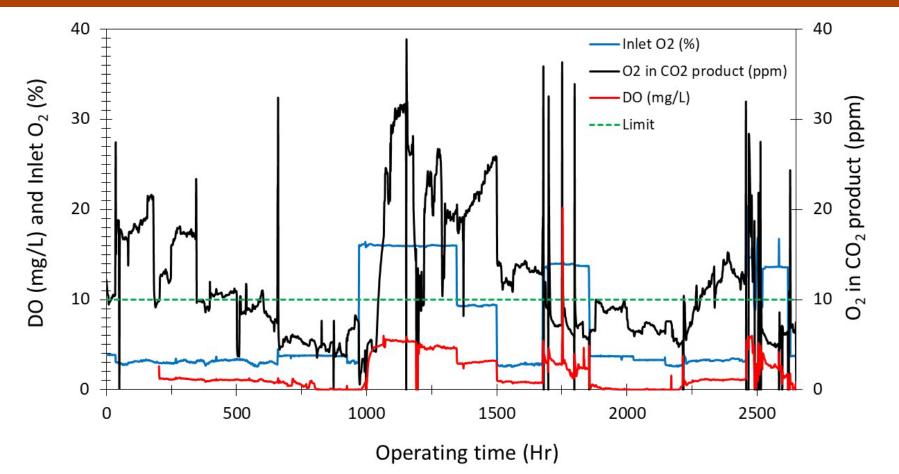
Key takeaways:

- (1) Relationship between cumulative mols $NH_3/mols\ NO_2$ and $[NO_2]_{inst}$ obeys power law
- (2) Flue gas O₂ concentration has little bearing on model results indicates the model over-simplifies the chemistry
- (3) Modeling oxidation should account for accumulation and oxidation of amino acids

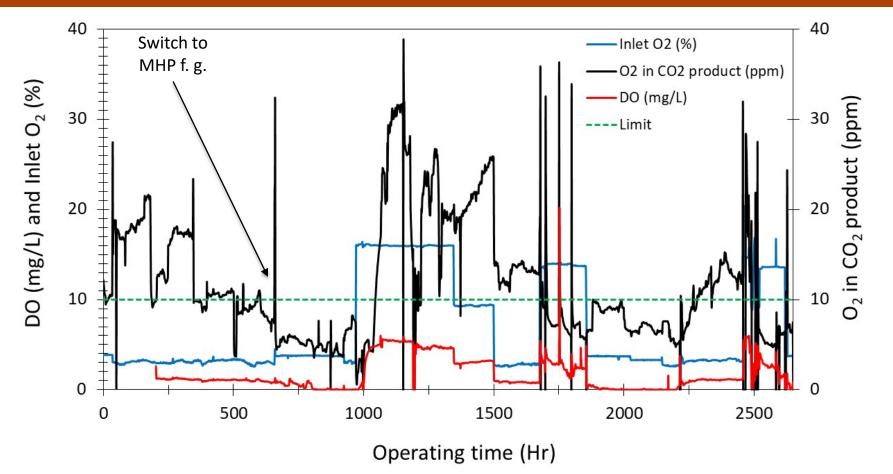


Oxygen measurements

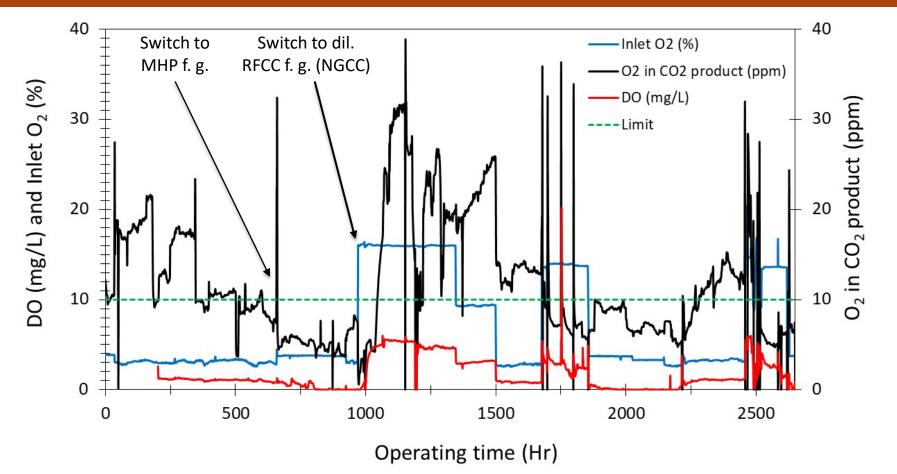




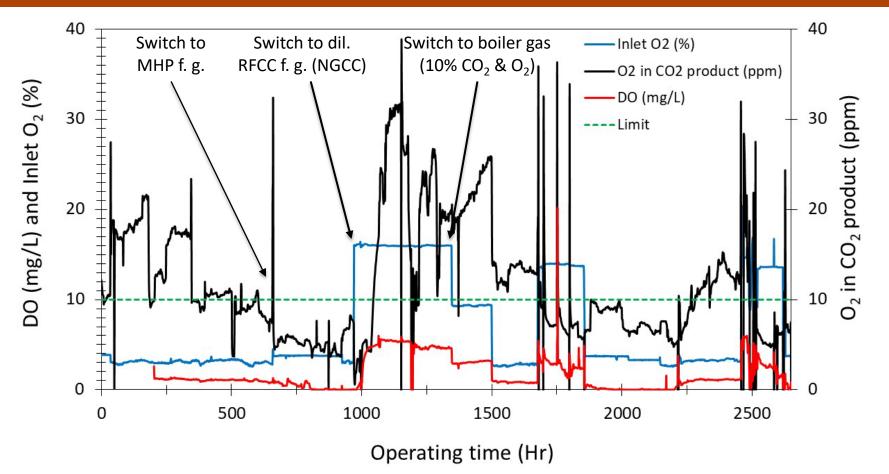




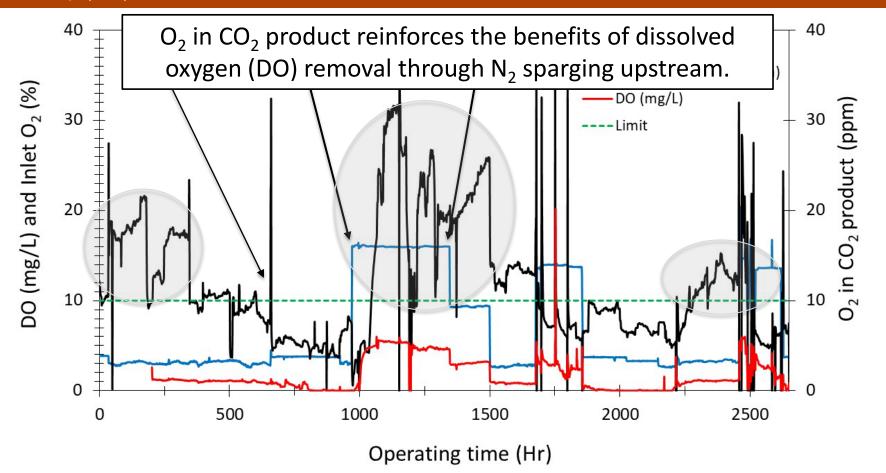






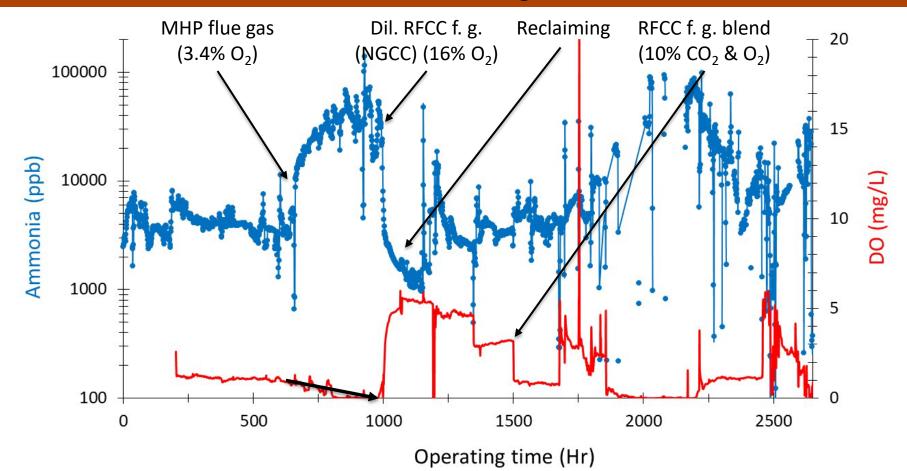






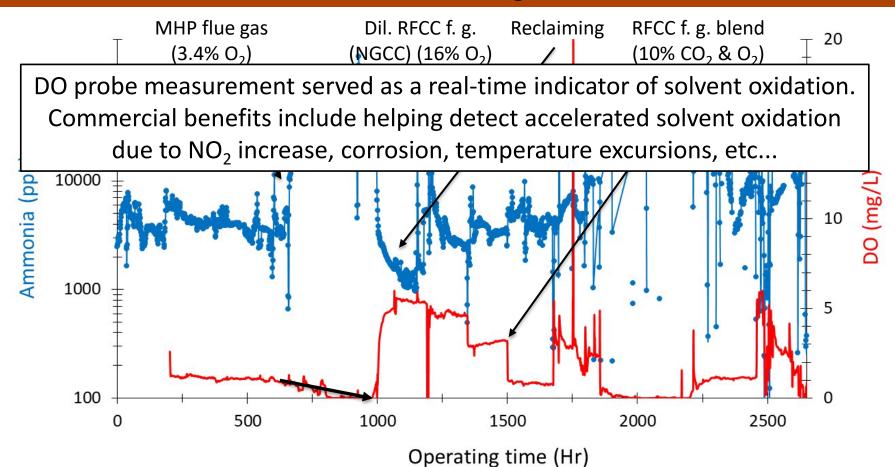


DO and NH₃ (FTIR) at TCM





DO and NH₃ (FTIR) at TCM



Conclusions

- MHP flue gas with 16 ppm NO₂ accelerated formation of amides, amino acids, and MNPZ
- Mols MNPZ formed/mols NO₂ absorbed ~0.3
- NO₂ accelerated evolution of NH₃
 - Modeled the ratio using steady state run periods
 - Model may be improved by accounting for amino acids
- Oxygen measurements
 - O₂ >10 ppm in CO₂ product when not depleted before stripper; supports argument for DO stripping in absorber
 - DO measurement is a useful real-time tool for monitoring solvent health

Acknowledgements

Texas Carbon Management Program
US Department of Energy
Technology Centre Mongstad
Disclaimer

The Technology Centre Mongstad pilot plant was supported by the U.S. DOE through FE0031861 with additional support from Honeywell UOP and the Texas Carbon Management Program.

One author of this paper consults for a process supplier on the development of amine scrubbing technology. The terms of this arrangement have been reviewed and approved by the University of Texas at Austin in accordance with its policy on objectivity in research. One author also has financial interests in intellectual property owned by the University of Texas that includes ideas reported in this paper.

Neither the United States Government nor any agency thereof, nor any of their employees, makes any warranty, express or implied, or assumes any legal liability or responsibility for the accuracy, completeness, or usefulness of any information, apparatus, product, or process disclosed, or represents that its use would not infringe privately owned rights. Reference herein to any specific commercial product, process, or service by trade name, trademark, manufacturer, or otherwise does not necessarily constitute or imply its endorsement, recommendation, or favoring by the United States Government or any agency thereof. The views and opinions of authors expressed herein do not necessarily state or reflect those of the United States Government or any agency thereof.



Questions?

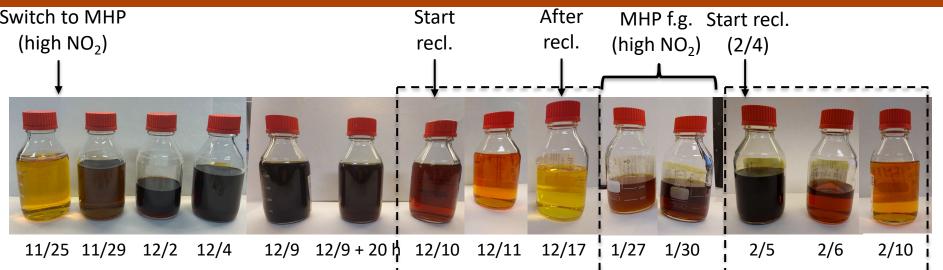


Project participants

Party	Person	Role
NETL	Krista Hill	Project Manager
Texas Carbon Management Program (TxCMP)	Dr. Gary Rochelle Dr. Fred Closmann	Principal Investigator Project Manager
Honeywell	Carl Stevens Nathan Lozanoski Ramiro Roman	Technology development
University of Oslo	Armin Wisthaler Tomas Mikoviny	Gas phase measurements (TOF-MS)
TCM	TCM Team	Pilot implementation



TCM solvent

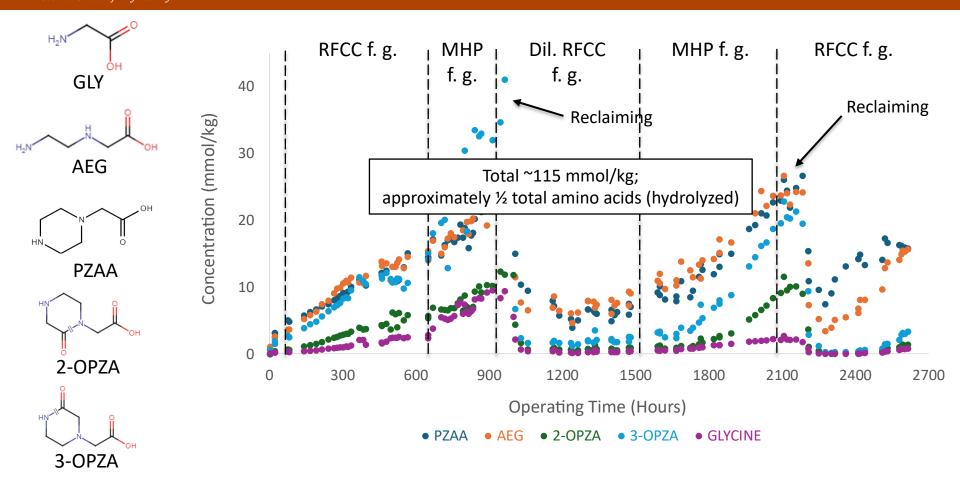


After reclaiming

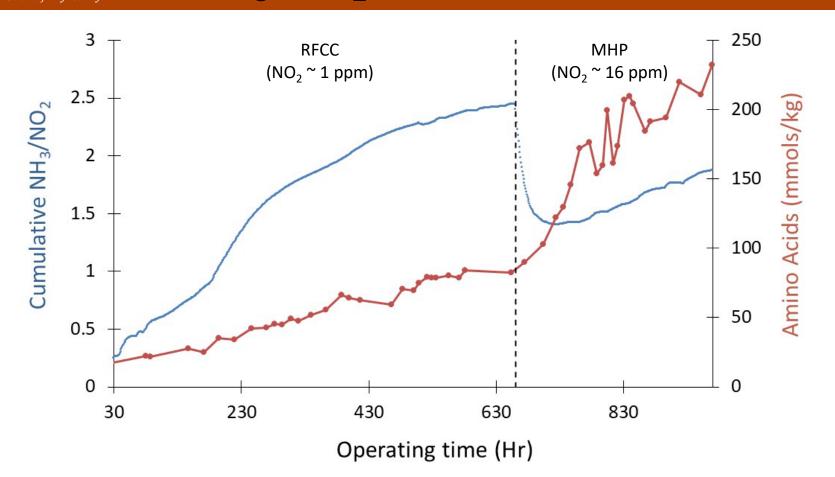


2/15 through 2/17

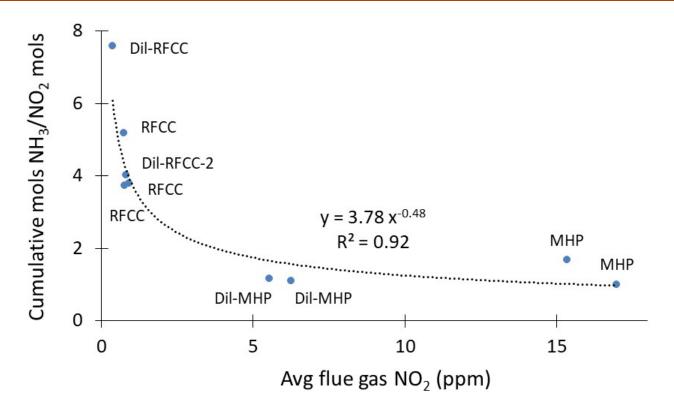
TCM lean sample (unhydrolyzed) free amino acids



NH₃/NO₂ and amino acids at TCM



Modeling NH₃ response to NO₂



Relationship between cumulative mols NH₃/mols NO₂ and [NO₂]_{inst} obeys power law.

Oxidation species (mmol/kg) by LC/MS at TCM

