



Insights into Maintaining High Soaking Pressure during CO₂ Huff-n-Puff in Shale Oil Reservoirs

Introduction

Since 2008, shale gas and oil production has grown substantially, generating strong momentum for exploration and production efforts (Gasparik et al., 2012). After multi-stage fracturing in horizontal wells, oil production consistently demonstrates a sharp decline within the first year, followed by a prolonged low-production rate period. Notably, the predicted oil recovery factor during the primary depletion process is generally less than 10% (Du et al., 2019; Li et al., 2022). To enhance oil recovery in unconventional oil reservoirs, technologies i.e., nanoparticles, gas injection, etc. have been investigated to improve sweep and/or displacement efficiencies (Shi et al., 2024; Ji et al., 2024; Wang et al., 2025). Previous experimental results of injecting CO₂ have shown significant potential to improve shale oil recovery by molecular diffusion, oil swelling, interfacial tension and viscosity reduction, and light components extraction (Jiang et al., 2022; Yang et al., 2025). CO₂ huff-and-puff has been regarded as a reliable and effective strategy for enhancing oil recovery in shale oil reservoirs as the injectivity of CO₂ injection is favorable as a result of continuous gas pathways from fracture and penetrating into the rock matrix through the diffusion mechanism. In the meantime, the injected CO₂ could be trapped in shale formations permanently.

CO₂ huff-and-puff in shale oil reservoirs typically starts with the injection of CO₂ into a single well and the injected CO₂ mainly occupies in hydraulic or natural fractures. Then, a shut-in or soaking period is performed to allow the CO₂ to dissolve into the oil in matrix, swell its volume, and reduce its viscosity. The concentration gradient pushes CO₂ to permeate into the matrix, and the volume of CO₂ contacted with oil relies on the solubility and diffusivity of CO₂, which are dependent on the soaking pressure and time. Subsequently, the well is returned to production and the response is monitored. Many researchers have concluded that CO₂ dissolution and diffusion are the dominant mechanisms for CO₂ EOR in shale oil reservoirs (S. B. Hawthorne et al., 2013; Tovar et al., 2021). However, the CO₂ dissolution and diffusion would lead to the reservoir pressure drops during soaking processes. Field test in the Lucaogou tight oil reservoir show that the wellhead pressure decreased from 27.6 MPa to 11.5 MPa during soaking process as CO₂ migrated into deep matrix pores driven by pressure and concentration gradients (Shi et al., 2024). The decreased pressure near wellbore hole conversely reduces the CO₂ solubility and diffusion coefficient, and thus significantly affect the performance of CO₂ huff-and-puff. Therefore, maintaining injection pressure during soaking by continuous injecting CO₂ could enhance the solubility and diffusivity of CO₂, thus improve the sweep efficiency and performance of CO₂ huff-and-puff.

In this study, maintaining high soaking pressure was proposed to enhance CO₂ dissolution and diffusion during soaking process. Four cycles' CO₂ huff-and-puff experiments with and without pressure maintenance were conducted considering different soaking pressure and time. In addition, nuclear magnetic resonance (NMR) T₂ distributions after each soaking cycles were collected to investigate the oil mobilization in different pore sizes. The findings in this study provides new insights into the field application of CO₂ huff-and-puff in shale oil reservoirs.

Materials and Experimental Method

The synthetic shale oil used in this study was prepared by mixing the crude oil collected from Shengli Oilfield with C12 (in a 1:1 ratio). The CO₂ with a purity of 99.999% was purchased from Dongfeng gas supply company, Chengdu. Synthetic core plugs with a diameter of 38 mm and length of 50 mm in were used to eliminate the effect of rock petrophysical properties on the performance of CO₂ huff-n-puff experiment. The porosity and permeability of the core plugs are 7.5% and 0.1 mD, respectively. Before experiment, the core plugs were dried in an oven at 100°C for 24 hours to remove moisture and were then vacuumed and saturated with oil under 25 MPa pressure for 48 hours. The core plugs were weighed after saturation process and T₂ spectra were collected using the low-field Nuclear Magnetic Resonance (LF-NMR) apparatus.



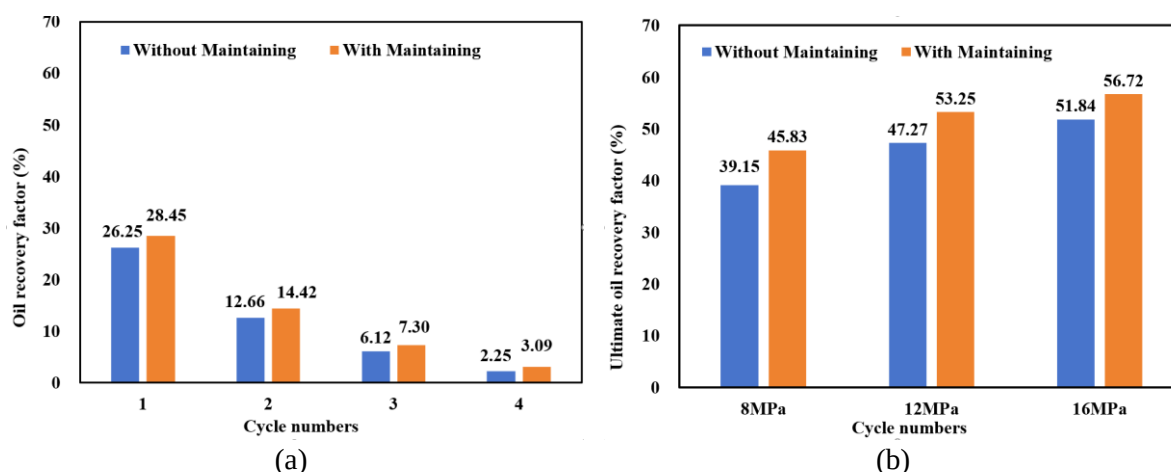
Ten cases of CO₂ huff-n-puff experiments with and without soaking pressure maintenance were designed considering different soaking pressure and time, as shown in Table 1. A brief introduction of the huff-n-puff experiment procedures are described as follows. (1) The core plug saturated with oil was placed vertically in the reactor and vacuumed for 2 hours. Then, the reactor was heated to maintain a constant temperature of 80°C. (2) CO₂ was injected into the reactor until the designated pressures were reached. The intake valve was then closed for the soaking propose. (3) After the soaking was complete, the pressure in the reactor was slowly reduced to atmospheric pressure. After cooling, the core plug was weighed and the T₂ spectrum was collected. (4) Steps (1) to (3) were repeated three times at the same injection pressure for the multicycle CO₂ huff and puff processes. (5) Oil recovery factor in each cycle was calculated based on the mass changes of the core plug after soaking.

Table 1. Experimental design of CO₂ huff-n-puff.

Scenario	Case	Soaking pressure (MPa)	Soaking time (h)	Cycle number
Without maintaining soaking pressure	1	8	4	4
	2	12	4	4
	3	16	4	4
	4	12	2	4
	5	12	6	4
Maintaining soaking pressure	6	8	4	4
	7	12	4	4
	8	16	4	4
	9	12	2	4
	10	12	6	4

Experimental Results and Discussion

Figure 1(a) shows the oil recovery factor of four CO₂ huff-n-puff cycles at the pressure and temperature of 12 MPa and 80°C, and the soaking time is 4 hours (cases 2 and 7). The oil recovery diminishes from 26.25% to 2.25% after four cycles for both cases with and without maintaining soaking pressure. As is respected, the oil recovery factor increases slightly when the soaking pressure is maintained during soaking process, which is because more CO₂ contacts oil in inner pore spaces by gas diffusion. After four cycles, the overall oil recovery increased from 47.27% to 53.25%, as shown in Figure 1(b). On the other hand, the oil recovery for cases without soaking pressure maintenance increases with soaking pressure, which are 39.15%, 47.27% and 51.87% at 8, 12, 16 MPa, respectively. In comparison to cases without pressure maintenance, oil recovery increased 6.68%, 5.98%, 4.86% for cases with pressure maintenance at 8, 12, 16 MPa, respectively.



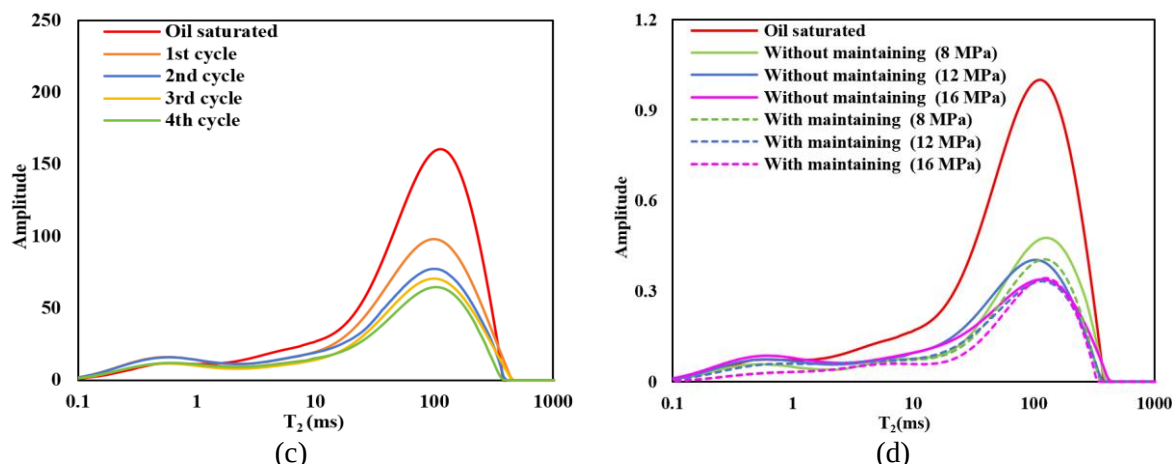


Figure 1 (a) Oil recovery factor at different cycles for cases 2 and 7. (b) Oil recovery factor with and without maintaining pressure at different soaking pressures. (c) T_2 distributions at different cycles for case 2. (d) Normalized T_2 distributions of fully oil saturated, and after soaking at 8, 12 and 16 MPa.

Oil mobilization in pore scale at different cycles for case 3 is evaluated from the NMR T_2 distribution results, as shown in Figure 1(c). Larger T_2 values corresponds the oil in larger pore spaces, and vice versa. In the first cycle, oil in larger pore spaces were recovered, and the amount of oil produced decreases with increasing cycles. This agrees with oil recovery factor showed in Figure 1(a). After four cycles, there are still unrecovered oil in larger pore spaces as well as smaller pore spaces. In addition, normalized T_2 distributions of fully oil saturated, and after soaking core plugs at 8, 12 and 16 MPa are showed in Figure 1(d). More oil can be recovered at higher soaking pressure, especially for cases with maintaining soaking pressure (dashed lines). It is interesting to note that oil in smaller pore spaces can be mobilized at the soaking pressure of 16 MPa, which is because the CO_2 solubility and diffusion coefficient are higher at larger pressure gradients. CO_2 can be transferred into inner and smaller pore spaces, and swells oil and reduces oil viscosity.

In addition to the soaking pressure, increasing soaking time also affects the amount of CO_2 transferred into inner and smaller pore spaces. Figure 2(a) shows the oil recovery factor at different soaking time for both with and without maintaining soaking pressure (soaking pressure: 12 MPa). The oil recovery factor increases with the soaking time of 2, 4, 6 hours, which are 42.77%, 47.27 and 54.09%, respectively. The oil recovery increasements with and without maintaining soaking pressure are 3.06%, 5.98% and 5.39% when soaking time increases from 2 hours to 6 hours, indicating an optimum soaking time can be determined depending on the amount of oil unrecovered. Similar to soaking pressure cases, more oil can be mobilized by prolonging the soaking time. However, maintaining soaking pressure at longer soaking time still cannot mobilize oil in smaller pore spaces.

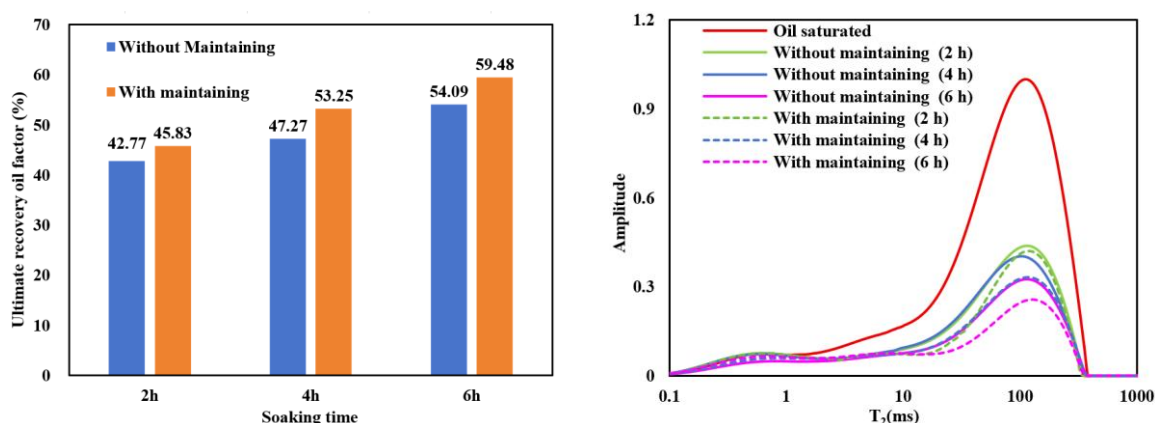


Figure 2 (left) Ultimate oil recovery factor at different soaking times. (right) Normalized T_2 distributions of fully oil saturated, and after 2-, 4- and 6-hours' soaking.



Conclusions

CO₂ dissolution and diffusion would lead to the reservoir pressure drops during soaking processes, which conversely reduce the CO₂ solubility, diffusion coefficient, and thus lead to the decrease of the ultimate oil recovery. Increasing soaking pressure and time can enhance the CO₂ dissolution and diffusion during CO₂ huff-n-puff in shale oil reservoirs. In this study, maintaining high soaking pressure was proposed in this study and the CO₂ huff-and-puff experiments with four cycles considering different soaking pressure and w/wo pressure maintenance were conducted. Experimental results show that the oil recovery factor for each cycle and the ultimate oil recovery factor increases by maintaining soaking pressure and prolonging the soaking time. The high soaking pressure maintenance technique proposed in this study effectively addresses the issue of pressure drop during the soaking phase, thereby increasing oil recovery. The findings in this study provides new insights into the field application of CO₂ huff-and-puff in shale oil reservoirs.

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