

Carburization and Melting of Hot Compacted Iron in a Coke Bed

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ABSTRACT

One of the key technologies in developing hydrogen-enriched ironmaking operations is the control of the carburization, melting, and dripping behavior of the iron ore burden materials. When a hot compacted iron (HCI) is charged in the blast furnace or the FINEX Melter-Gasifier, iron oxide reduction, the reduced iron's carburization, and the melting of iron and slag occur successively. This study investigated the reduction, carburization, melting and dripping behaviour of HCI under a CO-H₂ gas mixture using the high-temperature X-ray radiographic technique. Under 100% CO gas atmosphere, the dripping temperature was 1410°C. When 5% H₂ was introduced, the dripping temperature slightly decreased to 1400°C. Furthermore, the dripping temperature gradually increased as the H₂ gas composition increased. As 30% H₂ was introduced, the dripping temperature reached 1414°C. The carbon concentration in the drained metal samples gradually increased with increasing H₂ composition. It is considered that H₂ decreased FeO content in the slag, yielding the increased melting temperature and viscosity of the slag. On the other hand, H₂ accelerated the carburization of the reduced iron by CO gas, enabling the homogenization of the oxide materials to form a liquid phase. Therefore, it is considered that introducing H₂ in the reactor is helpful to increase productivity and energy efficiency by accelerating the liquid phase's formation.

INTRODUCTION

Steel is recognized as an essential material for sustainable development [IEA 2020]. Steel is used as an essential core material in renewable energy production, such as solar and wind power generation and nuclear power generation. Steel is also used as the core material of energy-efficient transportation: automobiles, ships, and trains. For example, steel is used for electric vehicle bodies, battery packs, and electric motors. The adoption of steel is also increasing for zero-energy building construction. At the same time, however, the demand for the reduction of greenhouse gas emissions from the iron- and steel-making processes cannot be ignored; the steel industry emits about 7% of global greenhouse gas emissions [IEA 2020], so the development of new zero-carbon processes is required.

Technology that utilizes hydrogen in the blast furnace process and FINEX process is considered the most realistic alternative to reduce greenhouse gas emissions [Yi 2019]. New iron ore burdens have been developed to be used in the H₂-enriched ironmaking process [Park 2023b], [Park 2022], [Park 2020], [Rajavaram 2016]. Here, low-reduced iron (LRI) is charged in the blast furnace or in the Melter-Gasifier as a form of hot compacted iron (HCI) [Yi 2021]. As the hydrogen is introduced in the reactor, the reduction of iron oxide is accelerated, and the liquid slag formation temperature increases [Lan 2020], [Long 2016]. Accordingly, the melting and dripping temperature of burden materials would be delayed, when compared to the conventional blast furnace operation [Dereje 2018]. Then, a stable gas permeability in the coke bed becomes complex to establish, and the efficient heat transfer from the gas to the burden materials would not be guaranteed. Consequently, controlling the holdup of liquid phases in the coke bed will be difficult.

In the coke bed, the carburization of the reduced iron generally takes place in advance, yielding successive liquid slag formation by homogenizing the oxide phases [Park 2021]. Therefore, much attention is paid to the acceleration of the carburization of the reduced iron. Fruehan reported that the carburization of solid iron was enhanced by introducing H₂ gas [Fruehan 1973]. Shin et al. carried out a series of experiments and revealed that the carburization was affected mainly by the ash content in the coke [Shin 2014], [Shin 2012] [Jang 2012b]. Shin et al. also reported that FeO content lowered the carburization and melting behavior of the reduced iron [Shin 2015]. Kim et al. suggested that the reaction was accelerated due to Marangoni flow [Kim 2001]. Despite much research on this matter, no report has been published for in-situ observation of the carburization, melting, and dripping behavior of the HCI sample under the CO-H₂ gas atmosphere.

Recently, the high-temperature X-ray radiographic technique has been utilized to investigate liquid phases' melting and dripping behavior through the coke bed [Shin 2010], [Park 2021]. In the present study, the carburization, melting, and dripping behavior of HCI in the coke bed is investigated by using the high-temperature X-ray radiographic method. Here, the effect of the composition of the CO-H₂ gas mixture is investigated.

EXPERIMENTAL

The experimental apparatus comprised a MoSi₂ resistance furnace and a high-temperature X-ray radiographic inspector system. A schematic illustration is shown in Fig. 1. An alumina reaction tube (inner diameter of 90 mm and length of 1000 mm) was placed vertically in the furnace. Coke particles of 8~9 mm diameter were charged in a graphite crucible (inner diameter of 55 mm and height of 75 mm) with 33 holes of 5 mm diameter drilled in the bottom. There were four layers of coke particles in the crucible. An ellipsoidal-type HCl sample (longer-axis length of 3.8~4.7 mm, shorter-axis length of 3.1~3.3 mm, and height of 1.5~2 mm) was then placed on the top of the coke layer. The samples used in this study were provided by POSCO. The chemical compositions of the HCl are given in Table 1. The reduction degree of HCl is 57.2%. The chemical composition of the coke and its ash contents are given in Tables 2 and 3, respectively. The sample assembly was covered by a graphite lid, and it was heated to 1000°C at a heating rate of +5°C/min under an N₂ gas atmosphere. From 1000°C, the reaction gas was changed into a CO or CO-H₂ gas mixture with a predetermined mixing ratio. The reaction gas was blown on the surface of the HCl sample with a flow rate of 1 L/min STP through an alumina lance (inner diameter of 6 mm) with a distance of 10 mm. The melting and dripping behavior of metal and slag was investigated with the high-temperature X-ray radiographic system with a tungsten target X-ray tube. The experiment finished at 1500°C, and the sample was cooled to room temperature in the furnace. After experiments, the carbon and sulfur compositions of the drained metal samples were analyzed with LECO-C/S analyzer.

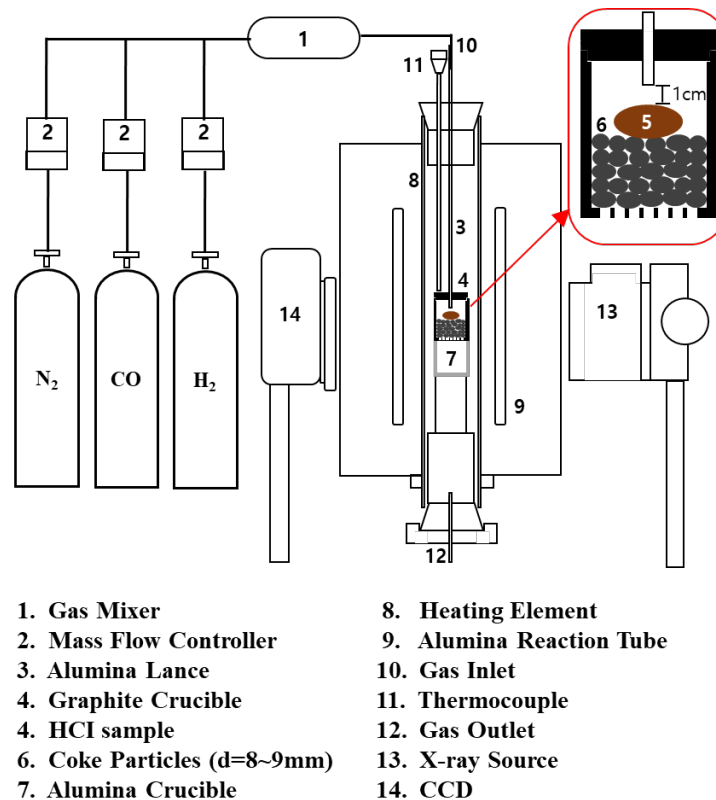


FIG 1 – Experimental apparatus for in-situ observation of carburization and melting

TABLE 1 – Chemical composition of the HCl sample

Element	Total Fe	Metallic Fe	FeO	CaO	SiO ₂	Al ₂ O ₃	MgO
wt%	72.2	32	36	3.7	4.2	2.1	1.2

TABLE 2 – Chemical composition of the coke particle

Element	Fixed C	Ash	Volatile Matter	Moisture
wt%	86.36	11.66	1.76	0.22

TABLE 3 – Chemical composition of the ash contents in the coke

Element	SiO ₂	Al ₂ O ₃	Fe ₂ O ₃	CaO	K ₂ O	P ₂ O ₅	MgO
wt%	54.55	27.40	6.08	2.78	1.28	1.09	0.87

RESULTS AND DISCUSSION

Ex-situ Observation

Fig 2 shows the top view and the cross-section view of the sample assembly. It is considered that the amount of metal holdup decreased while the slag holdup increased. The color of the slag was changed from grey-green to white, indicating that the FeO content in the slag gradually decreased. Fig. 3 shows the carbon and sulfur contents of the drained metal samples. The carbon concentration gradually increased, whereas the sulfur concentration monotonically decreased. Since the contact between the reduced iron and the coke particles was not controlled precisely, it is more reasonable to investigate the general trend of the chemical composition change with increasing the H₂ concentration in the gas mixture. Here, the decrease in the sulfur content supported the idea that the carburization reaction by the CO-H₂ gas mixture was more pronounced than that by direct contact with coke particles because the sulfur source was the coke [Lee 2007]. Accordingly, it is speculated that the increased H₂ concentration accelerated the reduction of iron oxide, which might increase the melting point of the slag, while increasing the slag viscosity [Nakamoto 2004].

Consequently, the slag holdup increased with increasing H₂ concentration. This observation shows a similar trend as the experimental results of Shin et al. [Shin 2015] with designed model experiments. In this study, the ash content would prevent carburization by solid coke [Jeong 2012b]. Park et al. reported that solid ash or high-viscosity liquid ash slag might prevent the carburization reaction by direct contact with coke particles [Park 2023a]. Therefore, there were more chances for the CO-H₂ gas mixture to provide the carbon source for the reduced iron.

In-situ Observation

Fig 4 shows the in-situ observation results of the sample assembly under a CO gas atmosphere. At 1280°C, liquid slag first appeared. Liquid metal formation was first investigated from 1380°C. This carburization and melting might be accelerated by the involvement of the FeO-containing slag [Kim 2001]. The liquid metal suddenly started to drain at 1409°C, while liquid slag remained in the coke bed. The drain of liquid slag occurred when the liquid metal pulled the liquid slag together. The liquid slag flew over the surface of liquid metal. A similar observation was reported by Jeong et al. [Jeong 2013]. However, in the present experiment, some part of the liquid metal eventually remained in the coke bed.

Fig. 5 shows the in-situ observation results when the CO-20%H₂ gas mixture was introduced. In this experiment, the first liquid slag formation was investigated at 1280°C, which is the same as the experiment with 100% CO gas. The liquid metal formation appeared at 1403°C. Due to the rapid reduction of iron oxide by H₂ gas, the carburization would not be enhanced by the existence of liquid slag. At 1405°C, the drain of liquid slag was investigated, followed by the drain of liquid metal. It is considered that the introduction of H₂ gas enhanced the carburization by CO gas.

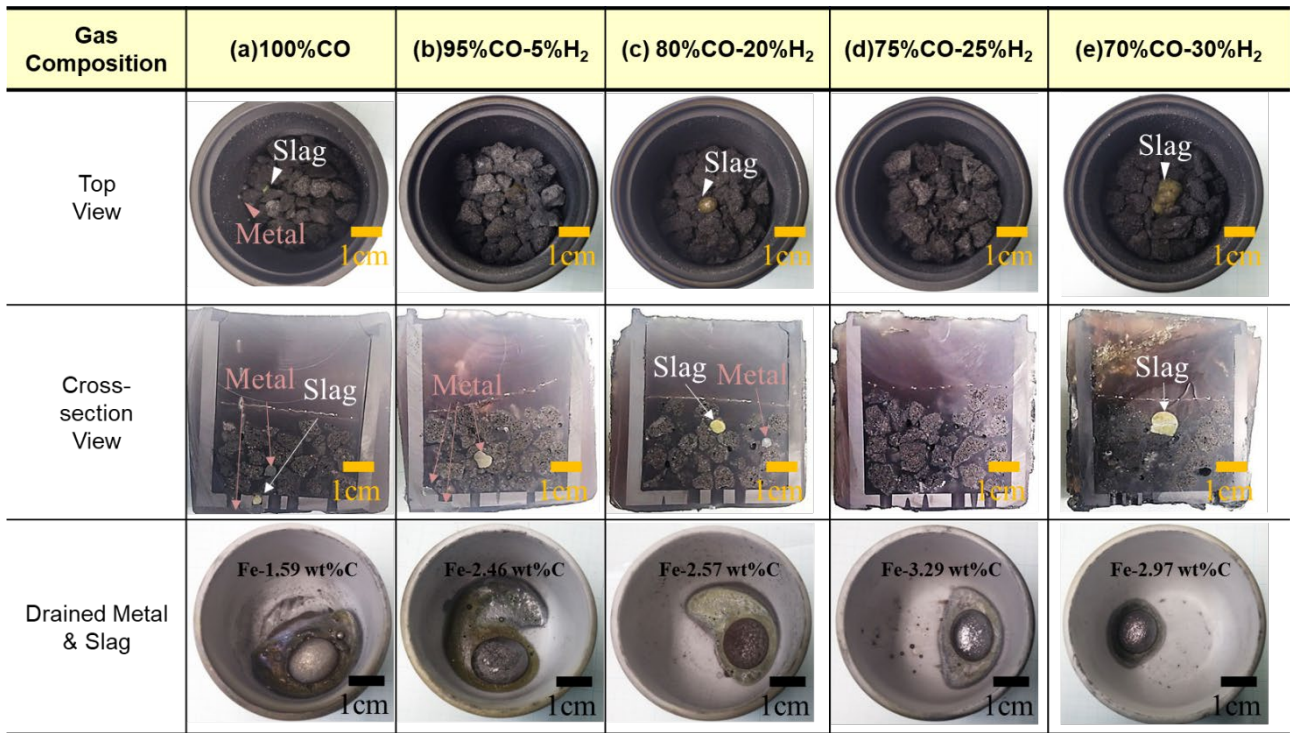


FIG 2 – Top and cross-section views of the sample assembly after experiments. The gas composition was varied (a)100% CO, (b) 95%CO-5%H₂, (b) 80%CO-20%H₂, (c) 75%CO-25%H₂, and (d) 70%CO-30%H₂. The drained metal and slag samples are shown separately.

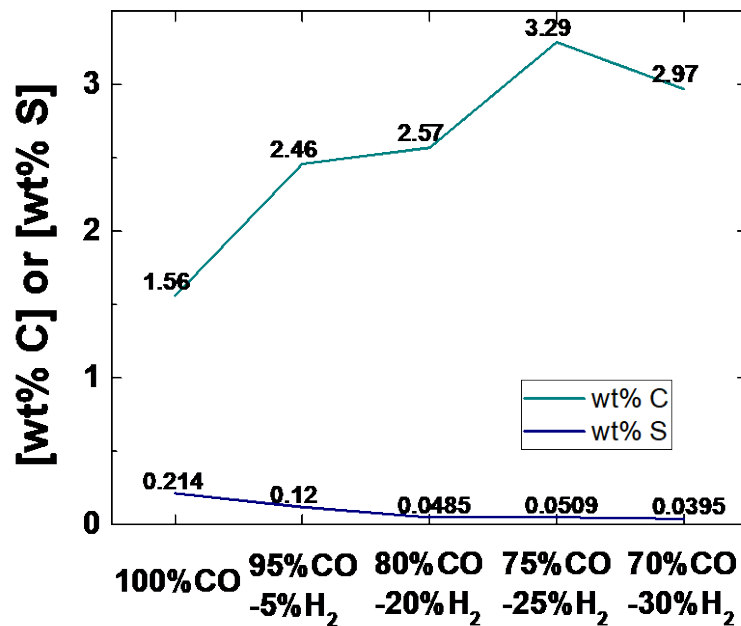


FIG 3 – Top and cross-section views of the sample assembly after experiments. The gas composition was varied (a)100% CO, (b) 95%CO-5%H₂, (b) 80%CO-20%H₂, (c) 75%CO-25%H₂, and (d) 70%CO-30%H₂. The drained metal and slag samples are shown separately.

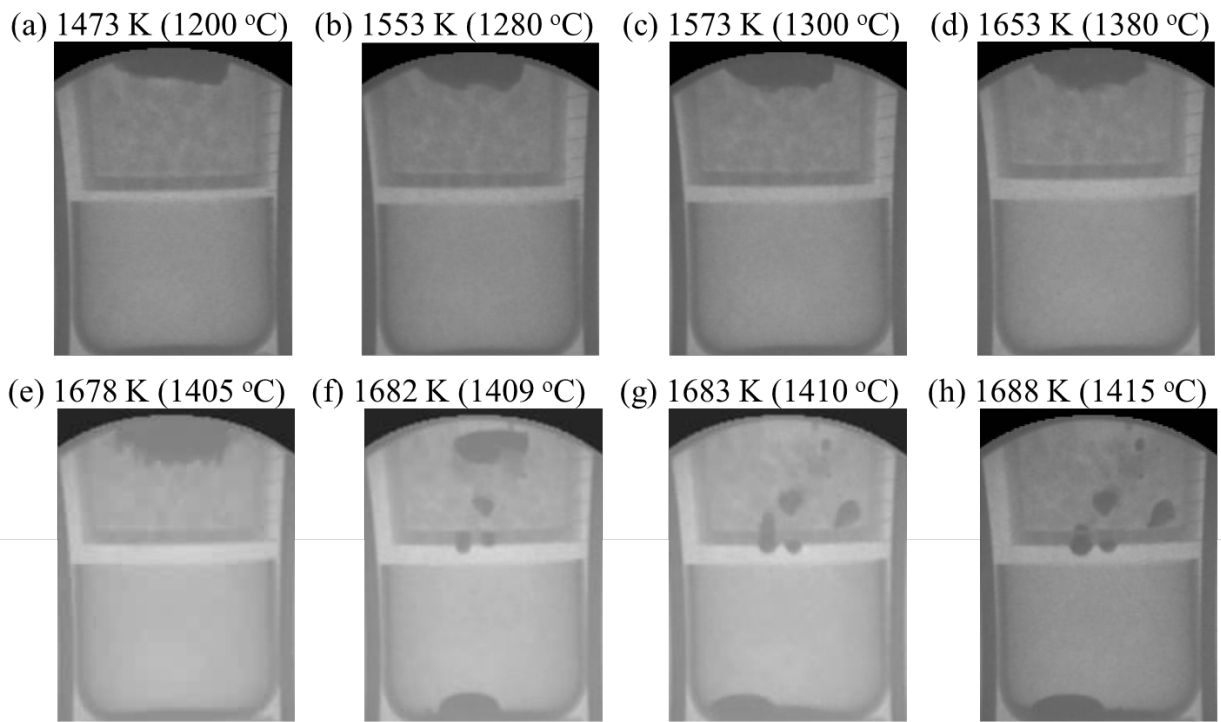


FIG 4 – In-situ observation of liquid metal and liquid slag formation from HCl on a coke bed under CO gas atmosphere.

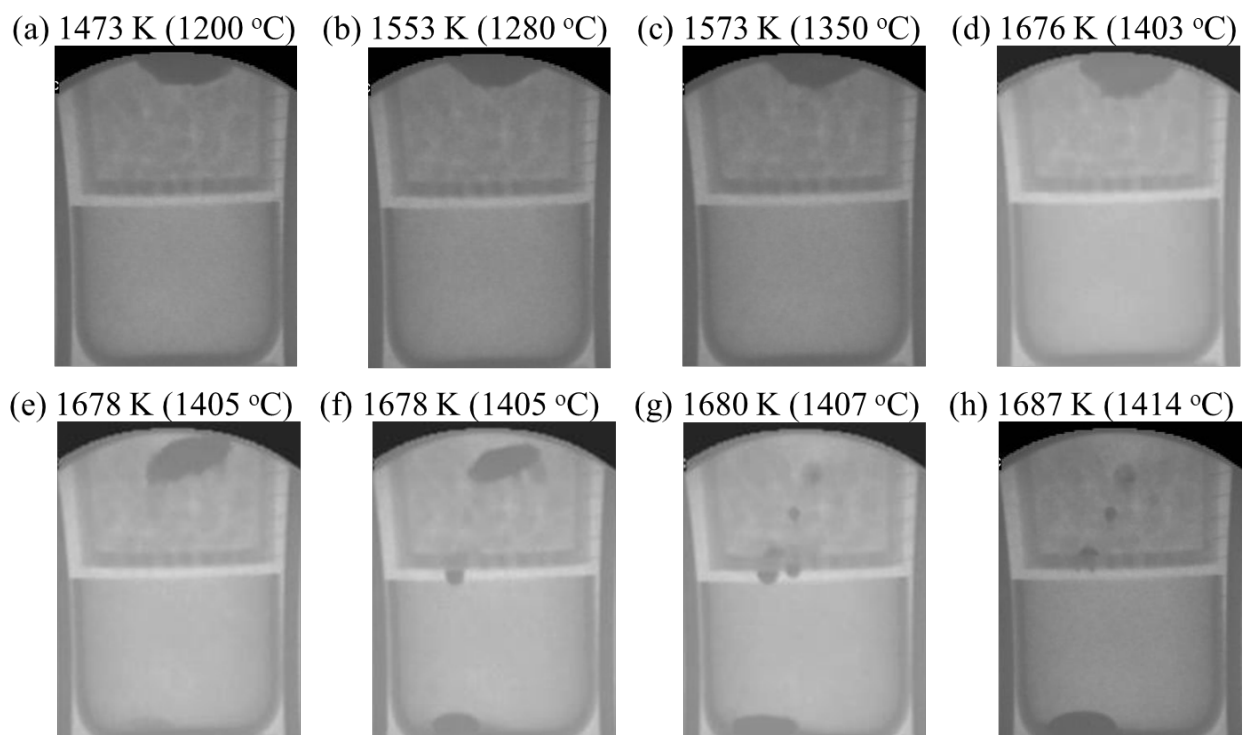


FIG 5 – In-situ observation of liquid metal and liquid slag formation from HCl on a coke bed under CO-20% H_2 gas atmosphere.

It is considered that the introduction of H₂ gas decreased FeO content in the slag, yielding the increased melting temperature of the slag as well as the slag viscosity [Park 2023a]. On the other hand, H₂ gas accelerated the carburization of the reduced iron, enabling the homogenization of the oxide materials to form a liquid phase [Oh 2017]. Therefore, it is considered that a reasonable introduction of H₂ in the blast furnace of the FINEX melter-gasifier is helpful to increase productivity and energy efficiency by accelerating the liquid phase's formation.

The slag holdup is affected by the particle size of the coke and thermophysical properties of liquid slag, such as density, surface tension, viscosity, and wettability [Jang 2012a], [Dereje 2021], [Dereje 2020]. In the practical blast furnace or FINEX melter-gasifier operations, the formation of the SiC layer would reduce the slag holdup by drastically modifying wettability [Kim 2023], [Oh 2016]. Therefore, the increased slag holdup investigated in this study would be reduced by the introduction of H₂ gas. Hence, the H₂-injecting ironmaking process would be more favorable for the establishment of an energy-efficient ironmaking process [Park 2023a].

In this study, however, detailed critical analysis, such as microstructure analysis of the sample and phase identification, was not carried out because the slag composition was changed by the reaction with the crucible. More sophisticated experimental design is anticipated in future work.

CONCLUSIONS

The reduction, carburization, melting, and dripping behavior of HCl was investigated under a CO-H₂ gas mixture with the high-temperature X-ray radiographic technique. Fig. 6 shows the summary of the experimental results. Under 100% CO gas atmosphere, the dripping temperature was 1410°C. When 5% H₂ was introduced, the dripping temperature slightly decreased to 1400°C. As the H₂ gas composition increased further, the dripping temperature gradually increased. The carbon concentration in the drained metal samples gradually increased with increasing H₂ composition. It is considered that H₂ decreased FeO content in the slag, yielding the increased melting temperature of the slag, while it also accelerated the carburization of the reduced iron by CO gas, enabling the homogenization of the oxide materials to form a liquid phase. It is considered that a reasonable introduction of H₂ in the reactor is helpful in increasing productivity and energy efficiency by accelerating the liquid phase's formation.

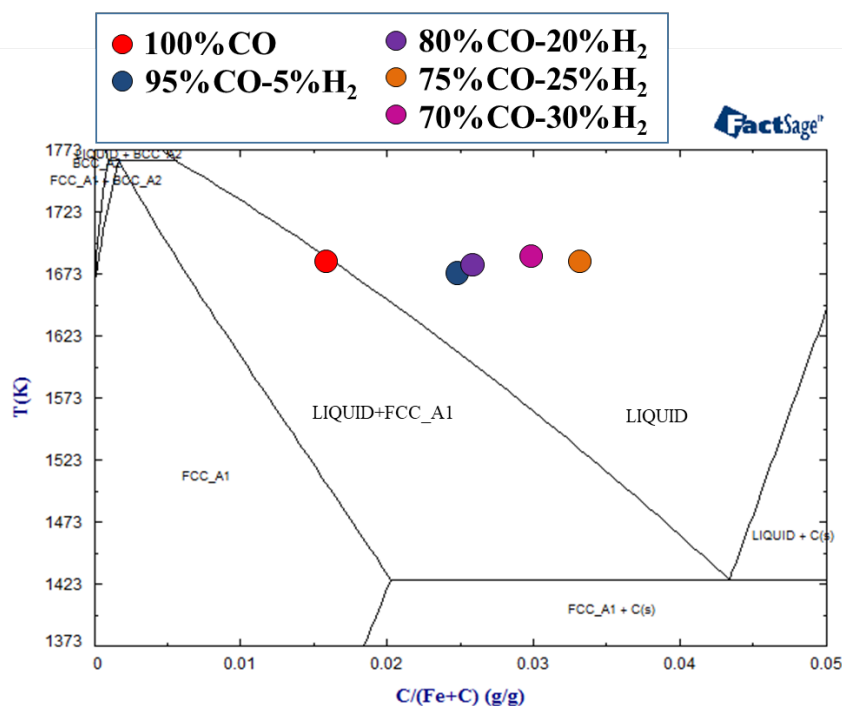


FIG 6 – Dripping temperature with respect to the carbon concentration of the dripped metal under various gas atmosphere.

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