

OPTIMIZATION OF COOLING FOR POST-COMBUSTION CARBON CAPTURE

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INTRODUCTION

Presentation is based on Fluor's Econamine FG PlusSM (EFG+) technology

- ▶ EFG+ is Fluor's commercially proven, proprietary post-combustion capture technology
- ▶ 30 plants built (to date)
- ▶ Designed for capturing CO₂ from low-pressure gas streams containing oxygen
- ▶ Experience with a wide range of flue gases
- ▶ Compilation of five pre-FEED studies on cooling optimization in 2024 to 2025

EFG+ application flue gas characteristics

3% CO₂ range 20%

1% O₂ range 15%

Gas Turbine and
Engine

Coal-Fired
Boilers

Oil-fired Boilers

SMR in H₂, NH₃,
and MeOH Plants

Tail Gas Units in
Sulphur Plants

Catalytic
Crackers



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THE LOW-GRADE HEAT EXCHANGE PROBLEM

1) Temperatures for carbon capture technology deployment

- ▶ Flue gas source is hot
 - Typically 160 to 180°C downstream of economizer
 - Further cooling challenged by available heat sinks and condensation
- ▶ Majority of capture technologies require modest temperatures
 - Typically 40 to 60°C
 - Aqueous solvents (traditional amines)
 - Solid adsorbents
 - Membranes
 - Cryogenics (even lower)
- ▶ Cooling gap of 100 to 140°C

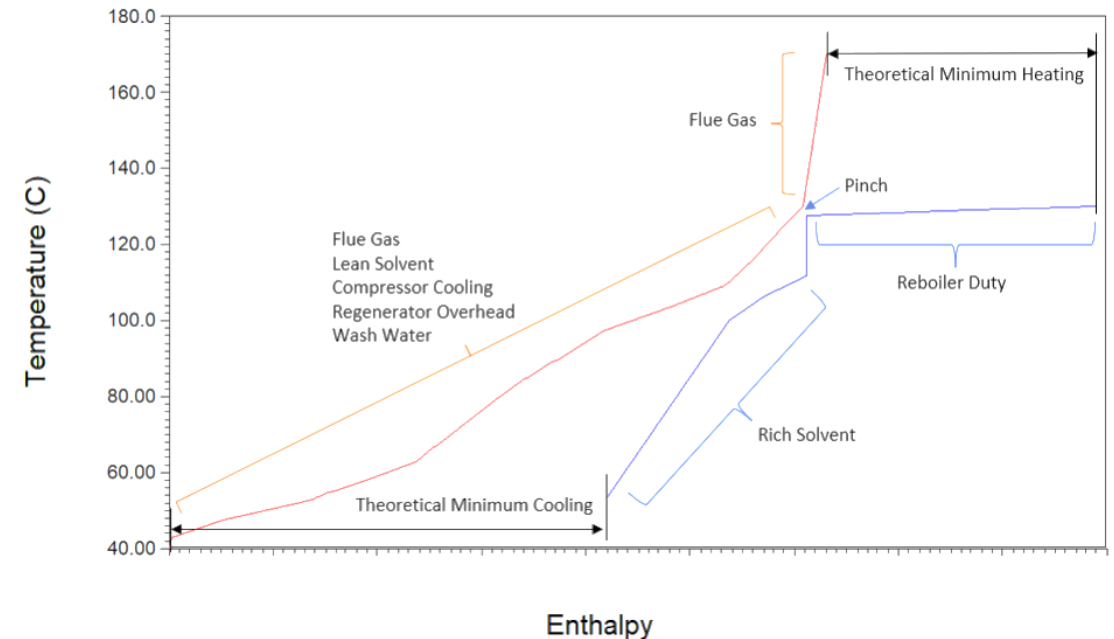


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THE LOW-GRADE HEAT EXCHANGE PROBLEM

2) Thermodynamics of post-combustion carbon capture process

- ▶ Carbon capture itself requires energy
 - Energy from reduction in entropy
 - Heat of absorption/solution
 - Heat from compression
- ▶ Process temperature cycles between
 - Absorption (40 to 60°C)
 - Desorption (120 to 150°C)
- ▶ Heat integration
 - Exhaust economic heat integration options first
 - Net losses through low-grade heat exchange to environment (air and/or water)



Sample Pinch Analysis Curve

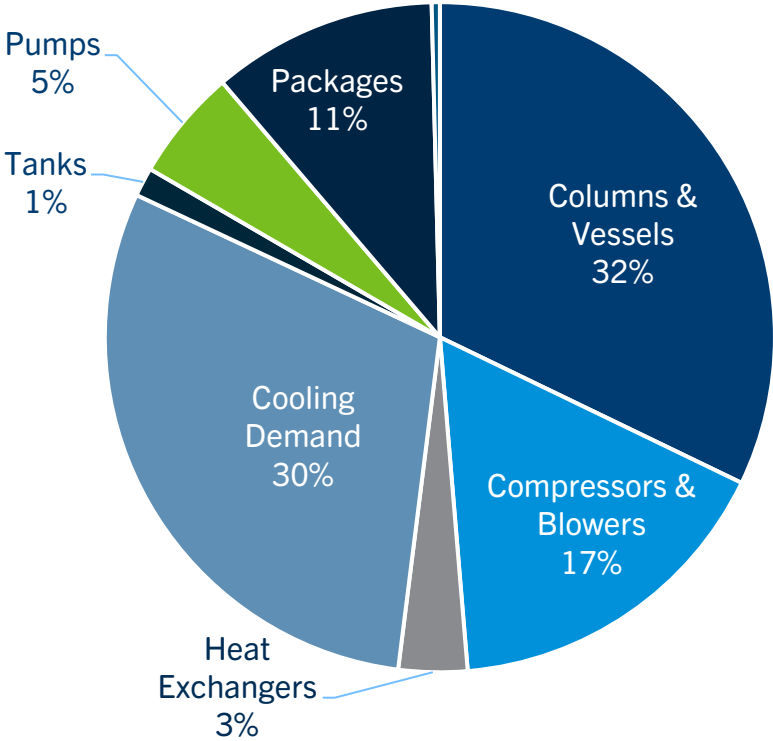


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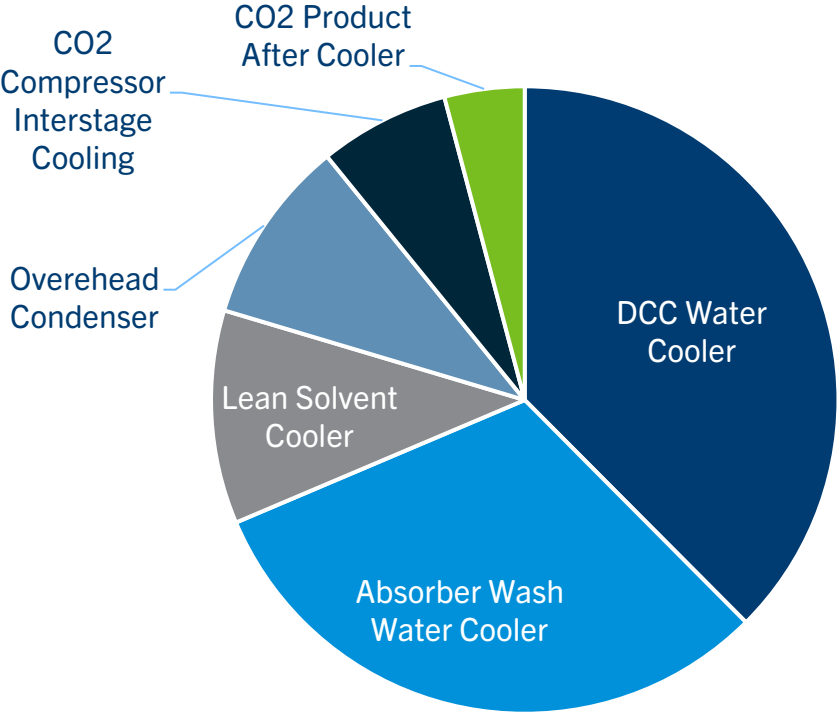
KEY ISSUE

Capital Cost of Carbon Capture*

Plant Equipment Cost



Cooling Duty Breakdown (out of 30%)

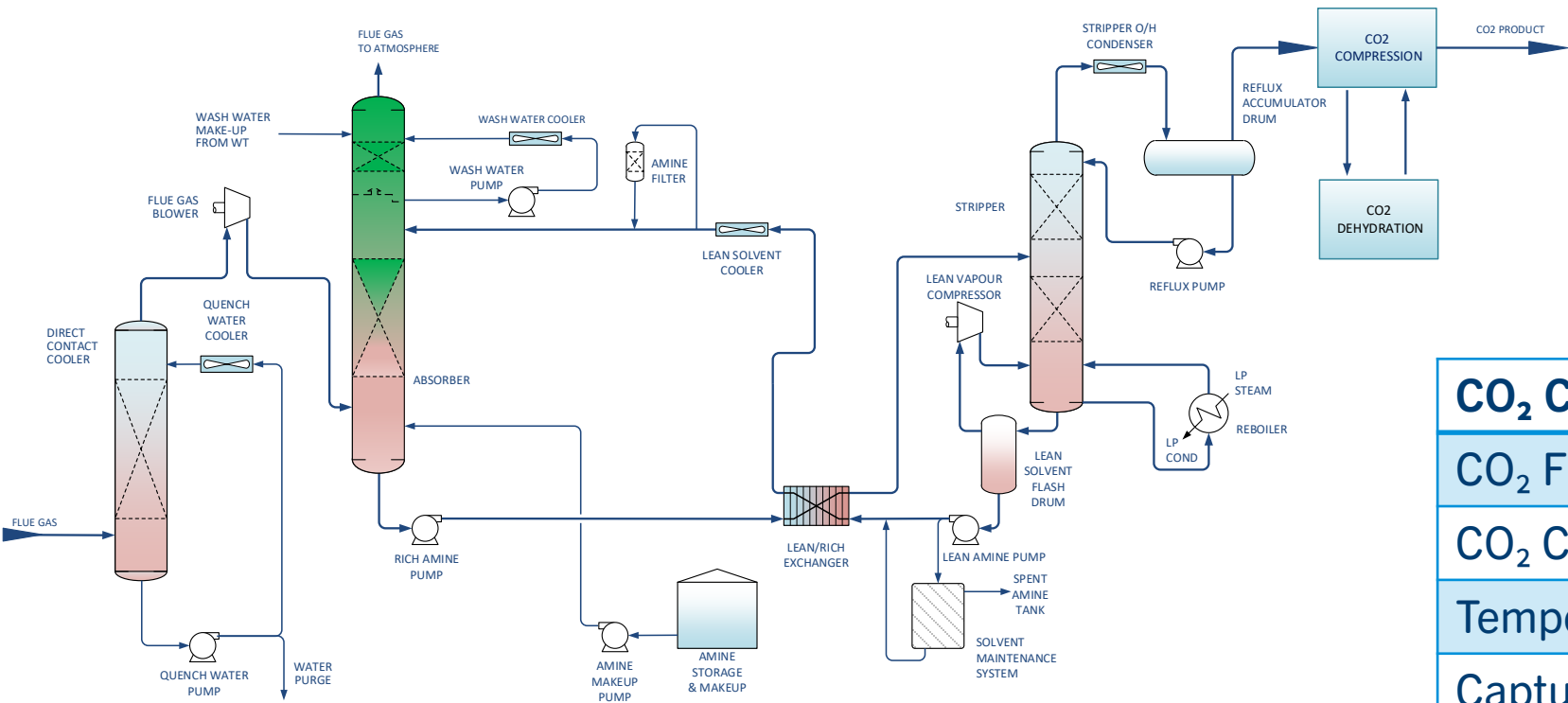


**Sample FEED project, optimized with a hybrid air and cooling water design*



CASE STUDY

Gas Turbine Exhaust



CO ₂ Concentration	4.5 wet vol%
CO ₂ Flow Rate	4,631 MTPD
CO ₂ Capture	4,400 MTPD
Temperature	200°C
Capture Efficiency	95%
Cooling Demand	6 GJ/tonne CO ₂

STUDY METHODOLOGY

- ▶ Equipment cost and total installed cost (TIC) from recent Fluor CCS projects (*United States Dollar [USD] basis*)
- ▶ Wood-Mackenzie Method^[1] utilized for levelized cost of carbon capture, 10 percent discount rate, 25-year project life
- ▶ Reference HMB is held constant for the study
- ▶ Three process cooling methods considered (*on the following slide*)
- ▶ Two project locations considered:
 - Southern California, United States
 - Alberta, Canada
- ▶ CCS is self supporting – i.e., no base plant utility availability for cooling

[1] P. Findlay and J. Mageau, "Towards a standard definition of levelised CCUS costs and revenues," in 17th International Conference on Greenhouse Gas Control Technologies, GHGT-17, Calgary, Canada, 2024.

COOLING METHODS

Cooling Water

- ▶ Cooling tower + P&F exchangers
- ▶ High efficiency
- ▶ Cooling water utility block dedicated plot space
- ▶ Make-up water required
- ▶ Higher water disposal rates

Air Cooling

- ▶ Air-cooled heat exchangers
- ▶ Large ISBL plot space requirement
- ▶ Low operating costs
- ▶ No water requirements
- ▶ No fluid disposal

Secondary Medium

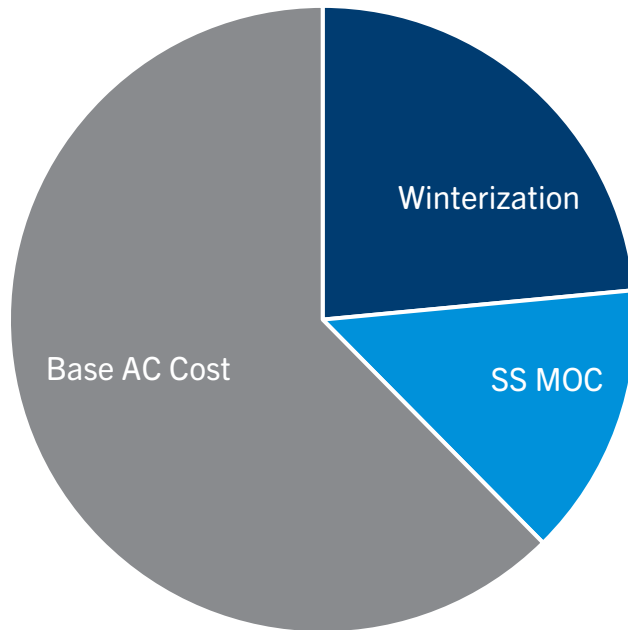
- ▶ Glycol or other non-freezing medium
- ▶ P&F exchangers + air coolers
- ▶ Initial chemical fill required
- ▶ Metallurgy and winterization advantages

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AIR COOLING COST DRIVERS

Alberta, Canada Example

Air Cooler Cost Breakdown

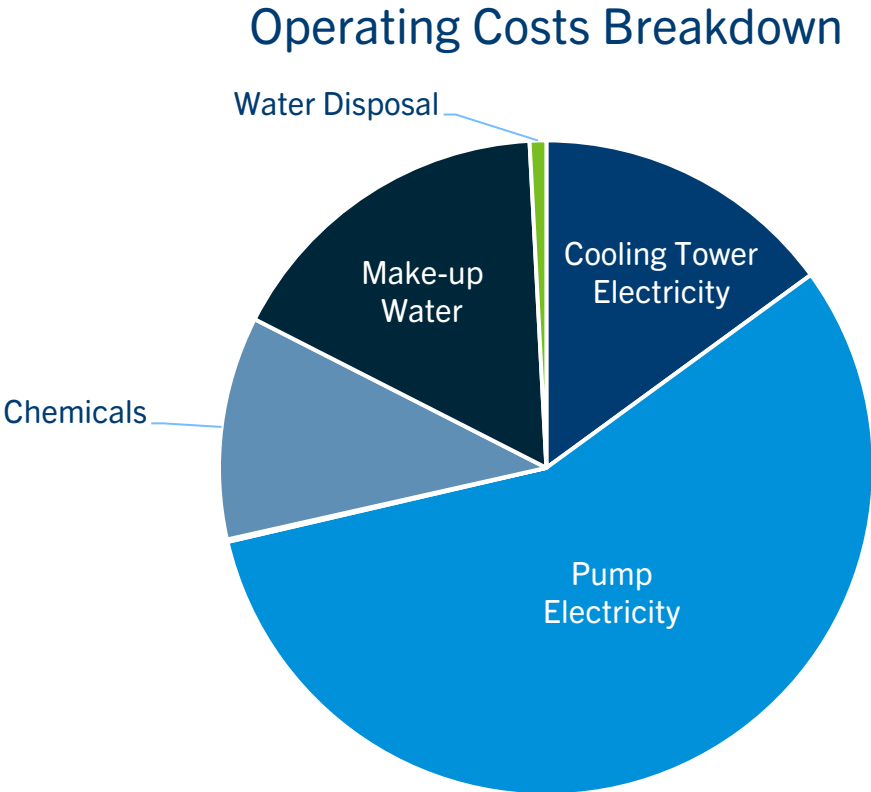
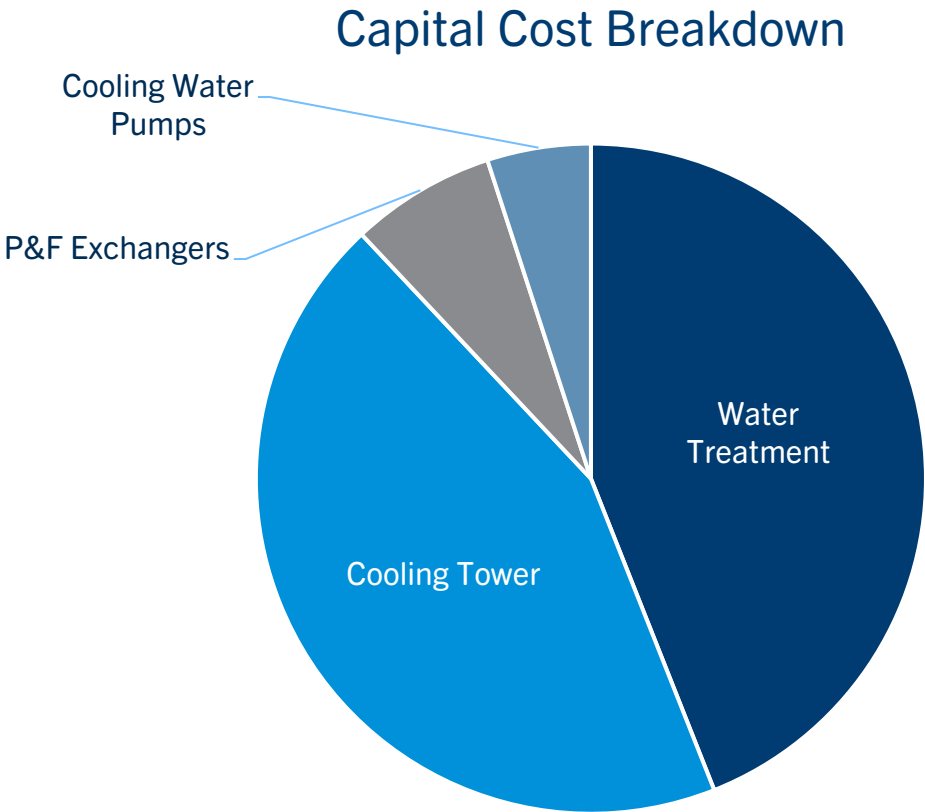


- ▶ Secondary cooling (using glycol)
 - Eliminates winterization
 - Reduces materials cost to about half
 - Cost adder for the glycol loop (capex & opex)
 - Net capex is lower, opex is higher
- ▶ Operating costs are primarily electricity price
 - No dependence on water



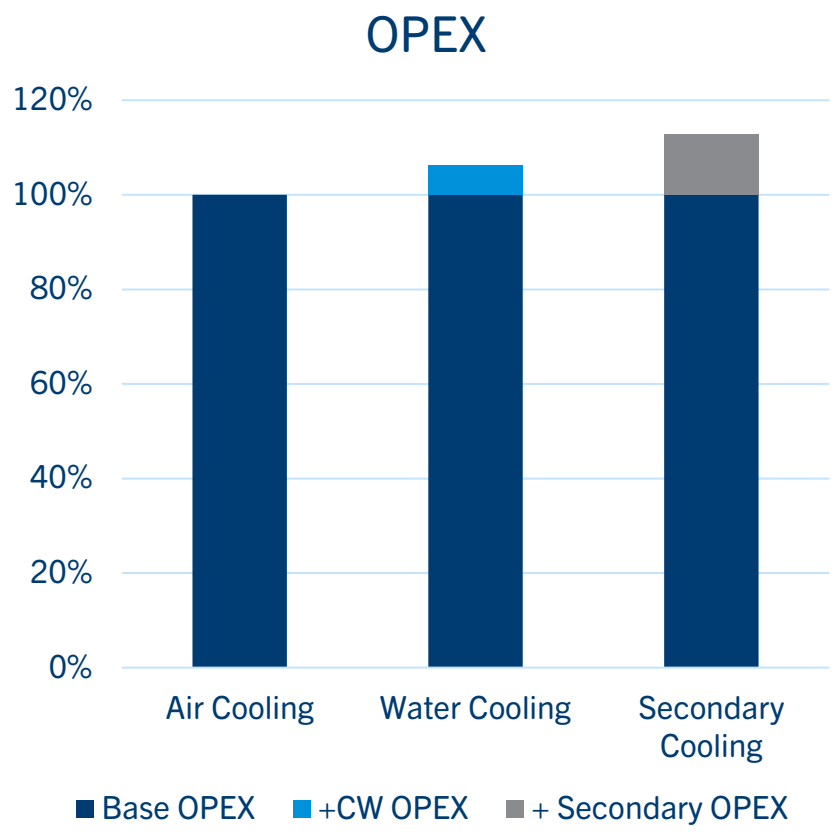
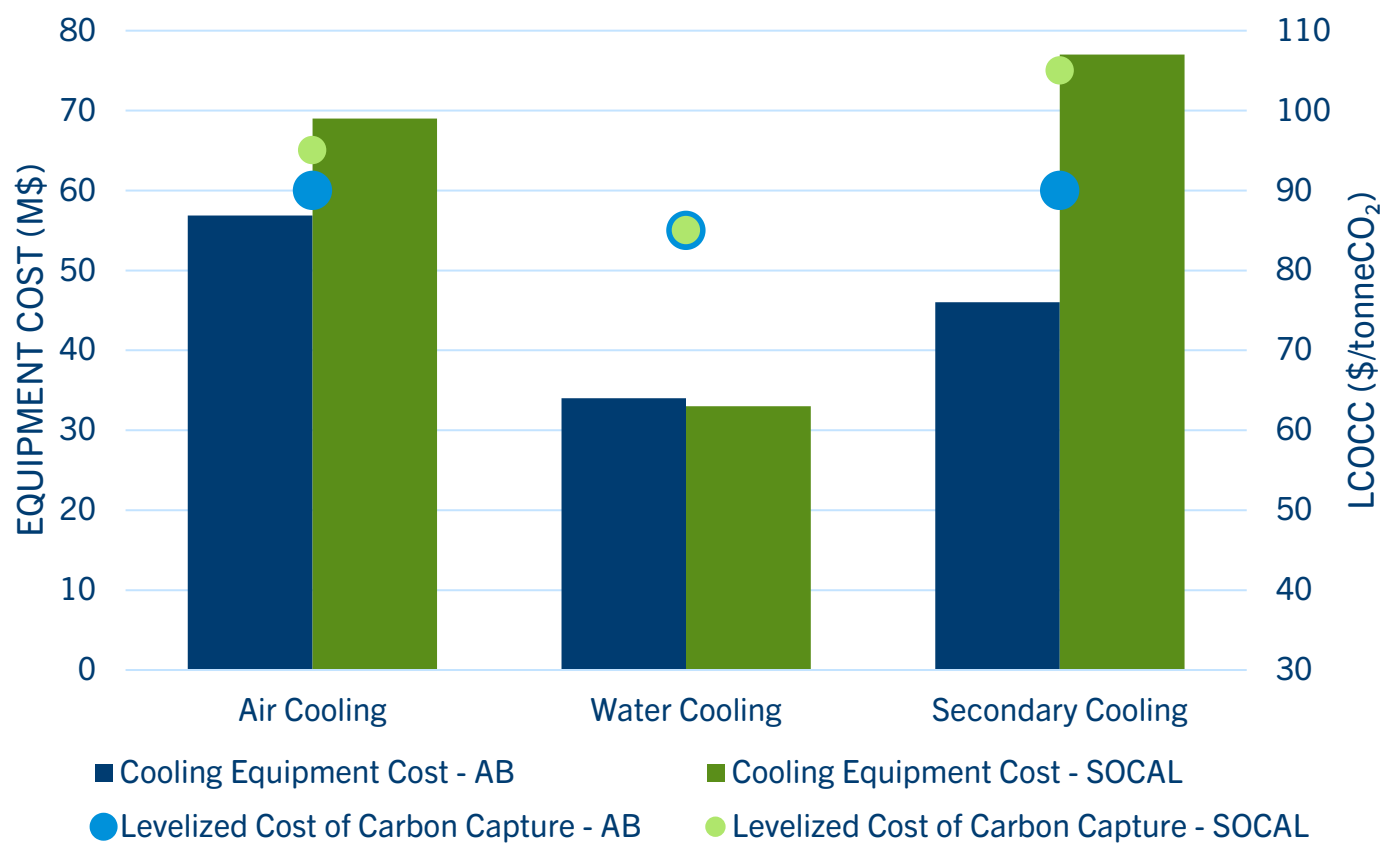
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COOLING WATER COST DRIVERS



RESULTS

Case Economics



Only cooling equipment costs are shown.

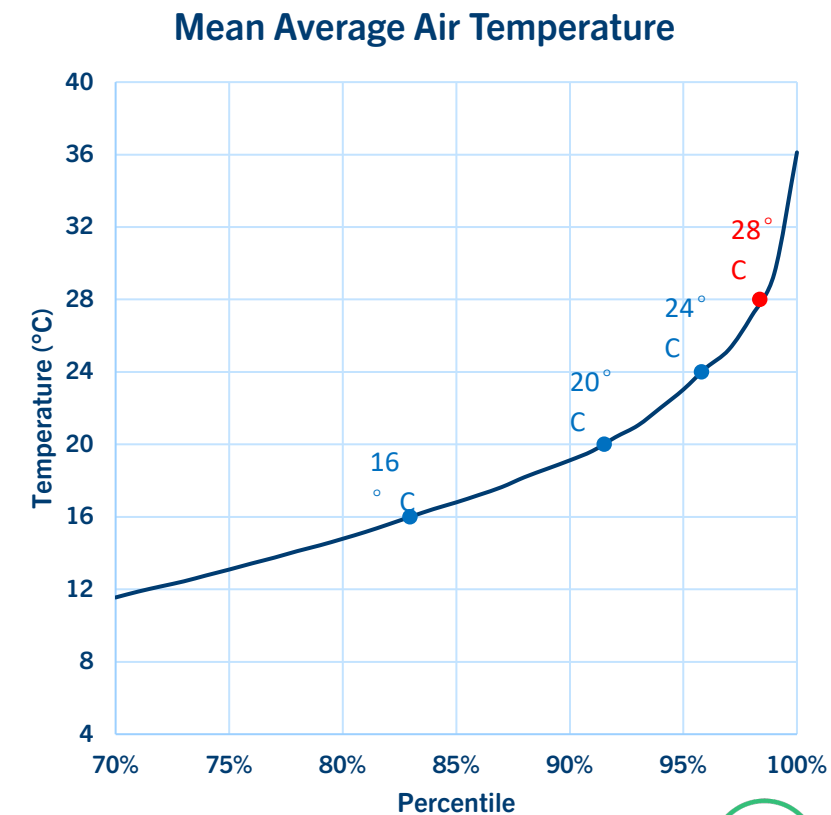


OPTIMIZATION OF DESIGN AIR TEMPERATURE

Alberta, Canada Example

- ▶ Ambient air temperature drives cooling in air cooling applications
- ▶ Design air temperature, and the difference between design air and process temperature, drives cost
- ▶ If the design air temperature is lower, costs are reduced but cooling is undersized on hot days
- ▶ Opportunity to take advantage of lower design air temperature in colder climates

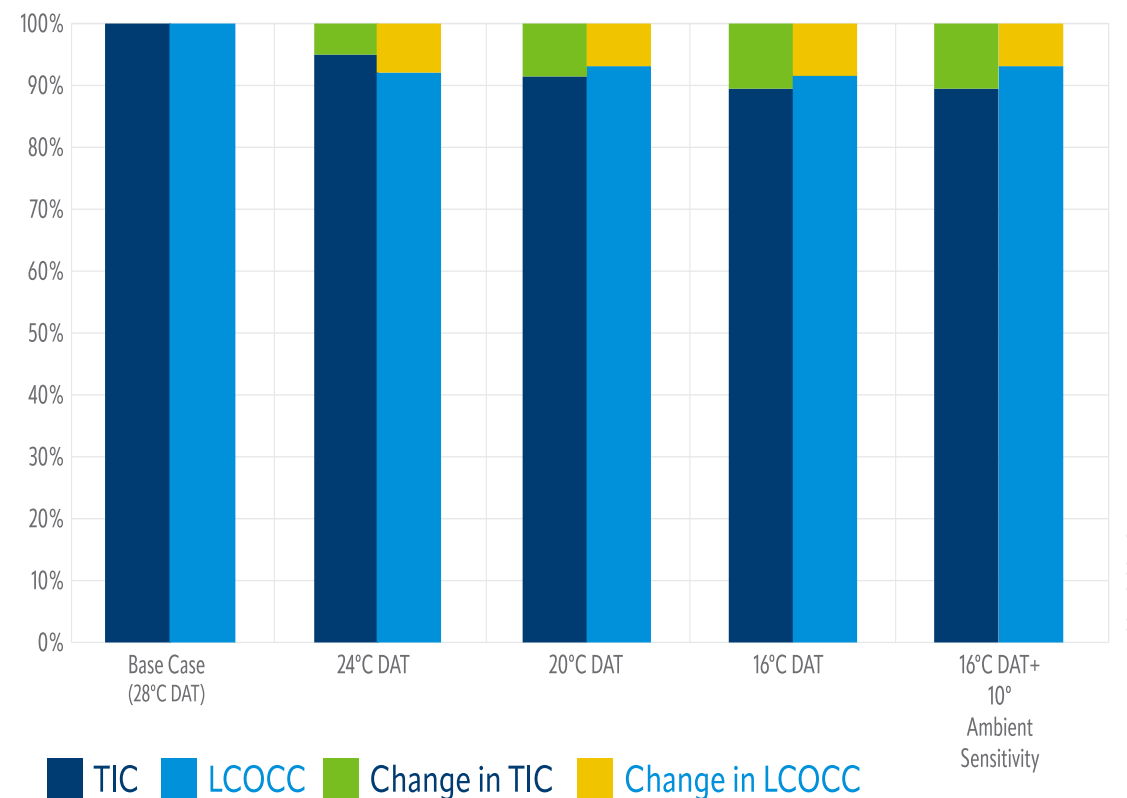
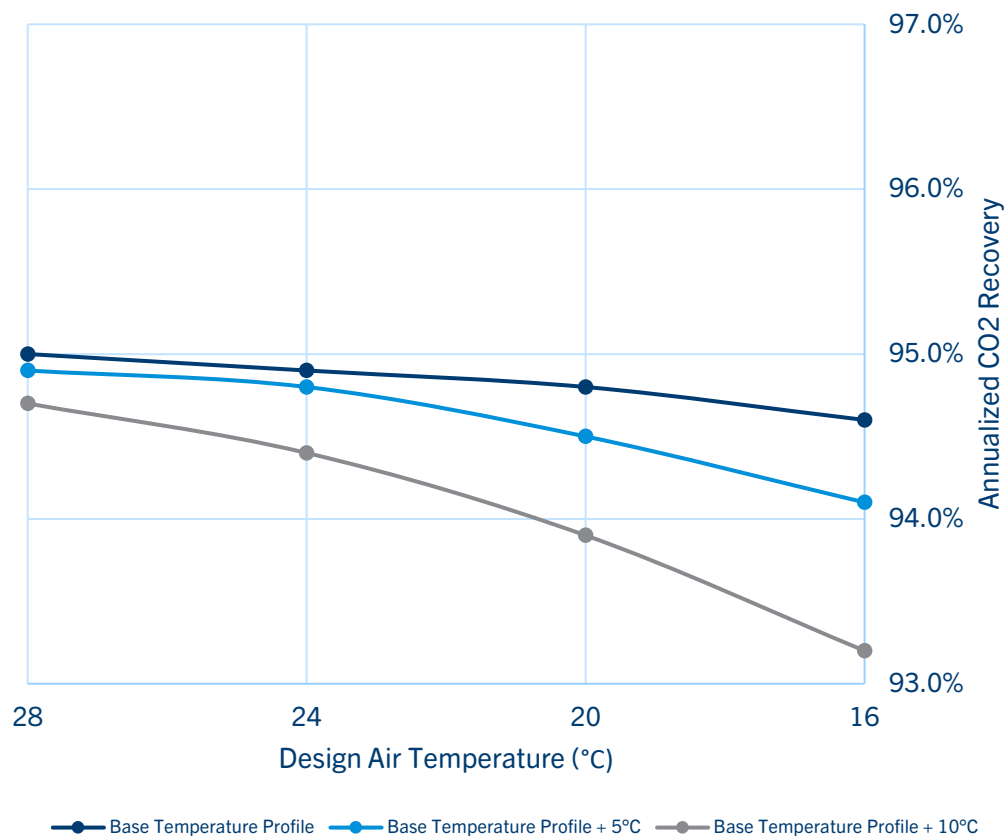
Dry Bulb – Base 28°C	24°C	20°C	16°C
Tube Area Reduction	-24%	-38%	-47%



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OPTIMIZATION OF DESIGN AIR TEMPERATURE

How Much CO2 Recovery is Lost if Air Coolers are Undersized?

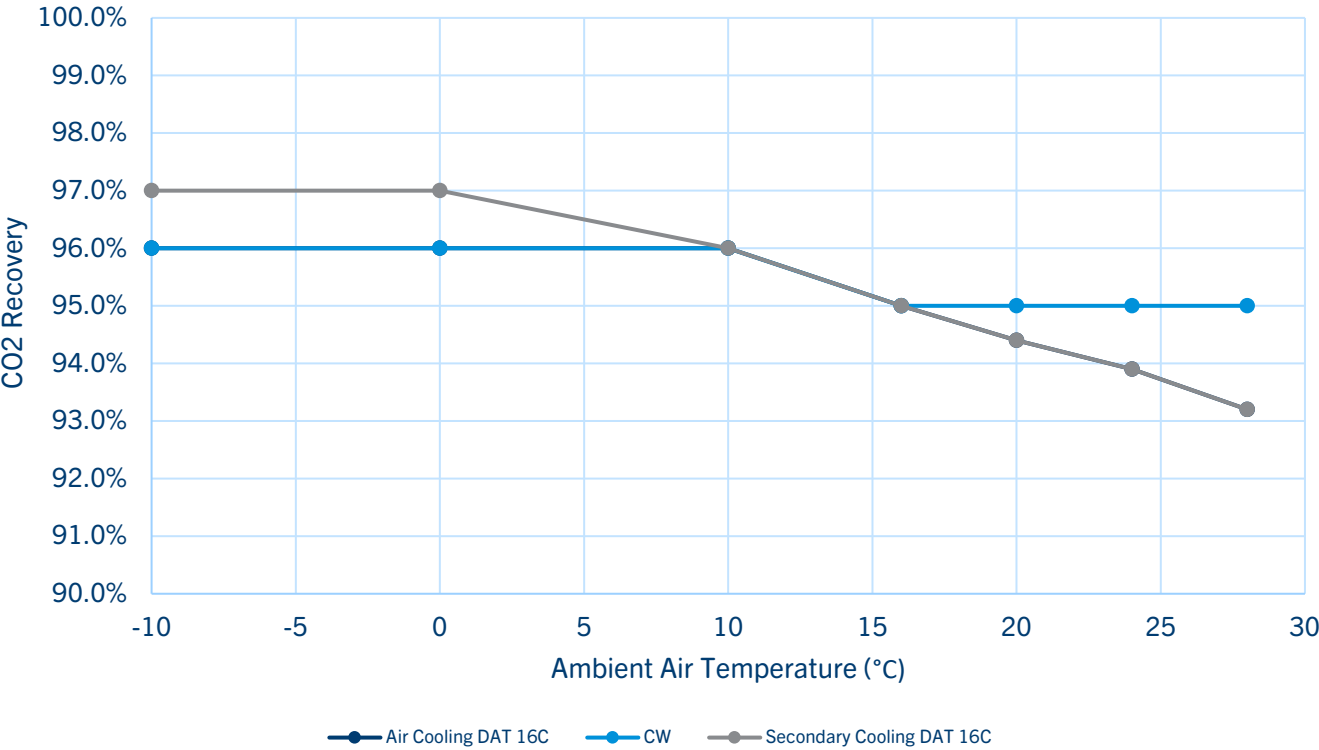


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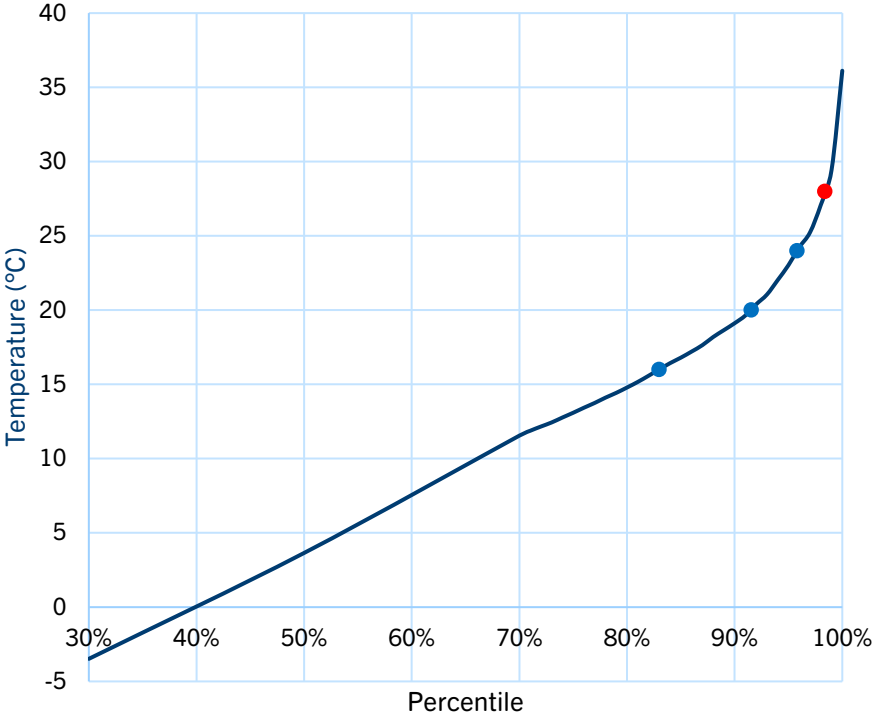
SEASONAL INTEGRATION OF AIR COOLING

Alberta, Canada Case

Expected CO2 Recovery



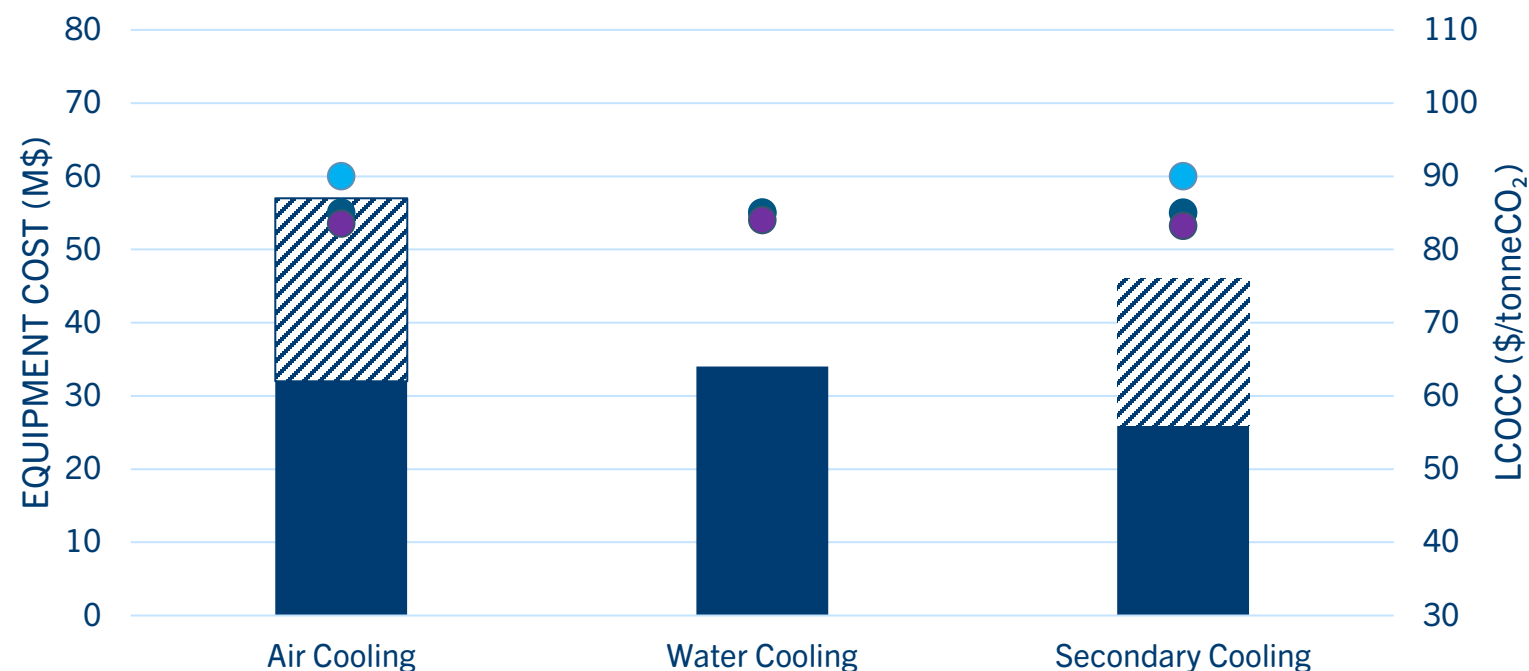
Mean Average Air Temperature



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COOLING IN A COLDER CLIMATE LOCATION

Results from Alberta, Canada Case Considering Seasonal Variability



■ Cooling Equipment Cost - AB

● Levelized Cost of Carbon Capture - 16°C DAT

● Levelized Cost of Carbon Capture - AB

● Levelized Cost of Carbon Capture - 16°C DAT w/ Winter Recovery

OTHER CONSIDERATIONS

- ▶ Hybrid cooling scheme optimization (air + water)
- ▶ Process water balance control is important with seasonal variability
- ▶ Solvent health and degradation
 - Capture efficiency cannot be jeopardized
 - Mitigate heat exchanger fouling
- ▶ Flow scheme and process optimization
 - Lean vapour compression
 - Heat recovery opportunities



CONCLUSIONS

Optimization of Cooling for PCCC

- ▶ PCCC cooling requires significant capital cost
- ▶ Climate (location) and utility availability constrain the facility
 - Water cooling, if available, is more economically attractive
 - Air cooling is less competitive using traditional approach
 - Air cooling can be optimized for colder climates
- ▶ No ‘single solution’ or wholistic approach available
- ▶ Integration of CCS island and BOP presents opportunity to lower costs
- ▶ Project economics are best optimized with a wholistic approach with the CCS technology provider



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THANK YOU

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